EVALUATING FLUSHING PROCEDURES TO PREVENT DRUG CARRYOVER DURING MEDICATED FEED MANUFACTURING

by

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B.S., Universidad Autónoma de Nuevo León, 2007

A THESIS

submitted in partial fulfillment of the requirements for the degree

MASTER OF SCIENCE

Department of Grain Science & Industry College of Agriculture

KANSAS STATE UNIVERSITY Manhattan, Kansas

2008

Approved by:

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Abstract

Carryover of medicated feed additives between batches of feed can potentially result in harmful drug residues in the edible tissues of food-animals. Flushing the equipment with an ingredient, such as ground grain, is one method used to remove any residual medicated feed from the system. It is generally recommended that the quantity of flush used be between 5 and 10% of the mixer's capacity. However, there is little data that supports this recommendation. Therefore, two experiments were conducted to 1.) determine which manufacturing equipment is the major source of carryover, 2.) evaluate which flush size adequately prevents drug carryover, and 3.) quantify the interrelationship between flush size and drug concentration. In Experiment 1, feed medicated with nicarbazin (Nicarb 25%®; 0.0125%) was manufactured and conveyed from the mixer, through a drag conveyor and bucket elevator, and then into a finished product bin. The system was then flushed using ground corn in the amount of 2.5, 5, 10, 15, or 20% of the mixer's capacity (454.5 kg). Subsequently, a non-medicated diet was conveyed through the system and samples were collected and analyzed for nicarbazin. No significant (P > 0.05) differences were detected among the flush treatments, and all treatments were effective in preventing nicarbazin carryover to the non-medicated diet. In Experiment 2, feed medicated with three levels of monensin (Rumensin® 80; 100, 600, and 1,200 g/ton) was manufactured and handled in the same manner as in Experiment 1. The flushing treatments examined were: 1, 2.5, and 5% of the mixer's capacity. Samples of the non-medicated diet for each treatment were collected and analyzed for monensin. There was significant interaction (P < 0.05) between drug level and sampling location between treatments. As the drug level in the medicated diet

increased, higher concentrations of monensin were detected in the non-medicated diet. Collectively, these studies demonstrate that a 2.5%, even a 1% flush size, is effective in preventing carryover of medicated feed additives. It was also demonstrated that the bucket elevator and finished product bin were the major sources of drug carryover in this particular feed manufacturing system.

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Dedication

I would like to dedicate this thesis to my parents, Aida and Gustavo, and to my siblings, Gus and Giga. Mom and Dad: Thank you for everything! You are my pillar of strength! I would like to express my sincere gratefulness for all your loving support and your constant words of encouragement. Gus and Giga: You are my best friends! You have always been there to help me, support me, and motivate me. Thanks for always being there for me! I also want to thank my uncle Jorge, my mentor. All of this was possible because of your unconditional support. I shall be forever in your debt. Thank you so much!

CHAPTER 1 - Introduction

Overview of Food Safety

In the last decade, there has been a substantial increase in the level of public awareness and concern relative to the safety and security of food supply. Consequently, the food industry has placed much emphasis on ensuring food safety. In spite of this increase in awareness, notable incidents still occur such as the most recent case of melamine contamination in the pet food industry (FDA, 2008). It has been estimated that pet food manufacturers have voluntarily recalled more than one hundred brands of dog and cat food across the United States since the outbreak (FDA, 2007a). This food safety incident also came to be an issue of concern to humans, since a portion of the pet food produced was used to feed food-producing animals. However, it was determined that the food-producing animals that were fed melamine contaminated feed posed a very low risk to human health (FDA, 2007b; USDA, 2007). With incidents like this, the need to develop outreach programs that disseminate information, guidelines, and risk-assessment strategies to producers, manufacturers, distributors, as well as consumers becomes a necessity to prevent contamination of our food supply. The United States' food supply has become one of the world's safest as a result of the implementation of these types of programs and through continuous monitoring of manufacturing, processing, and distribution facilities. The agencies that work together to provide a safe food supply in the United States include the United States Department of Agriculture (USDA), and the Food and Drug Administration (FDA).

The USDA, through the Food Safety and Inspection Service agency (FSIS), is responsible that all domestic and imported meat, poultry, and processed egg products are safe,

properly labeled and packaged accordingly. The USDA accomplishes this by establishing meat production standards in addition to routine inspections of food-producing animals and processing facilities. Meat production standards are established for food packaging, plant sanitation, and thermal processing. Inspections are also routinely performed on food-producing animals before and after slaughter, and on processing facilities to verify compliance with Sanitation Standard Operating Procedures (SSOP) regulations.

The FDA, through the Center of Veterinary Medicine (CVM), is responsible for ensuring quality and safety in foods and animal feeds, regulating the manufacture and distribution of feed ingredients and complete feeds, as well as assuring the safety and efficacy of animal drugs. This is accomplished with the evaluation of animal drugs for use in food-producing animals and through routine inspections of a facility's compliance with Current Good Manufacturing Practices (CGMP) regulations. These regulations contain the principles and guidelines for medicated feed manufacturing and are considered minimum guidelines. Below these minimum guidelines, products are deemed adulterated.

Current Good Manufacturing Practice Regulations – Feed Industry

The CGMP regulations for food and drugs are published in Title 21 of the Code of Federal Regulations (CFR). Title 21 consists of three chapters that are regulated by the FDA, the Drug Enforcement Administration, and the Office of National Drug Control Policy. The CGMP regulations are found in Parts 110 and 225 of Chapter 1 and are regulated by the FDA. Part 110 applies to the manufacturing, packing, and holding of human food, whereas Part 225 applies to the manufacturing, packing, and holding of medicated feed. All food and feed manufacturing, processing, and distribution facilities must comply with CGMP regulations. The legal basis of CGMP compliance for animal drugs is found in the Federal Food, Drug, and Cosmetic Act (FD&C Act, 2008). It states that if the methods, facilities or controls used for manufacturing, processing, packing, and holding of a drug (including a drug contained in a medicated feed) do not comply with CGMP, it would be deemed adulterated. Compliance with CGMP regulations assures that such drugs meet safety, identity, strength, quality, and purity requirements.

Depending on the drug sources used to manufacture medicated feed, medicated feed manufacturers are divided into two groups: those required to register and obtain a license with the FDA and those not required to be registered nor licensed (FDA-HHS, 2007a). This determines which section of the CGMP regulations manufacturers must abide by. Licensed facilities must comply with sections 225.10 through 225.115, whereas non-licensed facilities must comply with sections 225.120 through 225.202 of the CGMP regulations.

Drugs are divided into two categories – Category I and Category II (FDA-HHS, 2008). Category I drugs require no withdrawal period at the lowest use level in each approved species, and Category II drugs require a withdrawal period at the lowest use level for at least one approved species, and are regulated on a "zero-residue" basis.

Drug sources are divided in three types - Type A medicated articles, Type B and Type C medicated feeds (FDA-HHS, 2008). Type A medicated articles are products of standardized potency that contain one or more animal drugs intended for use in the manufacture of another medicated article or a medicated feed. Type B medicated feeds are produced from a Type A medicated article and are intended to manufacture either a Type B or Type C medicated feed. Type B

medicated feed. Type C medicated feed may be offered free choice together with other animal feed.

Facilities incorporating Category II - Type A medicated articles to animal feed must register with the FDA, obtain a Feed Mill License (FML), comply with more stringent CGMP regulations, perform regular drug assays, and are subjected to a mandatory biennial inspection by the FDA. These facilities must comply with criteria established in sections 226.10 through 226.115 of the CGMP regulations, which stipulates methods used in the manufacturing, processing, packing, and holding of Category II - Type A medicated articles (FDA-HHS, 2007b). Facilities manufacturing feed using all Category I and/or Category II - Type B drugs are not required to register with FDA or obtain a FML. As non-licensed facilities, they are subject to less detailed CGMP regulations, and are not subject to routine FDA inspections, although they may be inspected for cause or by state officials.

Compliance with CGMP regulations will not only ensure a product meets safety, identity, strength, quality, and purity standards, it will also prevent one of the major issues during medicated feed manufacturing – drug carryover. Drug carryover during medicated feed manufacturing may result in unsafe drug contamination of subsequent batches. This is may be detrimental to certain animal species and poses a risk for consumers through unsafe drug residues in the edible products from these animals (NRC, 1999). To avoid unsafe drug contamination, the CGMP regulations require subjecting all manufacturing equipment that comes in contact with animal drugs or medicated feed to effective cleanout procedures.

Drug Carryover during Medicated Feed Manufacturing

Unsafe drug contamination in animal feed is defined as the level of drug contamination which would result in an above tolerance drug residue in the edible tissue of the food-producing

animal or which has deleterious effects when fed to animals. The CGMP regulations require medicated feed manufacturers to use one or more approved cleanout procedures, such as cleaning, sequencing, and/or flushing to prevent drug carryover (FDA-HHS, 1976). Cleaning demands the complete shutdown of the facility to thoroughly clean the manufacturing equipment. Sequencing entails a pre-planned order of production of feeds designed to direct drug carryover into subsequent feeds that will not result in unsafe drug contamination. Flushing involves taking a specific quantity of an ingredient, such as ground grain, and conveying it through the system to "flush" out any residual medicated feed from the previous medicated batches.

