

HEAT CONDUCTION TRANSFER FUNCTIONS FOR
MULTI-LAYER STRUCTURES

by

TERRY DEL HUBBS

B.S., Kansas State University, 1975

A MASTER'S THESIS

submitted in partial fulfillment of the

requirements for the degree

MASTER OF SCIENCE

Department of Mechanical Engineering

KANSAS STATE UNIVERSITY
Manhattan, Kansas

1977

Approved by:


Major Professor

LD
2668
T4
1977
H82
C.2

207

TABLE OF CONTENTS

Chapter	Document	Page
I.	INTRODUCTION	1
	Problem	1
	Purpose	2
II.	DERIVATIONS	5
	Single-Layer Structure	5
	Multi-Layer Structures	8
	Surface Resistances	10
	z-Transform Method	13
	Inversion of z-Transforms	19
III.	CALCULATION OF THE z-TRANSFORM FUNCTIONS	22
	Roots of Function B	22
	Evaluation of z-Coefficients	24
	Calculation of Heat Flux	29
IV.	APPLICATIONS	30
	Two-Layer Wall	30
	Three-Layer Wall	35
	Temperature Control System	41
V.	CONCLUSION	50
	LIST OF REFERENCES	52
	APPENDIX A	53
	APPENDIX B	55
	APPENDIX C	59
	APPENDIX D	66
	APPENDIX E	76
	APPENDIX F	79
	APPENDIX G	86

LIST OF TABLES

Table	Page
1. Polynomial Coefficients Expressed as Equalities	20
2. Equalities for Calculation of Heat Flux	21
3. Double-Layer Wall	30
4. Roots of Double-Layer Wall	31
5. z-Coefficients for DELTA = 0.1 hr.	32
6. z-Coefficients for DELTA = 0.2 hr.	33
7. Heat Flux for DELTA = 0.1 hr.	36
8. Heat Flux for DELTA = 0.2 hr.	37
9. Triple-Layer Wall	35
10. Heat Flux for Three-Layer Wall	39
11. Air Conditioning Control System Constants	43

LIST OF FIGURES

Figure	Page
1. Single-Layer Slab	5
2. Multi-Layer Slab	8
3. Surface Resistance	10
4. Multi-Layer Slab and Resistances	11
5. Weighted Impulses	19
6. Inside Temperature	34
7. Outside Temperature	34
8. Heat Flux Response of Double-Layer Wall	38
9. Heat Fluxes of Two-Layer and Three-Layer Walls	40
10. Air Conditioning Control System	41
11. Air Conditioning Control System Block Diagram	42
12. Room Temperature Deviation for 75°F Setpoint	45
13. Outside Temperature Profile	46
14. Inside Heat Flux and Heat Input Deviation for 50°F Outside Temperature	47
15. Room Temperature Deviation for 50°F Outside Temperature	48
16. Triangular Pulse	55
17. Weighted Impulse	57
18. Room Air Space	79
19. Room Block Diagram	81
20. Heating Coil Block Diagram	82
21. Steam Flow Control Block Diagram	83
22. Block Diagram for Multi-Layer Wall	84
23. Air Conditioning Control System Block Diagram	85

NOMENCLATURE

$\theta(x,t)$	slab temperature ($^{\circ}\text{F}$)
$\theta(x,0) = \theta_{Go}$	initial slab temperature ($^{\circ}\text{F}$)
f	heat flux (BTU/hr)
v	temperature deviation from initial temperature ($^{\circ}\text{F}$)
x	local position with respect to x coordinate (ft)
t	time (hr)
α_r	thermal diffusivity of r^{th} layer (ft^2/hr)
k_r	thermal conductivity of r^{th} layer (BTU/hr-ft- $^{\circ}\text{F}$)
ρ_r	density of r^{th} layer (lb_m/ft^3)
c_r	specific heat of r^{th} layer (BTU/ lb_m - $^{\circ}\text{F}$)
Δx_r	thickness of r^{th} layer (ft)
R_1	inner thermal surface resistance (hr- $^{\circ}\text{F}/\text{BTU}$)
R_n	outer thermal surface resistance (hr- $^{\circ}\text{F}/\text{BTU}$)
s	the Laplace variable
T	Laplace transform of temperature, θ
F	Laplace transform of heat flux, f
V	Laplace transform of v
β_m	roots of the function $B=0$
Δ	sampling period of the z-transforms (hr)
$R(z)$	z-transfer function of Laplace transfer function, $-A/B$
$W(z)$	z-transfer function of Laplace transfer function, $1/B$

CHAPTER I

INTRODUCTION

Problem

In recent years, the words "energy shortage" have become commonplace. Some argue that the energy crunch is an imaginary crisis being used by energy producers to increase profits, while others insist that the energy shortage is a real and grave situation of severe consequence being used by energy producers to increase profits. All agree that energy costs have increased astronomically.

In the area of building climate control, economic factors have made some traditional engineering design techniques impracticable, improved the feasibility of other concepts, and coincidentally inspired new and innovative design tools. Much work has been done in the simulation of building air conditioning systems. The term air conditioning is not limited to cooling, but implies the entire process of conditioning air. Some primary concerns have been predicting heating and cooling loads accurately so that 1) heating, cooling, and air handling equipment may be sized properly, 2) various building configurations can be easily compared, and 3) changes made in building materials may be evaluated. In most cases, the simulation consists of a large digital computer program made up of several complicated subroutines. Often, a subroutine is written to handle a unique part of the physical problem, for example, one subroutine may find heat loss due to conduction heat transfer through walls, another subroutine may handle solar radiation and shading, while yet another simulates systems and equipment. These programs are most often used with a one hour stepsize and depend upon

U.S. Weather Bureau tapes for hourly environmental data, as well as user supplied data such as building dimensions, materials, etc. With a one hour stepsize, the availability of data is good, heating and cooling loads can be obtained to sufficiently satisfy many problems, and the computing time required is reasonable. An hourly stepsize also takes full advantage of the conduction transfer functions strong points, namely speed and accuracy. The output is often an hour-by-hour profile of building heat gain or loss. In most cases, to obtain hour-by-hour heat loss the inside temperature must be assumed to be constant. The hourly stepsize itself is sometimes limiting. For example, an hourly step may bypass some effects of a fast dynamic control system. Also, large inaccuracy could result due to input that deviates appreciably during an hour, and is then approximated with an hourly increment. These and similar restrictions limit the flexibility of these simulations. Such programs are written for and conform to studies of physical building characteristics reasonably well but are not equally well suited to studies of the buildings automatic climate controls. Control installations and changes are of paramount economic importance as such actions give quick payback [1].