The most effective method, but not widely used in the feed industry, is cleaning. The thorough cleaning of the manufacturing equipment following every batch of medicated feed can only be accomplished by completely shutting down the facility. This is both impractical and not economically feasible. A complete manufacturing system cleanout is only recommended under high-risk situations such as, when handling a high potency form of a drug, when physical properties (e.g., adhesive strength, electrostatic properties) of drugs are such that sequencing and flushing are not sufficient, when the manufacturing equipment is inaccessible, or when liquid ingredients are used in the diet.

The feed industry typically uses sequencing because it minimizes the manufacturing system's downtime. The ordering sequence determines the likelihood of drug carryover into subsequent batches. Medicated feed containing the same drug(s) should be produced in sequence, with the batch with the highest drug level batched first. This production sequence would be followed by a non-medicated feed for the same animal species. In most medicated feed manufacturing facilities, sequencing will reduce drug carryover to a level that eliminates the

potential for consequent tissue residue in animals. However, sequencing may not reduce carryover to a sufficient level if deficiencies in CGMPs exist. If properly planned and executed, it may be the most cost-effective cleanout procedure. Periodic re-evaluation of the sequencing procedures should be performed to verify and validate effectiveness.

When flushing, ground corn at an approximate particle size of 600 microns is usually used as the flush material. As the flush material is conveyed through the manufacturing system, it comingles with residual medicated feed from previous batches, diluting the drug concentration to a safe level. The FDA recommends using between 5 and 10% of the mixer's total capacity as the quantity of flush material. Once the flush material has been used to clean the system, it must be properly identified and stored to prevent cross contamination. Flushing is not often used as a cleanout procedure considering the economic implications of having to store and/or dispose the flush material.

Feed Additives and Their Uses

Nicarbazin

Nicarbazin is a prophylactic that has been used since the 1950s to control coccidiosis in broilers (Ott et al., 1956; Newberne and Buck, 1957). Nicarbazin has two components: 4,6 dimethyl-2-pyrimidinol (HDP) and 4,4'-dinitrocarbanilide (DNC) (Figure 1.1; Conway and McKenzie, 2007). The function of HDP is to increase absorption in the intestinal tract, and DNC is considered the coccidiostat (Cuckler et al., 1955; Rogers et al., 1983).

The FDA classifies nicarbazin as a Category II - Type A medicated article, which can be fed to different animal species. In the United States, nicarbazin is approved for broilers at a concentration of 113.5 g/ton as a sole medication to prevent cecal and intestinal coccidiosis, and

up to 181.6 g/ton when combined with growth-promoting drugs for increased rate of weight gain and improved feed efficiency. Diets with nicarbazin concentrations of 113.5 g/ton have been proven effective in preventing coccidiosis in broilers (Ott et al., 1956; Rubin et al., 1956; McLoughlin and Chester, 1959; McLoughlin et al., 1960; Gardiner and McLoughlin, 1963). A withdrawal period of 4 days is used if nicarbazin is the only drug used and 4-5 days if nicarbazin is fed in combination with other feed additives. These withdrawal periods provide the time needed for the concentration of the active compound (i.e., DNC) to fall below 4 ppm, which is the maximum allowable concentration in uncooked chicken muscle, liver, skin, and kidneys (FDA-HHS, 1975).

Feeding nicarbazin-contaminated feed may be detrimental to laying birds, such as hens (Jones et al., 1990; Hughes et al., 1991; Chapman, 1994; VerCauteren et al., 2001) and geese (Johnston et al., 2002). Nicarbazin affects egg production, weight, and hatchability, as well as the appearance of the yolk (i.e., mottling) (Ott et al., 1956; Sherwood et al., 1956; Jones et al., 1990; Hughes et al., 1991; Chapman, 1994).

Regulatory agencies have set tolerance levels for nicarbazin residues in uncooked chicken muscle, liver, skin and kidneys. In the United States, the FDA established 4 ppm (FDA-HHS, 1975), whereas internationally, the Joint FAO/WHO Expert Committee on Food Additives (JECFA) fixed a maximum residue level (MRL) of 0.2 ppm (FAO/WHO, 1999). Neither regulatory agency has yet established tolerance levels in eggs. However, in the UK, the Veterinary Medicines Directorate has defined a differential action limit (DAL) of 0.1 ppm of nicarbazin in eggs. Animal food-products above these guidelines pose a risk to consumers through unsafe drug residue in the edible products from these animals. European researchers have reported that feed contaminated with 1.9 ppm and 2.4 ppm of nicarbazin was sufficient to

exceed both egg DAL and liver MRL respectively (Cannavan et al., 2000; Cannavan and Kennedy, 2000).

Monensin

Monensin is classified as a Category I - Type A medicated article by the FDA. Monensin is an ionophore produced by the *Streptomyces cinnamonensis* strain and is typically fed as the sodium salt. It is composed by 2-(5-ethyltetrahydro-5(tetrahydro-3-methyl-5-(tetrahydro-6-hydroxy-6-hydroxymethyl)-3,5-dimethyl-2H-pyran-2-yl-2-furyl)-2-furyl)9-hydroxy-β-methoxy-a,g,2,8-tetramethyl-1,6-diaoxaspiro(4,5)decane-7-butyric acid) (Figure 1.2; Conway and McKenzie, 2007).

In the United States, monensin is approved at different concentration levels for different animal species. It is approved for broilers at a concentration of 90-110 g/ton as a sole medication and when combined with growth promoting drugs to prevent coccidiosis. This same concentration is approved for replacement chickens (intended for use as caged layers) with a maximum use of 16 weeks. Monensin is also approved for use in cattle rations as a sole medication for the prevention and control of coccidiosis (0.14-0.42 mg/lb of bodyweight), to increase weight gain (25-400 g/ton), and to improve feed efficiency (5-400 g/ton). When combined with growth promoting drugs, it is approved for the prevention and control of coccidiosis (10-30 g/ton) and to improve feed efficiency (50-1,200 g/ton). The FDA requires withdrawal periods of up to seven days depending on the monensin use level, the animal species being fed, and if used as a sole medication or in combination with other feed additives. Withdrawal periods provide time for the concentration of the active compound to fall below regulatory guidelines. Feeding chickens does not require having a withdrawal period, although it may limit feed intake resulting in reduced weight gain. Tolerances for monensin residues in

cattle are set at 0.10 ppm for liver and 0.05 ppm for muscle, kidney and fat (FDA-HHS, 1975). No tolerance for monensin residue has been established for chicken.

Feeding monensin-contaminated feed may be detrimental to certain animal species. Compared to nicarbazin, monensin does not have major effects on layer birds' egg production. Researchers have observed that concentrations from 264-440 mg/kg of monensin will make laying birds cease egg production (EFSA, 2008). Broilers present reduced body weight gain when fed monensin concentrations of 250 mg/kg (EFSA, 2005), although reduced body weight can also be observed when no withdrawal period is implemented in the feeding program for chickens. Horses are the most susceptible to monensin (Matsuoka, 1976). Concentration as low as 33 mg/kg may cause temporary anorexia, and up to 121 mg/kg will cause toxicity and subsequent death (EFSA, 2008).

Accidental feeding of monensin-medicated feed to horses has been documented to result in toxicity and death (Stoker, 1975; Matsuoka, 1976; Nava, 1978; Beck and Harries, 1979; Whitlock et al., 1979; Muylle et al., 1981). A major source of exposure is usually a result of accidental contamination during formulation of horse rations (Doonan et al., 1989). It was reported by the European Food Safety Authority (2008) that horses that consume cattle feed (with a 33 mg/kg monensin concentration) develop anorexia, whereas the consumption of broiler feed (with a 121 mg/kg monensin concentration) would cause toxicity, resulting in death. Monensin toxicity side effects in horses include anorexia, colic pain, sweating, tachycardia, uneasiness, polyuria, progressive ataxia, recumbence, and death (EFSA, 2008). The high susceptibility of horses to monensin is associated with a deficiency in demethylating enzymes, which facilitate clearing monensin out of the animal's system. Nebbia et al. (2001) showed that horses have a low catalytic efficiency to demethylate monensin. For this reason, horse feeds

should never be batched immediately after the production of a medicated feed containing monensin, unless adequate measures are taken to prevent drug carryover.

The Purpose of Animal Drug Use

Disease Control and Prevention: Coccidiosis

Nicarbazin and monensin are both approved animal drugs used as an aid in the prevention and control of coccidian infections. Coccidia are a variety of single-celled, species-specific, parasitic organisms from the subkingdom Protozoa of the phylum Apicomplexa (Long, 1982). Chickens are challenged by the species of coccidia that belong to the genus *Eimeria*, specifically *E. acervulina*, *E. brunetti*, *E. maxima*, *E. mittis*, *E. necatrix*, *E. praecox*, and *E. tenella* (Conway and McKenzie, 2007). Although there are seven different *Eimeria* species specific to chickens, *E. acervulina*, *E. maxima*, and *E. tenella* are the most prevalent in the United States. Cattle are primarily challenged by *E. auburnensis*, *E. bovis* and *E. zuernii* (EFSA, 2008).

The *Eimeria's* life cycle typically lasts about 4-7 days. The cycle begins when a susceptible animal ingests an oocyst, a thick-walled capsule that protects four sporocysts within, which contain two sporozoites. The sporozoites are then released in the digestive tract and invade specific epithelial cells depending on which *Eimeria* species challenges the animal. The sporozites will then transform to a feeding stage called trophozoite in about 12-24 hours. Subsequently, the parasitic nucleus will divide by a process of asexual reproduction and be referred to as a schizont. The schizont will rupture when mature, and releases the merozoites that will invade other epithelial cells to repeat the development cycle of the parasite. Given a parasite's "self-limiting" nature, multiplication will cease before killing the host, and the remaining oocysts will be shed in the feces.

Coccidian organisms are opportunistic in nature, for the most part challenging young and/or immuno-compromised animals by invading the intestinal lining. The primary symptom of a coccidian infection is diarrhea, which may become bloody in acute cases. In chickens, symptoms such as poor weight gain, poor feed conversion, poor egg production, and death can be observed (Conway and McKenzie, 2007). Cattle may present symptoms such as straining, and severe weight loss (Kirkpatrick and Selk, 2007).

Coccidiosis is one of the most common diseases in the poultry industry and one that can have major economic implications to producers. Studies have shown that exposure to coccidia usually begins shortly after chicks are placed on litter (Long and Rowell 1975; Long et al., 1975; Long and Millard 1978; Braunius 1984), with the highest level of infection occurring between three and six weeks of age (Conway and McKenzie, 2007). Chapman (1999) observed that the development of the bird's full natural immunity is not attained until seven weeks of age. The latter is highly dependable on the anticoccidial drug used and the level of challenge during the first five to six weeks of growth.

The prevention and control of coccidiosis is dependent upon the integration of anticoccidial drugs to a comprehensive feeding program. Anticoccidial drug shuttle programs are used to reduce the organism's resistance to anticoccidial drugs. The poultry industry shuttle programs typically use a chemical (e.g., nicarbazin) in the starter ration, and an ionophore (e.g., monensin) in the grower ration (Eckman, 1993). Programs using an ionophore in the starter ration and a chemical in the grower ration have also proven to be successful. However, nicarbazin is not recommended for use in the grower phase, especially in warm environments, because it has been shown to reduce the bird's heat tolerance (Buys and Rasmussen, 1978; McDouglad and McQuisition, 1980; Keshavarz and McDougald, 1981).

Growth Promotants: Ionophores

Ionophores are lipid-soluble molecules, usually synthesized by microorganisms that transport ions across cell membranes (Callaway et al., 2003). Ionophores are primarily utilized for ruminant animals as growth promotants. The main purpose of ionophores is to bind ions and move them across membranes. Monensin is an ionophore that can exchange H^+ for either Na⁺ or K⁺ (Russell and Strobel, 1989).

The rumen environment contains high sodium and low potassium concentrations. To be able to uptake nutrients, bacteria in the rumen maintain an intracellular concentration opposite to that of the rumen (Chow and Russell, 1992). Since the potassium gradient is greater than the sodium gradient in the rumen, protons will accumulate inside the bacterium (Chow et al., 1994). This will create a cytoplasmic acidification inside the bacterium, by which the bacterium reacts by activating a sodium-potassium exchanger (Booth, 1985). The purpose of activating this sodium-potassium exchanger (Na⁺/K⁺ ATPase) is to move protons out of the cell and re-establish the ionic gradient between the bacterium and the rumen. This will limit the intracellular ATPs used for growth, leading to cellular death (Russell, 1987; Russell and Strobel, 1989).

Two of monensin's major effects when fed to ruminant animals are: 1.) an increase in propionate production, and 2.) a decreases methane production in the rumen environment (Dinius et al., 1976; Richardson, et al., 1976; Russell and Strobel, 1989). Since propionate is the most efficiently utilized volatile fatty acid (VFA), an increase in propionate production in the rumen increases the energy availability to the animal (Russell and Strobel, 1989). Richardson et al. (1976) concluded that a decrease in the acetate to propionate ratio (i.e., an increase in propionate production) increases gross energy available to the animal by 5.6%. A decrease in methane production in the rumen is also observed with the use of monensin as a feed additive

(Wedegaertner and Johnson, 1983; Russell and Strobel, 1989; Johnson and Johnson, 1995). Methane-producing bacteria, called methanogens, are not directly inhibited by monensin. Monensin inhibits the bacteria responsible for feeding nutrients (i.e., H₂) to this methanogens (Van Nevel and Demeyer, 1977; Dellinger and Ferry, 1984).

In addition to these two major effects, monensin also reduces acidosis in ruminal animals (Galyean and Owens, 1988). Acidification in the rumen is due to the accumulation of lactic acid as a result of the rapid fermentation of dietary carbohydrate (Nagaraja, et al., 1982; Burrin and Britton, 1986; Russell and Rychlik, 2001). Ruminal acidosis is associated with reduced feed intake, low feed efficiency, and cyclic feeding, as well as death in some cases. Monensin reduces acidosis by directly inhibiting the lactate-producing bacteria (Dennis, et al., 1981).

Research Objectives

- 1) To determine which manufacturing equipment is the major source of drug carryover.
- To evaluate which flush size adequately prevents drug carryover into subsequent batches of non-medicated feed.
- 3) To quantify the interrelationship between flush size and drug concentration.

Thesis Organization

To address the previously mentioned objectives, two experiments were conducted in the Feed Processing Research Center in the Department of Grain Science & Industry at Kansas State University. In Experiment 1, nicarbazin was used as the sole feed additive to manufacture medicated broiler feed. This was followed by a flush – five different flush sizes were evaluated. Subsequently, a non-medicated broiler diet was batched, conveyed through the manufacturing system and sampled at four different locations to quantify nicarbazin carryover.

In Experiment 2, monensin together with other growth promoting drugs was used to manufacture medicated cattle feed. This was followed by a flush – three different flush sizes were evaluated. A non-medicated horse diet was subsequently batched, conveyed through the manufacturing system and sampled at four different locations to quantify monensin carryover.

The mixer, drag conveyor discharge, bucket elevator discharge, and finished product bin discharge were chosen as sampling locations to determine which manufacturing equipment is the major source of drug carryover in this particular manufacturing system. Flush sizes, ranging from 1 to 20% of the mixer's capacity, were chosen to evaluate which flush size prevents drug carryover into subsequent batches of non-medicated feed. Three different drug concentrations were used to formulate the medicated cattle diet in Experiment 2 to be able to quantify the interrelationship between flush size and drug concentration.



Figure 1.1 Chemical structure of the components of nicarbazin (adapted from Conway and McKenzie, 2007)



Figure 1.2 Chemical structure of monensin (adapted from Conway and McKenzie, 2007)

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CHAPTER 2 - Evaluating Flushing Procedures to Prevent Nicarbazin Carryover during Medicated Feed Manufacturing

Feed manufacturers produce a broad range of feeds targeted to different animal species. Low production facilities generally only have one production line on which all the different animal species feeds are produced. When switching from one type of feed to the subsequent one, residues of the first batch will remain in the production line and end up in the subsequent batch. The transfer of residues from one batch to the subsequent batch is called carryover. Drug carryover is a form of feed contamination that results when an animal drug gets transferred from one production batch to the subsequent batch in unsafe levels. Varying among animal species and age, unsafe levels may have detrimental effects on the animals and may result in above tolerance residue levels in the edible tissue of food-producing animals. Drug carryover can occur during feed manufacturing, processing, or distribution. To prevent drug carryover during feed manufacturing, all equipment that comes in contact with an animal drug or medicated feed shall be subjected to effective cleanout procedures.

The FDA's CGMP regulations serve as guidelines for medicated feed manufacturers to ensure their products meet identity, strength, and quality standards. These regulations required the implementation of adequate procedures for all equipment used to manufacture medicated feed to avoid unsafe levels of drug contamination during feed manufacturing. The CGMP regulations require medicated feed manufacturers to use one or more of the approved cleanout procedure, such as cleaning, sequencing, and/or flushing to prevent unsafe contamination by drug carryover (HHS-FDA, 1976).

The most effective cleanout procedure is considered the thorough cleaning of the manufacturing system. However, sequencing and flushing are the most commonly used in the feed industry. Flushing is typically used in low production facilities. The FDA recommends using of 5 to 10 percent of the mixer's total capacity as the flush material. However, these quantities are based solely on recommendations with little data available to support this practice. Consequently, establishing an interrelationship between flush size and drug carryover is a practical necessity.

One of the most economically significant feed additives in the feed industry is nicarbazin. Nicarbazin is primarily used in the poultry industry to prevent coccidiosis in broilers. The FDA classifies nicarbazin as a Category II - Type A medicated article used for different animal species. This prophylactic additive has been in use as an aid in preventing outbreaks of cecal and intestinal coccidiosis in chickens since the 1950s (Ott et al., 1956; Newberne and Buck, 1957). Nicarbazin has two components: 4,6 di-methyl-2-pyrimidinol (HDP) and 4,4'-dinitrocarbanilide (DNC) (Figure 2.1; Conway and McKenzie, 2007). The function of HDP is to increase absorption in the intestinal tract, and DNC is considered the coccidiostat (Cuckler et al., 1955; Rogers et al., 1983).