In order to investigate the effect of control system dynamics on energy consumption, a simulation with a stepsize short enough to manifest the dynamics of the control system is required. The problem approached in this research is the investigation of the effect on the conduction transfer functions and associated simulation algorithm of shortening the stepsize.

Purpose

The purpose of this thesis is to demonstrate and satisfactorily document an algorithm for transient heat conduction through multi-layer walls that

may be used as an element in a computer simulation to study effects of variations in the automatic temperature control systems of buildings. The algorithm should 1) be general enough to handle walls of any number of layers, 2) have a variable time increment which is short enough to be used with fast dynamic elements, 3) have no restrictive input, such as constant or periodic boundary conditions, 4) be reasonably accurate, 5) require as little computing time as possible, and 6) have few restricting assumptions.

This thesis will document a study of the thermal response factor technique applied to this problem with these criteria.

The development of the thermal response factor concept cannot be attributed to a single individual. Mitalas and Stephenson [2] suggest Nessi and Nisolle [3] as early investigators and cite Mackey and Wright [4] as having worked on the same problem with restricted boundary conditions. T. Kusuda [5] has also contributed to the method and attributes significant contributions to Mitalas and Arseneault [6].

Analytical solutions to one-dimensional unsteady-state systems with specified boundary conditions occupy substantial space in heat-flow and applied mathematics texts. Since the boundary conditions in practical applications may change in a manner unique to the particular system and application, even the most extensive compilation of formal solutions is unlikely to match a given practical case completely. However, with the use of a digital computer, differential difference methods may prove to be powerful tools [7]. Finite difference approximations are a well-known approach to solving transient heat transfer problems. Although the computational procedures involved are less complicated than with the response factor concept, small grid sizes are required for finite difference time and space coordinates if computational stability is to be retained for a

multi-layer heat flow problem [5]. The response factor method does not have these limitations.

The basic steps in the development of the response factor algorithm are

- 1) Obtain the differential equation to model heat conduction in a slab.
- 2) Derive expressions for temperature and heat flux by applying Laplace transforms.
- 3) Generalize the analysis to "n" layers.
- 4) Assume an input form and apply z-transforms to the Laplace transfer functions.
- 5) Manipulate the z-transfer functions into the form of infinite power series in z^{-1} and obtain the coefficients of the z terms.
- 6) Find the solution in time by expanding the z-polynomials.

The derivation of the algorithm follows the basic outline as listed above and is found in Chapter II. Chapter III explains the computer programs used to develop and apply the response factors, while Chapter IV contains examples where the response factors are used to obtain solutions to practical problems.

CHAPTER II

DERIVATIONS

Single Layer Structure

Consider a semi-infinite slab of a homogeneous material with a uniform initial temperature, $\theta(x,0)$. Conduction heat transfer through the slab is described by the one-dimensional heat-conduction equation,

$$\frac{\partial^2 \theta}{\partial x^2} = \frac{1}{\alpha} \frac{\partial \theta}{\partial t} \quad \text{where} \quad \alpha = \frac{k}{\rho c} \quad . \quad [8] \quad (1)$$

$\theta(x,t)$ - temperature
 x - local position with respect to x coordinate
 t - time
 α - thermal diffusivity
 k - thermal conductivity
 ρ - density
 c - specific heat

Below is a schematic cross-section of the layer, its initial condition, and the heat flux, f , at the left surface of the slab.

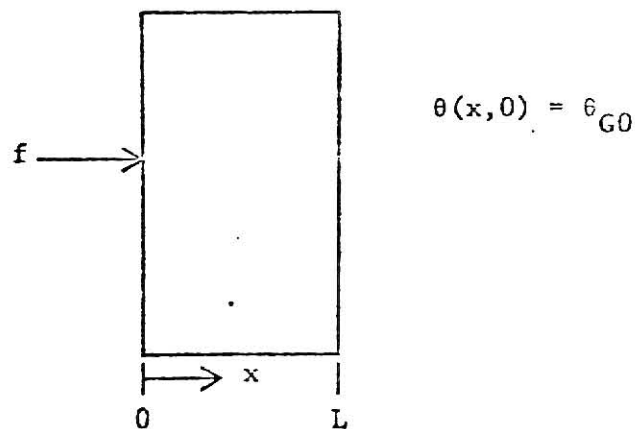


Figure 1. Single-Layer Slab.

Below, the Laplace transform of the one-dimensional heat conduction equation is obtained [9].

$$L\left[\frac{\partial^2 \theta}{\partial x^2}\right] = L\left[\frac{1}{\alpha} \frac{\partial \theta}{\partial t}\right]$$

$$\frac{d^2 T}{dx^2} = \frac{s}{\alpha} \left[T - \frac{\theta_{Go}}{s}\right] \quad (2)$$

T - Laplace transform of temperature, θ

s - the Laplace variable.

Equation (2) may be simplified by expressing the temperature as a deviation from the initial, uniform temperature.

$$v(x,t) = \theta(x,t) - \theta(x,0) .$$

Applying the Laplace transform to this expression yields

$$V = T - \frac{\theta_{Go}}{s} . \quad (3)$$

V - the Laplace transform of v .

Differentiating (3) twice with respect to x results in

$$\frac{d^2 V}{dx^2} = \frac{d^2 T}{dx^2} . \quad (4)$$

Substituting (3) and (4) into (2) yields

$$\frac{d^2 V}{dx^2} = \frac{s}{\alpha} V . \quad (5)$$

The significance of these operations is that equation (5) is not a partial differential equation like equation (1), but rather an ordinary differential equation where s is an algebraic variable.

The general solution to equation (5) is [10]

$$V_{(x,s)} = \frac{(V_0)'}{\sqrt{s/\alpha}} \sinh(\sqrt{s/\alpha} x) + V_0 \cosh(\sqrt{s/\alpha} x) \quad \text{where} \quad (6)$$

$$V_0 = L[v(0,t)] = L[\theta(0,t) - \theta_{Go}] .$$

The heat flux, f , at any x (see Figure 1) is

$$f = -k \frac{d\theta}{dx} . \quad [8]$$

Taking the Laplace transform yields

$$F = -k \frac{dT}{dx} \quad \text{where} \quad (7)$$

F - Laplace transform of heat flux, $f(x,t)$.