In the United States, nicarbazin is approved for broilers at a concentration of 113.5 g/ton as a sole medication to prevent cecal and intestinal coccidiosis, and up to 181.6 g/ton when combined with growth-promoting drugs for increased rate of weight gain and improved feed efficiency. Diets with nicarbazin concentrations of 113.5 g/ton have proven effective in preventing coccidiosis in broilers (Ott et al., 1956; Rubin et al., 1956; McLoughlin and Chester, 1959; McLoughlin et al., 1960; Gardiner and McLoughlin, 1963). A withdrawal period of four to five days is required to allow for elimination of the drug from edible tissue. A withdrawal period

of four days is used if it is the only drug used and five days if it is fed in combination with other additives. This withdrawal period provides time needed for the concentration of active compounds to fall below 4 ppm, which is the maximum allowable concentration in uncooked chicken muscle, liver, skin and kidneys (HHS-FDA, 1975).

Coccidia are a variety of single-celled, species-specific, parasitic organisms from the subkingdom Protozoa of the phylum Apicomplexa (Long, 1982). Infection by coccidia parasites that produce clinical manifestations of disease is called coccidiosis. Chickens are challenged by the species of coccidia that belong to the genus *Eimeria*, specifically *E. acervulina*, *E. brunetti*, *E. maxima*, *E. mittis*, *E. necatrix*, *E. praecox*, and *E. tenella* (Conway and McKenzie, 2007). Although there are seven different *Eimeria* species specific to chickens, *E. acervulina*, *E. maxima*, and *E. tenella* are the most prevalent in the United States.

Feeding nicarbazin-contaminated feed may be detrimental to laying birds, such as hens (Jones et al., 1990; Hughes et al., 1991; Chapman, 1994; VerCauteren et al., 2001) and geese (Johnston et al., 2002). Nicarbazin affects egg production, weight, and hatchability, as well as the yolk appearance (i.e., mottling) (Ott et al., 1956; Sherwood et al., 1956; Jones et al., 1990; Hughes et al., 1991; Chapman, 1994).

Regulatory agencies have set tolerance levels for residues of nicarbazin in uncooked chicken muscle, liver, skin and kidneys. In the United States, the FDA established 4 ppm (HHS-FDA, 1975), whereas internationally, the Joint FAO/WHO Expert Committee on Food Additives (JECFA) fixed a maximum residue level (MRL) of 0.2 ppm (FAO/WHO, 1999). Neither regulatory agency has yet established tolerance levels in eggs. However, in the UK, the Veterinary Medicines Directorate has defined a differential action limit (DAL) of 0.1 ppm of nicarbazin in eggs. Animal food-products above these guidelines pose a risk to consumers

through unsafe drug residues in the edible products from these animals. European researchers have reported that feed contaminated with 2 ppm and 2.4 ppm of nicarbazin was sufficient to exceed both egg DAL and liver MRL respectively (Cannavan et al., 2000; Cannavan and Kennedy, 2000).

To reduce the risk of drug residue in animal food products, manufacturing facilities in the United States must use one or more of the cleanout procedures required by the FDA. Given that flushing is commonly used among the feed industry, the present study was designed to establish the interrelationship between the flush size and the level of nicarbazin carryover throughout a particular feed manufacturing system. This study may prove useful to determine which manufacturing equipment is the major source of drug carryover, as well as to develop strategies to prevent drug carryover during medicated feed manufacturing.

Material and Methods

Feed Manufacturing and Sampling procedures. Five flush size treatments were evaluated using the same nicarbazin level (125 ppm): 1) 2.5; 2) 5.0; 3) 10; 4) 15; and 5) 20% of the mixer's capacity. The study was conducted in the Feed Processing Research Center in the Department of Grain Science & Industry at Kansas State University. The feed manufacturing system included the following major equipment: a 454.5 kg (1,000 lb) capacity drop bottom paddle mixer (Forberg, Hegdalveien, Larvik, Norway); a 3.79 kg/s (8.33 lb/s) capacity drag conveyor (Esmueller, Laurel, MS); a 19.96 MT/h (44,000 lb/h) capacity bucket elevator (Hayes & Stolz, Forth Worth, Texas); a 11-position electric distributor; and a 5.44 MT capacity finished product bin (Figure 2.2).

The manufacturing equipment was thoroughly cleaned prior to the start of the study and in between treatments. To clean each piece of equipment, Lockout/Tagout procedures were

followed to comply with the Occupational Safety & Health Administration's (OSHA) regulations. First, the complete system was shut down and the corresponding equipment was LOTO. The paddle mixer was cleaned using compressed air and a scraper to remove the excess of material buildup from the walls and paddles. Subsequently, a vacuum cleaner was used to vacuum the scrap material. Due to the inaccessibility of the drag conveyor and given its self-cleaning characteristics, the drag conveyor was clean by simply letting it run with no load for five minutes. To clean the bucket elevator, the boot section panels were removed and the whole boot section was vacuumed out. Also, the spout that transfers the material into the finished product bin was opened and scraped to remove material buildup. To clean the finished product bin, a rubber mallet was used to hit the bin and dislodged any material remaining on the bin walls and on the bin bottom. All of this material buildup excess was collected from the finished product bin and disposed off. The sampling probes were also cleaned prior and after each treatment. The multi-port sample probe (Burrows Equipment Co., Evanston, IL) and a plastic scoop were cleaned using a damped clean cloth and then dried using compressed air.

To prepare a batch, macro-ingredients were first measured and added into the mixer using a batching system. After that, minor- and micro-ingredients, as well as the feed additive (i.e., nicarbazin) were hand weighed and added to the mixer at the same location across treatments to ensure consistency. The mix cycles included a dry mix and a wet mix. After the addition of all the dry ingredients, the dry mix began and continued for 120 s. The wet mix began immediately after and continued for 180 s while soybean oil was being pumped into the mixer through internal spray nozzles.

Two 454.5 kg (1,000 lb) batches of the medicated diet (Table 2.1) were prepared prior to the start of the study using Nicarb® 25%. Medicated feed was prepared in excess and re-used to
ensure the same nicarbazin level in all the treatments and to replace loss in sampling and carryover. After the mix cycles, each batch was discharged from the mixer and conveyed by the drag conveyor into a bucket elevator, and then distributed into the finished product bin. After the complete transfer of both batches into the finished product bin, the medicated diet was bagged in 22.7 kg (50 lb) bags and set aside. The system was then thoroughly cleaned as previously described.

To contaminate the system, 454.5 kg (1,000 lb) of the previously prepared medicated diet was added to mixer and re-mixed for 120 s. A composite sample was then taken of six different sampled locations in the mixer using the multi-port sample probe. The medicated diet was then discharged from the mixer and conveyed by the drag conveyor into a bucket elevator, and then distributed into the finished product bin. After the medicated diet transferred completely into the finished product bin, it was bagged in 22.7 kg (50 lb) bags and set aside to re-use later.

Corn was ground to an approximate particle size of 500 microns using a hammer mill (Jacobson, Minneapolis, MN) with a 0.32 cm (1/8 inch) diameter screen, and used as the flushing material. The quantity of flush material used for each treatment was weighed out using the batching system and mixed for 120 s. After mixing, the flush material was discharged from the mixer, conveyed by the drag conveyor into a bucket elevator, and then distributed into the finished product bin. Once the flush had transferred completely into the finished product bin, it was bagged in 22.7 kg bag(s). A composite sample was collected from bag(s) using the multiport sample probe.

Following the flush, a 227.3 kg (500 lb) non-medicated diet (Table 2.1) was batched. After the mix cycles, a composite sample was taken of six different sampled locations in the mixer using the multi-port sample probe. The non-mediated diet was also sampled at the drag

conveyor and bucket elevator discharges as it was being conveyed through the system. Composite samples for the drag conveyor and bucket elevator were collected at 15, 30 and 45 s after the non-medicated diet started discharging the equipment. After the complete transfer of the non-medicated diet, it was placed in 22.7 kg (50 lb) bags. A composite sample was collected from bags 1-9 using the multi-port sample probe. The system was then thoroughly cleaned as previously described to start the next treatment. Treatments were randomly assigned an order for each of the three replications.

All composite samples from the mixer, drag conveyor discharge, bucket elevator discharge, and finished product were split using a riffler, and approximately 227.3 g (0.50 lb) were collected for nicarbazin analysis.

Laboratory Analysis. Samples were sent to a commercial laboratory (Eurofins Laboratories, Portage, MI) for nicarbazin analysis immediately after the study. Analysis was performed using the quantitation of nicarbazin in medicated feed articles by HPLC using Elanco B05511. Nicarbazin was extracted from 40 g of the medicated feed article using 200 mL of 80:20 ACN:Water. An aliquot of the extract was filtered and assayed using reverse-phase isocratic method, which measures the DNC moiety at a wave length of 340 nm. Nicarbazin concentration was reported based on an assumed equivalence of DNC and Nicarbazin. The lowest detection limit in the feed samples for the laboratory's nicarbazin assays was 1 ppm.