Differentiating equation (3) with respect to x yields

$$\frac{dT}{dx} = \frac{dV}{dx} ,$$

thus equation (7) may be written

$$F = -k \frac{dV}{dx} . \quad (8)$$

Equation (8) relates the heat flux at any point x in the slab to the gradient of the temperature at that point.

At $x=0$, it follows that

$$\frac{dV_0}{dx} = (V_0)' = - \frac{F_0}{k} ,$$

which may be substituted into the general solution, equation (6),

$$V(x) = -F_0 \frac{1}{k} \sqrt{\alpha/s} \sinh(\sqrt{s/\alpha} x) + V_0 \cosh(\sqrt{s/\alpha} x) . \quad (9)$$

The substitution eliminated the derivative in the solution, and both coefficients, F_0 and V_0 , are for $x=0$.

To obtain an expression for F , equation (9) is differentiated with respect to x ,

$$\frac{dV}{dx} = -F_0 \frac{1}{k} \cosh(\sqrt{s/\alpha} x) + V_0 \sqrt{s/\alpha} \sinh(\sqrt{s/\alpha} x) .$$

Substituting into equation (8) yields

$$F = F_0 \cosh(\sqrt{s/\alpha} x) - V_0 k \sqrt{s/\alpha} \sinh(\sqrt{s/\alpha} x) . \quad (10)$$

Equations (9) and (10) are now placed in matrix form.

$$\begin{bmatrix} V \\ F \end{bmatrix} = \begin{bmatrix} \cosh(\sqrt{s/\alpha} x) & -\frac{1}{k} \sqrt{\alpha/x} \sinh(\sqrt{s/\alpha} x) \\ -k \sqrt{s/\alpha} \sinh(\sqrt{s/\alpha} x) & \cosh(\sqrt{s/\alpha} x) \end{bmatrix} \begin{bmatrix} V_0 \\ F_0 \end{bmatrix}$$

The expressions in this matrix relate the temperature and heat flux at any x in the layer to the temperature and heat flux at $x=0$. Below is a matrix for the temperature and flux at $x=L$.

$$\begin{bmatrix} V_L \\ F_L \end{bmatrix} = \begin{bmatrix} \cosh(\sqrt{s/\alpha} L) & -\frac{1}{k} \sqrt{\alpha/s} \sinh(\sqrt{s/\alpha} L) \\ -k \sqrt{s/\alpha} \sinh(\sqrt{s/\alpha} L) & \cosh(\sqrt{s/\alpha} L) \end{bmatrix} \begin{bmatrix} V_0 \\ F_0 \end{bmatrix} \quad (11)$$

Note that this matrix relates the temperature and flux at one face to the temperature and flux at the other face. Also note that L is the thickness of the layer.

Multi-Layer Structures

Following the procedure of Carslaw and Jaeger (11), a multi-layer wall composed of n slabs as in Figure 2 is considered.

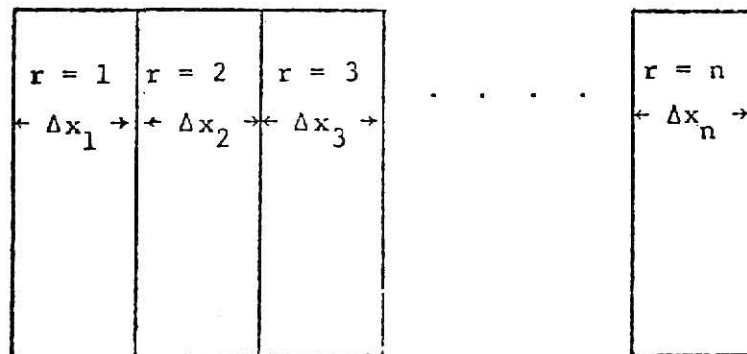


Figure 2. Multi-Layer Slab.

By generalizing matrix (11), the following matrix may be written for use with any particular layer in Figure 2. Recall that the substitution $v(x,t) = \theta(x,t) - \theta_{Go}$ was made in the derivation of the expressions in matrix (11) to oblige the initial condition $\theta(x,0) = \theta_{Go}$. Therefore each layer must be at the initial temperature θ_{Go} .

$$\begin{bmatrix} V_{r+1} \\ F_{r+1} \end{bmatrix} = \begin{bmatrix} \cosh(\sqrt{s/\alpha_r} \Delta x_r) & -\frac{1}{k_r} \sqrt{\alpha_r/s} \sinh(\sqrt{s/\alpha_r} \Delta x_r) \\ -k_r \sqrt{s/\alpha_r} \sinh(\sqrt{s/\alpha_r} \Delta x_r) & \cosh(\sqrt{s/\alpha_r} \Delta x_r) \end{bmatrix} \begin{bmatrix} V_r \\ F_r \end{bmatrix}$$

For brevity, the following substitutions are made.

$$\begin{aligned} A_r &= \cosh(\sqrt{s/\alpha_r} \Delta x_r) \\ B_r &= -\frac{1}{k_r} \sqrt{\alpha_r/s} \sinh(\sqrt{s/\alpha_r} \Delta x_r) \\ C_r &= -k_r \sqrt{s/\alpha_r} \sinh(\sqrt{s/\alpha_r} \Delta x_r) \\ D_r &= \cosh(\sqrt{s/\alpha_r} \Delta x_r) \end{aligned}$$

For layer one, $r=1$, and

$$\begin{bmatrix} V_2 \\ F_2 \end{bmatrix} = \begin{bmatrix} A_1 & B_1 \\ C_1 & D_1 \end{bmatrix} \begin{bmatrix} V_1 \\ F_1 \end{bmatrix} .$$

Similarly for layer two, $r=2$, and

$$\begin{bmatrix} V_3 \\ F_3 \end{bmatrix} = \begin{bmatrix} A_2 & B_2 \\ C_2 & D_2 \end{bmatrix} \begin{bmatrix} V_2 \\ F_2 \end{bmatrix} .$$

If there is perfect thermal contact between the slabs, simple substitution yields

$$\begin{bmatrix} V_3 \\ F_3 \end{bmatrix} = \begin{bmatrix} A_2 & B_2 \\ C_2 & D_2 \end{bmatrix} \begin{bmatrix} A_1 & B_1 \\ C_1 & D_1 \end{bmatrix} \begin{bmatrix} V_1 \\ F_1 \end{bmatrix} .$$

In like manner, the expressions relating inside and outside face temperature and heat flux for an n layer structure in matrix form are

$$\begin{bmatrix} V_{n+1} \\ F_{n+1} \end{bmatrix} = \begin{bmatrix} A_n & B_n \\ C_n & D_n \end{bmatrix} \begin{bmatrix} A_{n-1} & B_{n-1} \\ C_{n-1} & D_{n-1} \end{bmatrix} \cdots \begin{bmatrix} A_1 & B_1 \\ C_1 & D_1 \end{bmatrix} \begin{bmatrix} V_1 \\ F_1 \end{bmatrix} . \quad (12)$$

Surface Resistances

A linear thermal resistance, R , may be included at the surface of a layer as shown in Figure 3. Modeling the surface film in this way neglects any thermal capacitance of the film but accounts for the resistance to the flow of heat through it. Physically, the capacitance of the film is minute and may be neglected. The matrix notation relating the temperature and flux at the resistance to the temperature and heat flux at the slab surface is

$$\begin{bmatrix} V_1 \\ F_1 \end{bmatrix} = \begin{bmatrix} 1 & -R \\ 0 & 1 \end{bmatrix} \begin{bmatrix} V_I \\ F_I \end{bmatrix} . \quad [11]$$

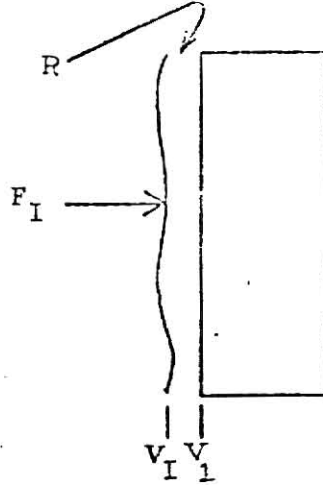


Figure 3. Surface Resistance.

Thermal resistances may be considered at both outer surfaces of the multi-layer slab as shown in Figure 4.

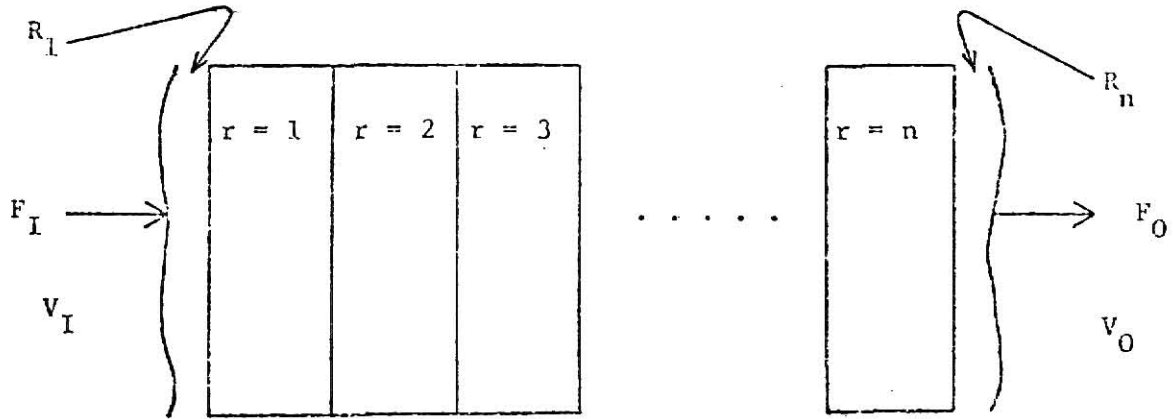


Figure 4. Multi-Layer Slab and Resistances.

The expressions relating inside and outside temperature and heat flux are

$$\begin{bmatrix} V_O \\ F_O \end{bmatrix} = \begin{bmatrix} 1 & -R_n \\ 0 & 1 \end{bmatrix} \begin{bmatrix} A_n & B_n \\ C_n & D_n \end{bmatrix} \begin{bmatrix} A_{n-1} & B_{n-1} \\ C_{n-1} & D_{n-1} \end{bmatrix} \cdots \begin{bmatrix} A_1 & B_1 \\ C_1 & D_1 \end{bmatrix} \begin{bmatrix} 1 & -R_1 \\ 0 & 1 \end{bmatrix} \begin{bmatrix} V_I \\ F_I \end{bmatrix}. \quad (13)$$

The product of two 2×2 matrices is a 2×2 matrix. Therefore, the results of multiplying the 2×2 matrices together will be a 2×2 . The resultant 2×2 matrix will be symbolized as

$$\begin{bmatrix} A & B \\ C & D \end{bmatrix}. \quad (14)$$

Expression (13) is now simplified to

$$\begin{bmatrix} V_O \\ F_O \end{bmatrix} = \begin{bmatrix} A & B \\ C & D \end{bmatrix} \begin{bmatrix} V_I \\ F_I \end{bmatrix}. \quad (15)$$

Expression (15) may be manipulated so the heat fluxes are both to the left of the equals sign. By matrix multiplication of expression (15), the following equations are obtained:

$$V_O = AV_I + BF_I \quad (16)$$

$$F_O = CV_I + DF_I \quad (17)$$

From equation (16)

$$F_I = -\frac{A}{B} V_I + \frac{1}{B} V_O \quad (18)$$

By substituting this equation into equation (17), an expression for the Laplace transform of the heat flux at R_1 as a function of the inside and outside temperatures is obtainable.

$$F_O = \frac{(BC - AD)}{B} V_I + \frac{D}{B} V_O \quad (19)$$

This equation may be simplified by recognizing that the term $(BC - AD)$ is the determinant of matrix (14). The determinant may be evaluated as follows.

$$\Gamma = \begin{vmatrix} A & B \\ C & D \end{vmatrix} = \Gamma_{Rn} \cdot \Gamma_n \dots \Gamma_2 \cdot \Gamma_1 \cdot \Gamma_{R1} = \begin{vmatrix} 1 & -R_n \\ 0 & 1 \end{vmatrix} \begin{vmatrix} A_n & B_n \\ C_n & D_n \end{vmatrix} \\ \dots \begin{vmatrix} A_2 & B_2 \\ C_2 & D_2 \end{vmatrix} \begin{vmatrix} A_1 & B_1 \\ C_1 & D_1 \end{vmatrix} \begin{vmatrix} 1 & -R_1 \\ 0 & 1 \end{vmatrix}$$

It is easily found that $\Gamma_{Rn} = \Gamma_{R1} = 1$.