Statistical Analysis. The study was designed as a 5 × 4 factorial (flush size × sampling location) arrangement of treatments. GLM procedures of the SAS Institute (SAS Institute, 2003) were used to detect significant differences (P < 0.05) between treatments. When significant differences were detected, least square means were used for means separation at $\alpha = 0.05$.

Results and Discussion

Drug levels of samples taken at the mixer for the medicated diets (Figure 2.3; Table 2.2) were very close to those formulated. Regulatory agencies set drug assay limits for each approved drug. Nicarbazin's assay limit is 85-115 percent of the labeled amount (125 ppm) for a Type B or Type C medicated feed, resulting in a range of 106.3-143.8 ppm. All treatments were within nicarbazin assays limits for this study. Laboratory drug assays' accuracy was \pm 0.01 ppm, with values less than 1 ppm considered non-detectable levels of nicarbazin in feed samples.

The need of accurate drug levels in medicated feed is crucial. Inaccurate inclusion of a drug into medicated diet can cause the drug to be ineffective or detrimental to the animal. Diets formulated with a nicarbazin concentration between 50-200 mg/kg allows for good growth and feed conversion in broilers. However, concentrations between 400-600 mg/kg will decrease the bird's body weight gain and lower its feed efficiency, and concentrations up to 1,500 mg/kg will increase the mortality rate. Laying birds are the most susceptible to nicarbazin. A decrease in hatchability and egg shell pigmentation can be observed when laying hens are fed contaminated diets with nicarbazin levels as low as 50 mg/kg (Jones, 1990). Concentrations of nicarbazin of up to 125 mg/kg reduce the hen's egg production, as well as affecting the egg's weight and yolk appearance (Jones et al., 1990). Booth and McDonald (1982) observed that nicarbazin caused a 65% egg production reduction, and completely inhibited the egg hatchability when fed at a concentration of 125 mg/kg.

Table 2.2 shows the effect of flush size on nicarbazin carryover in sampling locations throughout the feed manufacturing process. It was observed that as the quantity of flush material used to flush the system increased, the nicarbazin concentration decreased (Figure 2.4). This demonstrates a dilution effect as a result of an increase in flush size used to cleanout the

manufacturing system. These drug concentrations represent the amount of carryover to the subsequent batches if sequencing was used as the cleanout procedure. However, none of the treatments would exceed drug residue guidelines because, due to economical implications, feed manufacturers generally prepare no less than 454.55 kg (1,000 lb) of feed per batch. This would set the nicarbazin concentrations for all treatments below the guidelines for feed. European researchers have reported that feed contaminated with 2.0 ppm and 2.5 ppm of nicarbazin was sufficient to exceed both egg DAL and liver MRL respectively (Cannavan et al., 2000; Cannavan and Kennedy, 2000).

Feed manufacturing equipment can influence the amount of drug carryover into subsequent batches. To determine which manufacturing equipment is the major source of drug carryover in this particular feed manufacturing system, the following equipments was evaluated: mixer, drag conveyor, bucket elevator, and the finished product bin. Drug concentrations in sampling locations across treatments for the non-medicated diets were not significant (P > 0.05), except for the sample taken at the bucket elevators discharge for Treatment 5. The mixer and drag conveyor showed non-detectable nicarbazin carryover levels. However, the bucket elevator and the finished product bin showed carryover, although neither exceeded residue guidelines proposed by researchers (Cannavan et al., 2000; Cannavan and Kennedy, 2000).

Table 2.2 also shows nicarbazin carryover in the bucket elevator across treatments. Treatment 1 showed a higher value of nicarbazin carryover than Treatments 2, 3, and 4, while Treatment 5 differed (P < 0.05) from the rest showing zero drug carryover. This drug carryover pattern can be explained by dilution. As the flush size used to flush the manufacturing system increased, dilution of the residue's drug concentration increased. Bucket elevators do not empty completely because of the bucket elevator's boot section design. Reduction, or possible

elimination, of drug carryover can be achieved by using a self-cleaning boot section. Selfcleaning boot sections are designed with a reduced bucket-to-base clearance for minimal material residue, hence a reduction in drug carryover. Wear in conveying systems can also become a source for drug carryover, as reduced flow in specific areas tends to accumulate the material being conveyed.

The finished product bin showed higher values compared to the rest of the equipment evaluated in this study. Most of the drug carryover observed in the finished product bin may be attributed to nicarbazin's physicochemical characteristics. Nicarbazin poses a high electrostatic potential and consequently has a tendency to cling to the bin walls. Characteristics such as product moisture and environmental conditions may also cause adhesion of the drug to the bin walls. When comparing nicarbazin carryover in the finished product bin across treatments, there was no significant difference across treatments. However, both Treatments 2 and 3 exceed the egg DAL of 2.0 ppm.

Table 2.3 shows the calculated nicarbazin carryover in sampling location throughout the feed manufacturing process. Treatments 1 and 4 showed a distinctive drug carryover sequence with most of the carryover observed in the bucket elevator, whereas Treatments 2, 3, and 5 have the highest nicarbazin carryover in the finished product bin. Table 2.3 clearly demonstrates that the finished product bin is the equipment in this particular manufacturing system that produced the highest nicarbazin carryover (Treatment 2 - 1.5 ppm).

There was no significant interaction (P > 0.05) found between flush sizes and sampling location (Table 2.4). However, flush size and sampling location were a significant source of variation in drug carryover.

Conclusions

In conclusion, a suitable interrelationship between the flush size and the level of nicarbazin carryover throughout a feed manufacturing system was established. All of the flushes prevented significant carryover. The use of a 2.5% flush size proved more effective than a 5% and 10% flush size, and almost as effective as a 15% and 20% flush size. Also, the bucket elevator and the finished product bin were identified among the feed manufacturing equipment as the major sources of nicarbazin carryover in this particular manufacturing system.

Given that this data is only valid for this particular manufacturing system, further research is necessary to validate this study and to evaluate different flushing cleanout procedures, such as using double flushing. In addition, different manufacturing equipment should be addressed as well as different manufacturing process flows. Equipment such as single discharge mixer, ribbon mixers, screw conveyors, pellet mills, coolers, among others, should be evaluated as sources of drug carryover. Different manufacturing process flows should also be studied to evaluate the equipment's probability of becoming a source of drug carryover with respect to its location in the manufacturing process.



Figure 2.1 Chemical structure of the components of nicarbazin (adapted from Conway and

McKenzie, 2007)



Figure 2.2 Manufacturing flow process used in Experiment 1



Figure 2.3 Nicarbazin concentrations in medicated diets sampled at the mixer for each flush

treatment



Figure 2.4 Nicarbazin concentrations in the flush material sampled at the finished product bin

for each flush treatment



Figure 2.5 Nicarbazin concentrations in the non-medicated diets at different sampling location

for each flush treatment

	Medicated	Non-Medicated	
Ingredients	0/0		
Major-ingredient(s)			
Corn	68.89	68.94	
Soybean meal	20.40	20.40	
Minor-ingredient(s)			
Fish meal	5.50	5.50	
Micro-ingredient(s)			
Di-calcium phosphate	0.51	0.51	
Limestone	0.58	0.58	
Salt	0.33	0.33	
DL-Methionine	0.31	0.31	
Lysine	0.18	0.18	
Poultry Vit/Min premix	0.25	0.25	
Liquid-ingredient(s)			
Soybean oil	3.00	3.00	
Feed additive(s)			
Nicarb® 25%	0.05	0.00	
Total	100.00	100.00	

 Table 2.1 Diets used in Experiment 1 to evaluate nicarbazin carryover

	Flush treatments, % of mixer capacity ²					
Type of batch	2.5	5.0	10	15	20	SEM ³
Sampling location	ppm ¹					
Medicated diet						
Mixer	117.3 ^a	111.7 ^a	111.5 ^a	120.3 ^a	114.3 ^a	8.09
Flush						
Finished product bin	19.2 ^b	14.8 ^{b,c}	12.0 ^{b,c}	6.5 ^c	5.6 ^c	2.01
Non-medicated diet						
Mixer	0.0 ^{d,x}	0.4 ^{d,x}	0.0 ^{d,x}	0.0 ^{d,x}	0.0 ^{d,x}	0.19
Drag conveyor	0.0 ^{d,x}	0.4 ^{d,x}	0.0 ^{d,x}	0.0 ^{d,x}	0.0 ^{d,x}	0.17
Bucket elevator	$1.4^{e,x}$	$1.0^{e,x}$	0.8 ^{e,x}	0.8 ^{e,x}	0.0 ^{d,y}	0.33
Finished product bin	1.8 ^{e,x}	2.1 ^{e,x}	2.2 ^{f,x}	1.4 ^{e,x}	1.5 ^{e,x}	0.31

Table 2.2 Effects of flush size on nicarbazin carryover in sampling locations throughout the feed manufacturing process

¹ Nicarbazin carryover concentrations are means (n = 3) in ppm, with limit of detection ± 1 ppm

² Forberg 454.5 kg (1,000 lb) capacity drop bottom paddle mixer

³ Pooled SEM (n = 3) of the five flush size treatments by rows

^a Means within the row with different superscript differ (P < 0.05)

^{b-c} Means within the row with different superscript differ (P < 0.05)

^{d-f} Means within the non-medicated diet columns with different superscript differ (P < 0.05)

^{x-y} Means within the non-medicated diet rows with different superscript differ (P < 0.05)

	Flush Treatments, % of mixer capacity ¹				
Type of batch	2.5	5.0	10	15	20
Sampling location			ppm ²		
Non-medicated diet					
Mixer	0.0	0.4	0.0	0.0	0.0
Drag conveyor	0.0	0.0	0.0	0.0	0.0
Bucket elevator	1.4	0.6	0.8	0.8	0.0
Finished product bin	0.4	1.5	1.4	0.6	1.5
Total nicarbazin carryover	1.8	2.1	2.2	1.4	1.5

Table 2.3 Calculated nicarbazin carryover in sampling location throughout the feed

 manufacturing process

¹ Forberg 454.5 kg (1,000 lb) capacity drop bottom paddle mixer

² Nicarbazin concentrations are calculated differences between two locations within treatments

Table 2.4 Pair-wise comparison of sampling location and flush size of non-medicated

 diet treatments in Experiment 1

Sources of Variation	$P < 0.05^{1}$
Flush size	0.0185
Sampling location	< 0.0001
Flush size × Sampling location	0.3110

¹Significant differences detected using least square means for mean separation at $\alpha = 0.05$

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CHAPTER 3 - Evaluating Flushing Procedures to Prevent Monensin Carryover during Medicated Feed Manufacturing

Feed manufacturers produce a broad range of feeds targeted to different animal species. When facilities switch from one type of feed to the next, residues of the first batch will remain in the production line and end up in the subsequent batch. The transfer of residues from one batch to the subsequent batch is called carryover. Drug carryover is a form of feed contamination that results when an animal drug gets transferred from one production batch to the subsequent batch in unsafe levels. Drug carryover is undesirable given that it may have detrimental effects on the animals and may result in above tolerance residue levels in the edible tissue of food-producing animals. Drug carryover can occur during feed manufacturing, processing, or distribution. To prevent drug carryover during feed manufacturing, all equipment that comes in contact with an animal drug or medicated feed shall be subjected to effective cleanout procedures.

The FDA's CGMP regulations serve as guidelines for medicated feed manufacturers to ensure their products meet identity, strength, and quality standards. These regulations required the implementation of adequate procedures for all equipment used to manufacture medicated feed to avoid unsafe levels of drug contamination during feed manufacturing. The CGMP regulations require medicated feed manufacturers to use one or more of the approved cleanout procedure, such as cleaning, sequencing, and/or flushing to prevent unsafe contamination by drug carryover (HHS-FDA, 1976).

The most effective cleanout procedure is considered the thorough cleaning of the manufacturing system. However, sequencing and flushing are the most commonly used in the feed industry. Flushing is typically used in low production facilities, which generally only have

one production line on which all the different animal species feeds are produced. The FDA recommends using of 5 to 10 percent of the mixer's total capacity as the flush material. However, these quantities are based solely on recommendations with little data available to support this practice. Consequently, establishing an interrelationship between flush size and drug carryover is a practical necessity.

One of the most economically significant feed additives in the feed industry is monensin. Monensin is a feed additive approved for use in animal feed. The FDA classifies monensin as a Category I - Type A medicated article used for different animal species. Monensin is an ionophore produced by the *Streptomyces cinnamonensis* strain. Typically fed as the sodium salt, it is composed by 2-(5-ethyltetrahydro-5(tetrahydro-3-methyl-5-(tetrahydro-6-hydroxy-6hydroxymethyl)-3,5-dimethyl-2H-pyran-2-yl-2-furyl)-2-furyl)9-hydroxy-β-methoxy-a,g,2,8tetramethyl-1,6-diaoxaspiro(4,5)decane-7-butyric acid) (Figure 3.1; Conway and McKenzie, 2007).

In the United States, monensin is approved for different animal species, each at different concentration levels. When monensin is used in broiler diets as the sole medication or in combination with growth promoting drugs, it is approved to be included at a concentration of 90-110 g/ton. This same concentration is approved for replacement chickens (intended for use as caged layers) with a maximum use of 16 weeks. The FDA also approves the use of monensin in cattle rations. If used as the sole medication, it prevents coccidiosis (0.14-0.42 mg/lb of bodyweight), increases weight gain (25-400 g/ton), and improves feed efficiency (5-400 g/ton). When combined with growth promoting drugs, it prevents coccidiosis (10-30 g/ton) and improves feed efficiency (50-1,200 g/ton). Withdrawal periods when using monensin can be up to seven days, depending on the monensin use level, the animal specie being fed, and if

monensin is used as a sole medication or in combination with other feed additives. Withdrawal periods provide time for the concentration of active compound to fall below regulatory guidelines. Feeding chickens does not require having a withdrawal period, although it may limit feed intake resulting in reduced weight gain. Tolerances for monensin residues in cattle are set at 0.10 ppm for liver and 0.05 ppm for muscle, kidneys and fat (FDA-HHS, 1975). No tolerance for monensin residue has been established in chickens.

Coccidia are a variety of single-celled, species-specific, parasitic organisms from the subkingdom Protozoa of the phylum Apicomplexa (Long, 1982). Infection by coccidia parasites that produce clinical manifestations of disease is called coccidiosis. Chickens are challenged by the species of coccidia that belong to the genus *Eimeria*, specifically *E. acervulina*, *E. maxima*, and *E. tenella* (Conway and McKenzie, 2007). Cattle are primarily challenged by *E. bovis* and *E. zuernii* (EFSA, 2008).

Feeding monensin-contaminated feed may be detrimental to certain animal species. Compared to nicarbazin, monensin does not have a major effect on a layer bird's egg production, although researchers have observed that monensin concentrations between 264-440 mg/kg will cause layer birds to cease egg production (EFSA, 2008). Broilers present reduced body weight gain when fed diets that have a monensin concentration of 250 mg/kg (EFSA, 2005). Horses are the most susceptible to monensin (Matsuoka, 1976). Concentrations as low as 33 mg/kg may cause temporary anorexia and concentrations up to 121 mg/kg will cause toxicity and subsequent death (EFSA, 2008).

Accidental feeding of monensin-medicated feed to horses has been documented to result in toxicity and death (Stoker, 1975; Matsuoka, 1976; Nava et al., 1978; Beck et al., 1979; Whitlock et al., 1979; Muylle et al., 1981; Amend et al., 1985). Accidental feeding is a result of

drug carryover during feed manufacturing (Doonan et al., 1989). It was reported by the European Food Safety Authority (2008) that horses that consume cattle feed (with a concentration of 33 mg/kg of monensin) would develop anorexia, whereas the consumption of broiler feed (with a concentration of 121 mg/kg of monensin) would cause toxicity, resulting in death. Monensin toxicity side effects in horses include anorexia, colic pain, sweating, tachycardia, uneasiness, polyuria, progressive ataxia, recumbence, and death (EFSA, 2008). The high susceptibility of horses to monensin is associated with a relative deficiency in demethylating enzymes, which facilitate clearing monensin out of the animal's system. Nebbia et al. (2001) showed that horses have a low catalytic efficiency to demethylate monensin. For this reason, horse feeds should never be batched immediately after feed that contains monensin, unless adequate measures were taken to prevent drug carryover.

To reduce the risk of drug residue in animal food-products, manufacturing facilities in the United States generally use one or more of the cleanout procedures (i.e., cleaning, sequencing, and/or flushing) required by the FDA. Flushing is commonly used among the feed industry. Generally, 5 to 10 percent of the mixer's total capacity is used as the flush material. The present study was designed to establish the relationship between the flush size and the level of monensin carryover throughout a feed manufacturing system. This study may prove useful to establish critical control points throughout the feed manufacturing process, as well as to develop strategies to prevent drug carryover during medicated feed manufacturing.

Materials and Methods

Feed Manufacturing and Sampling procedures. Three flush size treatments (% of the mixer's capacity) were evaluated using three different Rumensin® 80 drug levels (100, 600, and 1,200 g/ton). Treatments were: 1) 1.0/100; 2) 1.0/600; 3) 1.0/1,200 4) 2.5/100; 5) 2.5/600; 6)

2.5/1,200 7) 5.0/100; 8) 5.0/600; and 9) 5.0/1,200. The study was conducted in the Feed Processing Research Center in the Department of Grain Science & Industry at Kansas State University. The feed manufacturing system included the following major equipment: a 454.5 kg (1,000 lb) capacity drop bottom paddle mixer (Forberg, Hegdalveien, Larvik, Norway); a 3.79 kg/s (8.33 lb/s) capacity drag conveyor (Esmueller, Laurel, MS); a 19.96 MT/h (44,000 lb/h) capacity bucket elevator (Hayes & Stolz, Forth Worth, Texas); a 11-position electric distributor; and a 5.44 MT capacity finished product bin (Figure 3.2).