Now consider the determinant of the matrix for layer r .

$$\Gamma_r = \begin{vmatrix} \cosh(\sqrt{s/\alpha_r} \Delta x_r) & -\frac{1}{k_r} \sqrt{\alpha_r/s} \sinh(\sqrt{s/\alpha_r} \Delta s_r) \\ -k_r \sqrt{s/\alpha_r} \sinh(\sqrt{s/\alpha_r} \Delta x_r) & \cosh(\sqrt{s/\alpha_r} \Delta x_r) \end{vmatrix} \\ = \cosh^2(\sqrt{s/\alpha_r} \Delta x_r) - \sinh^2(\sqrt{s/\alpha_r} \Delta x_r) = 1$$

It may be seen that the determinant of matrix (14) is equal to 1.

Equation (19) now simplifies to

$$F_O = \frac{1}{B} V_I + \frac{D}{B} V_O . \quad (20)$$

Equations (18) and (20) are now placed in matrix form.

$$\begin{bmatrix} F_I \\ F_O \end{bmatrix} = \begin{bmatrix} -\frac{A}{B} & \frac{1}{B} \\ \frac{1}{B} & \frac{D}{B} \end{bmatrix} \begin{bmatrix} V_I \\ V_O \end{bmatrix} \quad (21)$$

The above matrices relate the inside and outside temperatures to the inside and outside heat fluxes. The terms in the 2x2 matrix are the transfer functions in the Laplace domain.

z- Transform Method

For this procedure to be of practical value, the inverse Laplace transforms must be found. Inverse Laplace transforms may be found in a variety of ways. For example direct integration may be used, tables of Laplace transforms are sometimes helpful, the partial fraction expansion method may be applied, or z-transforms can be employed. However, the complexity of the Laplace transforms, in this case, nearly eliminates direct integration or the use of tables. The z-transform technique as outlined in reference [2] will be used in this work. With this method, an input form is selected and multiplied by the transfer function to obtain the Laplace transform of the output. The z-transform of the output, the input times the transfer function, is then found. The z-transfer function is then obtained by dividing the z-transform of the output by the z-transform of the input used to obtain the Laplace transform of the output. What follows is a detailed development of the z-transform method.

Recall that the terms in the 2x2 matrix of expression (21), A, B, and D, are all functions of the Laplace variable, s. It may be helpful to return to

expression (13) and page 8 to again see how the terms are developed. One finds that the terms are composed of sums of products of sinh and cosh terms. So, the upper left Laplace transfer function, $-\frac{A}{B}$, consists of a string of cosh and sinh terms divided by some other array of cosh and sinh terms. The size of the string of terms is determined by "n", the number of layers in the structure. The hyperbolic functions have an infinite set of roots, but are approximated with a finite number of roots.

The upper equation from expression (21) is

$$F_I = -\frac{A}{B} V_I + \frac{1}{B} V_O . \quad (22)$$

Here, the Laplace transform of the output, F_I , is the sum of a transfer function, $-\frac{A}{B}$, times an input, V_I , and another transfer function, $\frac{1}{B}$, times another input, V_O . The z-transform of the output heat flux will be composed of the sum of the two responses due to each input. A detailed derivation of the z-transfer function for the $-\frac{A}{B}$ transfer function is included in this thesis. The other z-transfer functions are easily developed following the same pattern.

To obtain a z-transfer function, an input form must be chosen. The selection of the input form is equivalent to designating a function for interpolating between the discrete values given by the z-transform coefficients [2]. A step function is synonymous to representing the input by a staircase approximation, while a ramp input is equivalent to linear interpolation between the discrete values. Inputs of higher order than the ramp input yield unstable transfer functions because the z-transfer functions have poles at the zeroes of the z-transform of the input. A step input form is satisfactory for small time increments and slowly changing inputs, while a ramp input is preferable for larger time increments or rapidly deviating inputs. Ramp inputs are used in the following developments.

The Laplace transform of the output, O , may be found with the following equation.

$$O = -\frac{A}{B} I$$

O - Laplace transform of the output

$-\frac{A}{B}$ - Laplace transfer function

I - Laplace transform of the input

In this case, the input is a ramp function, and

$$I = \frac{1}{s^2} \quad [12]$$

Therefore,

$$O = -\frac{A}{s^2 B}$$

This output has a double pole at $s=0$, and other poles at the roots of B .

See Appendix A for a discussion of the roots of the expression B .

The partial fraction expansion of O is

$$O = \frac{p_2}{s^2} + \frac{p_1}{s} + \frac{q_1}{s + \beta_1} + \frac{q_2}{s + \beta_2} + \dots + \frac{q_n}{s + \beta_n} + \dots \quad (23)$$

where the β 's are the roots of the expression B , and p_2 , p_1 , and the q 's are defined below.

$$p_2 = \left[-\frac{A}{B} \right] \Big|_{s=0} \quad p_1 = - \left[\frac{B \frac{dA}{ds} - A \frac{dB}{ds}}{B^2} \right] \Big|_{s=0} \quad q_m = \left[-\frac{A}{s^2 B} (s + \beta_m) \right] \Big|_{s=-\beta_m}$$

The q 's are the residues of O . In the present form, the evaluation of a q term would result in an indeterminate solution. However, L'Hospital's Rule may be used to find an expression which yields determinant results. This expression is shown below.

$$q_m = \left[-\frac{A}{s^2 \frac{dB}{ds}} \right] \Big|_{s=-\beta_m}$$

Realize that p_2 , p_1 , and the q 's are all constants that have been evaluated at specific values of s , namely 0 and $-\beta_m$. Thus their presence will not affect the form of the z -transform of the function in which they are located. If the z -transform of the partial fraction expansion of O , Equation (21), is then found, the result is $O(z)$.

$$O(z) = \frac{p_2 \Delta}{z(1 - z^{-1})^2} + \frac{p_1}{(1 - z^{-1})} + \sum_{m=1}^{\infty} \left[\frac{q_m}{(1 - e^{-\beta_m \Delta} z^{-1})} \right]$$

Δ - sampling period of the z -transforms.