The manufacturing equipment was thoroughly cleaned prior to the start of the study and in between treatments. To clean each piece of equipment, Lockout/Tagout procedures were followed to comply with the Occupational Safety & Health Administration's (OSHA) regulations. First, the complete system was shut down and the corresponding equipment was LOTO. The paddle mixer was cleaned using compressed air and a scraper to remove the excess of material buildup from the walls and paddles. Subsequently, a vacuum cleaner was used to vacuum the scrap material. Due to the inaccessibility of the drag conveyor and given its selfcleaning characteristics, the drag conveyor was clean by simply letting it run with no load for five minutes. To clean the bucket elevator, the boot section panels were removed and the whole boot section was vacuumed out. Also, the spout that transfers the material into the finished product bin was opened and scraped to remove material buildup. To clean the finished product bin, a rubber mallet was used to hit the bin and dislodged any material remaining on the bin walls and on the bin bottom. All of this material buildup excess was collected from the finished product bin and disposed off. The sampling probes were also cleaned prior and after each treatment. The multi-port sample probe (Burrows Equipment Co., Evanston, IL) and a plastic scoop were cleaned using a damped clean cloth and then dried using compressed air.

To prepare a batch, macro-ingredients were first measured and added into the mixer using a batching system. After that, minor- and micro-ingredients, as well as the feed additive (i.e., nicarbazin) were hand weighed and added to the mixer at the same location across treatments to ensure consistency. The mix cycles included a dry mix and a wet mix. After the addition of all the dry ingredients, the dry mix began and continued for 120 s. The wet mix began immediately after and continued for 180 s while soybean oil was being pumped into the mixer through internal spray nozzles.

Two 340.9 kg (750 lb) batches of the medicated diet (Table 3.1) were prepared prior to the start of the study using Rumensin® 80 for each drug level (100, 600, 1,200 g/ton). Medicated feed was prepared in excess and re-used to ensure the same nicarbazin level in all the treatments and to replace loss in sampling and carryover. After the mix cycles, each batch was discharged from the mixer and conveyed by the drag conveyor into a bucket elevator then distributed into the finished product bin. After the complete transfer of both batches into the finished product bin, the medicated diet was bagged in 22.7 kg (50 lb) bags and set aside. The system was then thoroughly cleaned as previously described.

To contaminate the system, 454.5 kg (1,000 lb) of the previously prepared medicated diet was added to mixer and re-mixed for 120 s. A composite sample was then taken of six different locations in the mixer using the multi-port sample probe. The medicated diet was then discharged from the mixer and conveyed by the drag conveyor into a bucket elevator, and then distributed into the finished product bin. After the medicated diet transferred completely into the finished product bin, it was bagged in 22.7 kg (50 lb) bags and set aside to re-use later.

Corn was ground to an approximate particle size of 500 microns using a hammer mill (Jacobson, Minneapolis, MN) with a 0.32 cm (1/8 inch) diameter screen, and used as the flushing

material. The quantity of flush material used for each treatment was weighed out using the batching system and mixed for 120 s. After mixing, the flush material was discharged from the mixer, conveyed by the drag conveyor into a bucket elevator, and then distributed into the finished product bin. Once the flush had transferred completely into the finished product bin, it was bagged in 22.7 kg bag(s). A composite sample was collected from bags 1-9 using the multiport sample probe.

Following the flush, a 227.3 kg (500 lb) non-medicated diet (Table 3.1) was batched. After the mix cycles, a composite sample was taken of six different locations in the mixer using the multi-port sample probe. The non-mediated diet was also sampled at the drag conveyor and bucket elevator discharges as it was being conveyed through the system. Composite samples for the drag conveyor and bucket elevator were collected at 15, 30 and 45 s after the non-medicated diet started discharging the equipment. After the complete transfer of the non-medicated diet, it was placed in 22.7 kg (50 lb) bags and sampled. The system was then thoroughly cleaned as previously described to start the next treatment. Treatments were randomly assigned an order for each of the two replications.

All composite samples from the mixer, drag conveyor discharge, bucket elevator discharge, and finished product were split using a riffler, and approximately 227.3 g (0.50 lb) were collected for nicarbazin analysis.

Laboratory Analysis. Samples were sent to a commercial laboratory (Trilogy Analytical Laboratory, Washington, MO) for monensin analysis. This was performed using the AOAC Official Method 997.04. Samples were extracted as follows: 5 g of the sample was added to 200 ml extraction solution (90 + 10 methanol/water) and shook for 1 hour. Samples were then filtered

and injected onto the HPLC. The lowest detection limits in the feed samples for the laboratory's monensin assays was 1 ppm.

Statistical Analysis. The study was designed as a $3 \times 4 \times 3$ factorial (flush size \times sampling location \times drug level) arrangement of treatments. GLM procedures of the SAS Institute (SAS Institute, 2003) were used to detect significance differences (P < 0.05) between treatments. When significant differences were detected, least squares means was used for means separation at $\alpha = 0.05$.

Results and Discussion

Drug levels of samples taken at the mixer for the medicated diet (Figure 3.3; Table 3.3) were very close to those formulated. Regulatory agencies set drug assay limits for the production of medicated feed. Monensin's assay limit is 85-115 percent of the labeled amount (100, 600, and 1,200 g/ton), resulting in a range of 77.4-104.7, 464.1-627.9 and 928.2-1,255.8 ppm, respectively. Only Treatments 1, 2 and 5 were slightly outside of their respective range (Trt 1=105.9 ppm; Trt 3=125.2 ppm; Trt 5=677.0 ppm). This might be due to laboratory drug assays sampling accuracy. Laboratory drug assays' accuracy was \pm 0.01 ppm, with values less than 1 ppm considered as non-detectable levels of monensin in feed samples.

The need of accurate drug levels in medicated feed is crucial because an inaccurate inclusion of a drug into medicated diet can cause the drug to be ineffective or detrimental to the animal. Laying birds feed on diets that have monensin concentrations between 264-440 mg/kg will cause the birds to cease production and their feed intake would be greatly depressed (EFSA, 2008). Broiler fed monensin concentrations of 250 mg/kg may present reduced body weight gain (EFSA, 2008), although reduced body weight can also be observed when no withdrawal period is implemented in the feeding program for chickens. Non-targeted animals, such as horses, are the

most susceptible to monensin (Matsuoka, 1976). Concentration as lows as 33 mg/kg may cause temporary anorexia, and concentrations up to 121 mg/kg will cause toxicity and subsequent death (EFSA, 2008).

Table 3.3 shows the effect of flush size on monensin carryover in sampling location and formulated monensin drug level throughout the feed manufacturing process. It was observed that as the quantity of flush material used to flush the system increased, the monensin concentration decreased (Figure 3.4). This dilution effect is a result of an increase in flush size used to cleanout the manufacturing system. These drug concentrations represent the amount of carryover to subsequent batches if sequencing was used as the cleanout procedure. However, none of the treatments exceeded drug residue guidelines because, due to economical implications, feed manufacturers generally prepare no less than 454.55 kg (1,000 lb) of feed per batch. This would set the monensin concentrations for all treatments below the guidelines for feed.

The equipment used to manufacture feed can influence the amount of drug carryover into subsequent batches. To determine which manufacturing equipment is the major source of drug carryover in this particular feed manufacturing system, the following equipment was evaluated: mixer, drag conveyor, bucket elevator, and the finished product bin. Figure 3.3 showed that the data was mostly consist among the three formulated drug levels. The sampling location among the three formulated drug levels that had the least carryover was the drag conveyor, with the finished product bin being the major source of drug carryover. None of the treatments exceeded tolerance limits (33 ppm) that may have detrimental effects to horses.

Monensin concentrations in non-medicated diets at each sampling location did not differ (P > 0.05) between Treatments 1-3 (100 g/ton). These same treatments presented zero carryover at the mixer and drag conveyor. There was a slight amount of carryover in the bucket elevator,

with the greatest amount of carryover in the finished product. Treatment 1 showed a higher monensin concentration followed by Treatment 2 and then Treatment 3. Dilution of the residue's drug concentration can explain this carryover pattern. As the quantity of flush material used to flush the system increases, dilution of the feed residue's drug concentration increases. Monensin concentrations in non-medicated diets for Treatments 4-6 (600 g/ton) differ significantly (P <0.05) at the bucket elevator and finished product bin. This drug level (600 g/ton) was enough to cause carryover in all sampling locations. In all of the equipment that presented carryover, the 1% flush size had the highest carryover, followed by 2.5%, and then 5%. These treatments followed the same dilution pattern as Treatments 1-3. Monensin concentrations in non-medicated diets for Treatments 7-9 (1,200 g/ton) did differ (P < 0.05) on all the sampling locations among those treatments. These treatments presented carryover in all sampling locations, with Treatments 8 and 9 showing a higher overall monensin concentration than Treatment 7. Laboratory assay accuracy might have been the cause of this discrepancy.