When a common denominator is found,

$$\begin{aligned} O(z) = & \left(\frac{1}{z(1-z^{-1})^2 \prod_{m=1}^{\infty} (1 - e^{-\beta_m \Delta} z^{-1})} \right) [p_2 \Delta \prod_{m=1}^{\infty} (1 - e^{-\beta_m \Delta} z^{-1}) \\ & + p_1 z(1-z^{-1}) \prod_{m=1}^{\infty} (1 - e^{-\beta_m \Delta} z^{-1}) \\ & + z(1-z^{-1})^2 \prod_{m=1}^{\infty} (1 - e^{-\beta_m \Delta} z^{-1}) \cdot \left[\sum_{m=1}^{\infty} \left(\frac{q_m}{1 - e^{-\beta_m \Delta} z^{-1}} \right) \right] . \end{aligned}$$

From this expression for the output, it is possible to find a z -transfer function, $R(z)$, by dividing by the z -transform of the input. Recall that the input was a ramp function. The z -transform of a ramp function is

$$I(z) = \frac{\Delta}{z(1 - z^{-1})^2} .$$

Now, $R(z)$, the z -transfer function of the Laplace transfer function $-\frac{A}{B}$ is found to be

$$\begin{aligned}
R(z) = \frac{O(z)}{I(z)} = & \left(\frac{1}{\prod_{m=1}^{\infty} (1 - e^{-\beta_m \Delta} z^{-1})} \right) [p_2 \prod_{m=1}^{\infty} (1 - e^{-\beta_m \Delta} z^{-1}) \\
& + \frac{p_1}{\Delta} z(1-z^{-1}) \prod_{m=1}^{\infty} (1 - e^{-\beta_m \Delta} z^{-1}) \\
& + \frac{z(1-z^{-1})^2}{\Delta} \prod_{m=1}^{\infty} (1 - e^{-\beta_m \Delta} z^{-1}) \left[\sum_{m=1}^{\infty} \left(\frac{q_m}{1 - e^{-\beta_m \Delta} z^{-1}} \right) \right]] .
\end{aligned}
\tag{24}$$

This z-transfer function, or pulse transfer function may be used to relate the pulsed output of the wall to its pulsed input.

In summary, an input form has been selected and the Laplace transform of the output was found by multiplying that input by a Laplace transfer function that reflects the thermal characteristics of a multi-layer wall. The z-transform of the output was then found. This output was divided by the z-transform of the input to yield a z-transfer function for the wall.

The z-transfer function was not obtained by taking the z-transform of the Laplace transfer function. If the z-transfer function were obtained in that way, and then multiplied by the z-transform of the input, the sampled output obtained would be the response due to a "sampled" input rather than a continuous input. That is

$$IG(z) \neq I(z) G(z)$$

where the G term is the transfer function. See reference (12), page 644.

The transfer function, $R(z)$, may be put in the form of a ratio of two infinite power series in z^{-1} . In practice however, a finite set of roots of the function B is employed resulting in series of finite numbers of terms.

$$R(z) = \frac{a_1 + a_2 z^{-1} + a_3 z^{-2} + \dots + a_{n+1} z^{-n}}{b_1 + b_2 z^{-1} + b_3 z^{-2} + \dots + b_{n+1} z^{-n}}$$

a - numerator coefficients

b - denominator coefficients

n - number of roots of function B

The coefficients may be evaluated by expanding the numerator and denominator of equation (24). Calculation of these coefficients is discussed in Chapter III.

$R(z)$, the z-transfer function for the Laplace transfer function $-\frac{A}{B}$ has now been derived. By following the same steps, another z-transfer function, which is called $W(z)$, may be developed for the Laplace transfer function $\frac{1}{B}$. (See expression (21)). When the partial fraction expansion of the $\frac{1}{B}$ transfer function is found, the following constants are necessary.

$$u_2 = \left[\frac{1}{B} \right] \Big|_{s=0}, \quad u_1 = \left[\frac{\frac{dB}{ds}}{B^2} \right] \Big|_{s=0}, \quad v_m = \left[\frac{1}{s^2 \frac{dB}{ds}} \right] \Big|_{s=-\beta_m}$$

As before, the Laplace transfer function may be maneuvered into a z-transfer function in the following form.

$$W(z) = \frac{c_1 + c_2 z^{-1} + c_3 z^{-2} + \dots + c_{n+1} z^{-n}}{d_1 + d_2 z^{-1} + d_3 z^{-2} + \dots + d_{n+1} z^{-n}}$$

c - numerator coefficients

d - denominator coefficients

n - number of roots of function B

When the two z-transfer functions have been derived, it is found that they have the same denominator. Then

$$b_1 + b_2 z^{-1} + b_3 z^{-2} + \dots + b_{n+1} z^{-n} = d_1 + d_2 z^{-1} + d_3 z^{-2} + \dots + d_{n+1} z^{-n} .$$

Inversion of z-Transforms

For the moment, consider an input of a train of weighted impulses as in Figure 5.

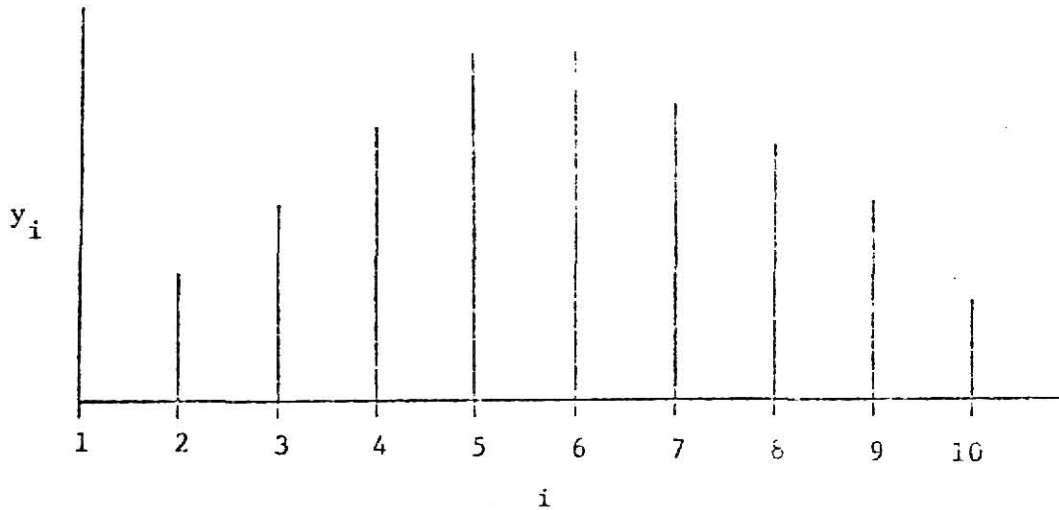


Figure 5. Weighted Impulses.

The impulses are equally spaced and each impulse is weighted by a constant, y_i . $I(z)$, the z-transform of this input function is

$$I(z) = \sum_{i=1}^{\infty} y_i z^{-i+1} = y_1 + y_2 z^{-1} + y_3 z^{-2} + \dots .$$

Similarly, the z-transform of an output function of the same form may be expressed as

$$O(z) = o_1 + o_2 z^{-1} + o_3 z^{-2} + \dots .$$

It is known that

$$O(z) = G(z)I(z) . \quad [12]$$

$O(z)$ - z-transform of the output

$G(z)$ - z-transfer function

$I(z)$ - z-transform of the input

And for the transfer function $R(z)$ it follows that

$$O_1 + O_2 z^{-1} + O_3 z^{-2} + \dots = \left(\frac{a_1 + a_2 z^{-1} + a_3 z^{-2} + \dots + a_{n+1} z^{-n}}{b_1 + b_2 z^{-1} + b_3 z^{-2} + \dots + b_{n+1} z^{-n}} \right) \cdot (y_1 + y_2 z^{-1} + y_3 z^{-2} + \dots) .$$

By clearing the denominator and multiplying, equation (25) may be derived.

$$\begin{aligned} O_1 b_1 + (O_2 b_1 + O_1 b_2) z^{-1} + (O_3 b_1 + O_2 b_2 + O_1 b_3) z^{-2} + (O_4 b_1 + O_3 b_2 + \\ + O_2 b_3 + O_1 b_4) z^{-3} + \dots = y_1 a_1 + (y_2 a_1 + y_1 a_2) z^{-1} + (y_3 a_1 + \\ + y_2 a_2 + y_1 a_3) z^{-2} + (y_4 a_1 + y_3 a_2 + y_2 a_3 + y_1 a_4) z^{-3} + \dots \quad (25) \end{aligned}$$

Both sides of equation (25) are polynomials, so the coefficients of the various powers of z^{-1} on each side of the equation must be equivalent.

Furthermore, each side of the equation is convergent and the coefficient of the z^{-k} term in each series is the value of the function at time $k\Delta$. Δ is the sampling period of the z-transforms. A set of equalities may be formulated from equation (25) and are listed below in Table 1.

Table 1. Polynomial Coefficients Expressed as Equalities.

$k\Delta$	Equalities
0	$O_1 b_1 = y_1 a_1$
1Δ	$O_2 b_1 + O_1 b_2 = y_2 a_1 + y_1 a_2$
2Δ	$O_3 b_1 + O_2 b_2 + O_1 b_3 = y_3 a_1 + y_2 a_2 + y_1 a_3$
3Δ	$O_4 b_1 + O_3 b_2 + O_2 b_3 + O_1 b_4 = y_4 a_1 + y_3 a_2 + y_2 a_3 + y_1 a_4$

If the output at $k\Delta$, O_{k+1} , is unknown but the input and transfer function are known, the output may be found by solving the equations. Values of the output are used in subsequent equations.

This technique may be extended to include the transfer function $W(z)$ and invert the z -transformation of equation (22) to obtain values of the heat flux at specific points in time. As shown above, coefficients of like powers of an expanded polynomial can be equated yielding expressions that may be used to find the heat flux at $t = k\Delta$, f_{k+1} , when the input temperatures and transfer functions are known. A few of these expressions are contained in Table 2.

Table 2. Equalities for Calculation of Heat Flux.

$k\Delta$	Equalities
0	$f_1 b_1 = U_1 a_1 + V_1 c_1$
1Δ	$f_2 b_1 + f_1 b_2 = U_2 a_1 + U_1 a_2 + V_2 c_1 + V_1 c_2$
2Δ	$f_3 b_1 + f_2 b_2 + f_1 b_3 = U_3 a_1 + U_2 a_2 + U_1 a_3 + V_3 c_1 + V_2 c_2 + V_1 c_3$
3Δ	$f_4 b_1 + f_3 b_2 + f_2 b_3 + f_1 b_4 = U_4 a_1 + U_3 a_2 + U_2 a_3 + U_1 a_4 + V_4 c_1 + V_3 c_2 + V_2 c_3 + V_1 c_4$
$\vdots$	$\vdots$

f - heat flux at film surface, f_I (see Figure 4).

U - previously defined by V_I

V - previously defined by V_0

U_{k+1} and V_{k+1} are discrete values of the inside and outside temperatures at $t = k\Delta$, and likewise the output, f_{k+1} , is discrete values of the heat flux at $t = k\Delta$. The z -transfer functions, however, were developed with a ramp input. A discussion of this may be located in Appendix B.

CHAPTER III

CALCULATION OF THE z-TRANSFER FUNCTIONS

To obtain the coefficients of the z-transfer functions, a variety of numerical constants must be found. Except for a few, the constants are evaluated from large, complicated functions. Evaluating the constants by hand would be impractical. A digital computer is a necessary tool for the application of the concept. In most cases, the computer programming may be done in a straight-forward, brute force manner. However, a few scraps of ingenuity greatly improve some of the programs' flexibility and comprehensiveness. The computer programs in this chapter are all done in double precision for increased accuracy. It was found that extended accuracy is necessary for reliable results as the stepsize in time is decreased. All of the programs are composed of an array of general subroutines. The subroutines were written with extreme versatility and will no doubt prove useful to others extending this work.

Roots of Function B

First, it is necessary to acquire the roots of the function B. It is known that there is an infinite set of negative real roots of this function. As the roots become larger, they contribute less and less to the value of the coefficients. If the values of the denominator coefficients are to be accurate within $\pm 10^{-8}$, then

$$e^{-\beta_{\max} \Delta} < 10^{-8} . \quad [2]$$

From this it is noted that the value of the stepsize, Δ , is also a factor in determining how many roots of B are necessary.