Given that drop bottom mixers and drag conveyors are equipment that empty thoroughly and are not identified as equipment with possible areas for residue accumulation, the carryover present in Treatments 4-9 might be because of the high level of drug used to formulate the diet. In the case of the bucket elevators, some bucket elevators do not empty completely because of the design of the boot section. A reduction, or possible elimination, of drug carryover can be achieved by using a self-cleaning boot section. Self-cleaning boot sections are designed with a reduced bucket-to-base clearance for minimal material residue, hence a reduction in drug carryover. Wear in conveying systems can also become a source of drug carryover, as reduced flow in specific areas tends to accumulate the material being conveyed. Most of the drug carryover observed in the finished product bin may be attributed to monensin's physicochemical

characteristics, as well as product moisture and environmental conditions that may have caused adhesion of the drug to the bin walls.

Table 3.4 shows the calculated monensin carryover in sampling location of all treatments. Treatments 1, 4, and 6 showed a distinctive drug carryover sequence with most of the carryover observed in the bucket elevator, whereas Treatments 2, 3, 5, 8, and 9 have the highest monensin carryover in the finished product bin. Table 3.4 clearly demonstrates that the bucket elevator and the finished product bin are the equipment in this particular manufacturing system that produced the highest nicarbazin carryover.

There was no significant interaction (P > 0.05) found between sampling location and flush size, and flush sizes and drug level (Table 3.5). However, sampling location, flush size, drug level, and sampling location and drug level interaction were significant sources of variation in drug carryover.

Conclusions

In conclusion, a suitable interrelationship between the flush size and the level of monensin carryover throughout a feed manufacturing system was established. The use of a 1.0% flush size proved effective, as did the rest of the flush sizes. Consequently, all the flushes prevented significant carryover and none exceeded monensin tolerance limit (33 ppm) that may cause detrimental effect to horses. Also, the bucket elevator and the finished product bin were identified among the feed manufacturing equipment as the major sources of monensin carryover in this particular manufacturing system.

Given that this data is only valid for this particular manufacturing system, further research is necessary to validate this study and to evaluate different flushing cleanout procedures, such as using double flushing. In addition, different manufacturing equipment should be

addressed as well as different manufacturing process flows. Equipment such as single discharge mixer, ribbon mixers, screw conveyors, pellet mills, coolers, among others, should be evaluated as sources of drug carryover. Different manufacturing process flows should also be studied to evaluate the equipment's probability of becoming a source of drug carryover with respect to its location in the manufacturing process.



Figure 3.1 Chemical structure of monensin (adapted from Conway and McKenzie, 2007)



Figure 3.2 Experiment 2 manufacturing process flow



Figure 3.3 Monensin concentrations in the medicated diets sampled at the mixer for each flush

treatment and each formulated Rumensin®80 level



Figure 3.4 Monensin concentrations in the flush material sampled at the finished product bin for

each flush treatment and each formulated Rumensin®80 level



Figure 3.5 Monensin concentrations in the flush material sampled at the finished product bin for each flush treatment and each formulated

Rumensin®80 level

	Rumensin® 80, g/ton		
-	100	600	1,200
Ingredients	%		
Major-ingredient(s)			
Corn	40.26	40.04	39.58
Minor-ingredient(s)			
Limestone	25.49	25.49	25.49
Urea	20.76	20.76	20.76
Micro-ingredient(s)			
Salt	4.96	4.96	4.96
Potassium chloride	4.16	4.16	4.16
KSU Beef trace mineral	0.73	0.73	0.73
Vitamin E-20	2.07	2.07	2.07
Vitamin A-30	0.15	0.15	0.15
Phosphate selenite	0.34	0.34	0.34
Liquid-ingredient(s)			
Soybean oil	0.62	0.62	0.62
Feed additive(s)			
Rumensin® 80	0.06	0.28	0.75
Tylan® 40	0.19	0.19	0.19
MGA® 200	0.21	0.21	0.21
Total	100.00	100.00	100.00

Table 3.1 Medicated diets used in Experiment 2 to evaluate monensin carryover
Ingredients	Non-Medicated, %
Major-ingredient(s)	
Corn	60.57
Minor-ingredient(s)	
Dehydrated alfalfa	15.00
Ground oats	10.60
Soybean meal	10.00
Micro-ingredient(s)	
Monocalcium phosphate	0.38
Salt	0.10
KSU Swine vitamin premix NB6157B	0.25
KSU HT trace mineral NB8557B	0.10
Liquid-ingredient(s)	
Molasses 8%	2.00
Soybean oil	1.00
Total	100.00

Table 3.2 Non-medicated diet used in Experiment 2 to evaluate

monensin carryover

I able J.J. Ellects of flush str		sin carryov	ver in sam	pung loca		ormulated		N OU IEVEI	unrougnour	une reeu mar	nuracturing p	ocess
					FIU	lsn i reaum	ents, % of	mixer cap	acity			
		10	0 g/ton			9	00 g/ton			1,2	.00 g/ton	
Type of batch	1.0	2.5	5.0	SEM ³	1.0	2.5	5.0	SEM ³	1.0	2.5	5.0	SEM ³
Sampling location							ppm ¹					
Medicated diet												
Mixer	105.9 ^a	125.2 ^a	103.2 ^a	9.92	551.8 ^a	677.0 ^a	605.3 ^a	16.94	1,138.9 ^a	$1,114.3^{a}$	1,089.5 ^a	12.87
Flush												
Finished product bin	77.3 ^b	19.0°	8.4 ^c	4.93	243.0 ^b	90.6°	33.6°	8.37	409.1 ^b	184.4 ^b	98.0 ^b	37.03
Non-medicated diet												
Mixer	$0.0^{d,x}$	0.0 ^{d,x}	0.0 ^{d,x}	0.00	$4.1^{d,x}$	$1.4^{d,x}$	$1.0^{d,x}$	0.78	$5.7^{d,y}$	$5.4^{d,y}$	$4.6^{d,x}$	0.75
Drag conveyor	0.0 ^{d,x}	0.0 ^{d,x}	0.0 ^{d,x}	0.00	3.7 ^{d,x}	2.1 ^{d,x}	$1.3^{d,x}$	0.81	5.1 ^{d,y}	$4.8^{d,y}$	$3.9^{d,x}$	0.22
Bucket elevator	$2.3^{d,x}$	0.0 ^{d,x}	0.0 ^{d,x}	0.28	8.2 ^{d,y}	4.3 ^{d,x}	4.3 ^{d,x}	0.68	6.8 ^{d,x}	8.2 ^{d,y}	$2.2^{d,x}$	1.11
Finished product bin	3.3 ^{d,x}	2.9 ^{d,x}	1.9 ^{d,x}	0.22	$10.1^{e,y}$	6.8 ^{e,x}	6.8 ^{e,x}	1.82	12.1 ^{d,y}	$15.5^{e,y}$	$15.2^{e,y}$	1.99
¹ Monensin carryover conce	entrations are	e means (n	= 2) in pp	m, with li	mit of dete	sction ± 1	mdq					

 2 Forberg 454.5 kg (1,000 lb) capacity drop bottom paddle mixer

³ Pooled SEM (n = 2) of the three flush size treatments by rows

^a Means within the row followed by different letters are significantly different (P < 0.05)

^{b-c} Means within the row followed by different letters are significantly different (P < 0.05)

 $^{d-f}$ Means within the non-medicated diet columns followed by different letters are significantly different (P < 0.05)

^{x-y} Means within the non-medicated rows followed by different letters are significantly different (P < 0.05)

				Flush Trea	atments, %	of mixer ca	apacity ²		
		100 g/	/ton		600 g/1	on		1,200 g	'ton
Type of batch	1.0	2.5	5.0	1.0	2.5	5.0	1.0	2.5	5.0
Sampling location					ppm ¹				
Non-medicated diet									
Mixer	0.0	0.0	0.0	4.1	1.4	1.0	5.7	5.4	4.6
Drag conveyor	0.0	0.0	0.0	0.0	0.7	0.3	0.0	0.0	0.0
Bucket elevator	2.3	0.0	0.0	4.1	2.2	3.0	1.1	2.8	0.0
Finished product bin	1.0	2.9	1.9	1.9	2.5	2.5	5.3	7.3	10.6
Total monensin carryover	3.3	2.9	1.9	10.1	6.8	6.8	12.1	15.5	15.2
¹ Monensin carryover concent	trations are	calculated	difference	es between	two locatio	ns within t	reatments		

Table 3.4 Calculated monensin carryover in sampling location and formulated Rumensin® 80 level throughout the feed manufacturing process

 2 Forberg 454.5 kg (1,000 lb) capacity drop bottom paddle mixer

Sources of Variation	$P < 0.05^{1}$
Drug level	< 0.0001
Flush size	0.0576
Sampling location	< 0.0001
Drug level × Sampling location	0.0056
Flush size × Sampling location	0.8100
Drug level × Flush size	0.1965
Drug level × Flush size × Sampling location	0.8999

Table 3.5 Pair-wise comparison of sampling location, flush size and formulatedRumensin® 80 level of non-medicated diet treatments in Experiment 2

¹Significant differences detected using least square means for mean separation at $\alpha = 0.05$

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