The program that calculates the roots, β_m , of the function B is referred to in the discussion as Root-finder. Input to the program is N, the number of layers, R1, the inner surface resistance, RN, the outer surface resistance, A, the thermal diffusivity of each layer, CON, the specific heat of each layer, and DELX, each layer's thickness. Root-finder is initialized at some starting value of the variable s. The value of B is then found at this s, then s is decremented and the value of B is again calculated. If the signs of the values of B differ, it is known that a root of the function B lies between the initial and the decremented value of s. When the general position of a root has been located, program control is sent to a subroutine named BETA. This subroutine converges on the root quickly but must have the value of the function's derivative to do so. For this reason, another subroutine, DERIV, is utilized. DERIV finds the derivative of each element of matrix (14) for a specified value of s. Two support subroutines are called by other subroutines. One is called MATMUL and does matrix multiplication. The other, HMADD, performs matrix addition.

The size of the constant used to decrement s is not strictly defined. A large constant reduces the computing time required to find the roots, but caution should be exercised so that too large a constant is not used, as two roots could be stepped over thus resulting in no change in sign of the function.

When the subroutines FIGURE and DERIV are executed, the value of the function and derivative for each element of the 2x2 matrix (14) at a particular s is calculated. Therefore, these subroutines may be used to calculate other constants also.

A Fortran listing of the ROOTFINDER program is located in Appendix C. The roots are printed and punched onto cards when ROOTFINDER is executed.

Evaluation of z-Coefficients

Once the roots have been obtained, other constants essential to the evaluation of the z-transfer function coefficients may be found. The constants, p_2 , p_1 , u_2 , and u_1 do not depend on the roots of the function B as they are evaluated at $s = 0$. The expressions for p_2 , p_1 , u_2 , and u_1 are again listed.

$$\begin{aligned} p_2 &= \left[-\frac{A}{B} \right] \Big|_{s=0}, & p_1 &= - \left[\frac{B \frac{dA}{ds} - A \frac{dB}{ds}}{B^2} \right] \Big|_{s=0}, \\ u_2 &= \left[\frac{1}{B} \right] \Big|_{s=0}, & u_1 &= - \left[\frac{\frac{dB}{ds}}{B^2} \right] \Big|_{s=0} \end{aligned} \quad (26)$$

If zero is substituted for the variable s in the functions A , B , $\frac{dA}{ds}$, or $\frac{dB}{ds}$, indeterminate forms are obtained. However, simpler expressions may be derived that produce numerical results.

It has been shown that

$$\begin{bmatrix} A_r & B_r \\ C_r & D_r \end{bmatrix} = \begin{bmatrix} \cosh(\sqrt{s/\alpha_r} \Delta x_r) & -\frac{1}{k_r} \sqrt{\alpha_r/s} \sinh(\sqrt{s/\alpha_r} \Delta x_r) \\ -k_r \sqrt{s/\alpha_r} \sinh(\sqrt{s/\alpha_r} \Delta x_r) & \cosh(\sqrt{s/\alpha_r} \Delta x_r) \end{bmatrix}.$$

When s equals zero, the B_r term is indeterminate, but by applying L'Hospital's Rule or a series expansion the following equality may be derived.

$$\begin{bmatrix} A_r & B_r \\ C_r & D_r \end{bmatrix} \Big|_{s=0} = \begin{bmatrix} 1 & -\frac{\Delta x_r}{k_r} \\ 0 & 1 \end{bmatrix}. \quad (27)$$

By expanding, it may be seen that

$$\begin{bmatrix} A & B \\ C & D \end{bmatrix} \bigg|_{s=0} = \begin{bmatrix} 1 & -R_1 - \frac{\Delta x_1}{k_1} - \frac{\Delta x_2}{k_2} - \dots - \frac{\Delta x_n}{k_n} - R_n \\ 0 & 1 \end{bmatrix} \quad (28)$$

By differentiating, it can be shown that

$$\begin{bmatrix} \frac{dA_r}{ds} & \frac{dB_r}{ds} \\ \frac{dC_r}{ds} & \frac{dD_r}{ds} \end{bmatrix} = \begin{bmatrix} \frac{\Delta x_r}{2\sqrt{\alpha_r s}} \sinh(\sqrt{s/\alpha_r} \Delta x_r) & -\frac{\Delta x_r}{2k_r s} \cosh(\sqrt{s/\alpha_r} \Delta x_r) + \frac{1}{2k_r s} \sqrt{\alpha_r/s} \sinh(\sqrt{s/\alpha_r} \Delta x_r) \\ -\frac{k_r \Delta x_r}{2\alpha_r} \cosh(\sqrt{s/\alpha_r} \Delta x_r) - \frac{k_r}{2\sqrt{\alpha_r/s}} \Delta x_r & \frac{\Delta x_r}{2\sqrt{\alpha_r/s}} \sinh(\sqrt{s/\alpha_r} \Delta x_r) \end{bmatrix}.$$

And with techniques used in evaluation of expression (17), the much simplified result below is found.

$$\begin{bmatrix} \frac{dA_r}{ds} & \frac{dB_r}{ds} \\ \frac{dC_r}{ds} & \frac{dD_r}{ds} \end{bmatrix} \bigg|_{s=0} = \begin{bmatrix} \frac{\Delta x_r^2}{2\alpha_r} & -\frac{\Delta x_r^3}{6\alpha_r k_r} \\ -\frac{k_r \Delta x_r}{\alpha_r} & \frac{\Delta x_r^2}{2\alpha_r} \end{bmatrix} \quad (29)$$

The derivatives of the elements of expression (14) in general are

$$\begin{aligned} \begin{bmatrix} \frac{dA}{ds} & \frac{dB}{ds} \\ \frac{dC}{ds} & \frac{dD}{ds} \end{bmatrix} &= \begin{bmatrix} 1 & -R_n \\ 0 & 1 \end{bmatrix} \begin{bmatrix} \frac{dA_n}{ds} & \frac{dB_n}{ds} \\ \frac{dC_n}{ds} & \frac{dD_n}{ds} \end{bmatrix} \begin{bmatrix} A_{n-1} & B_{n-1} \\ C_{n-1} & D_{n-1} \end{bmatrix} \dots \begin{bmatrix} A_1 & B_1 \\ C_1 & D_1 \end{bmatrix} \begin{bmatrix} 1 & -R_I \\ 0 & 1 \end{bmatrix} \\ &+ \begin{bmatrix} 1 & -R_n \\ 0 & 1 \end{bmatrix} \begin{bmatrix} A_n & B_n \\ C_n & D_n \end{bmatrix} \begin{bmatrix} \frac{dA_{n-1}}{ds} & \frac{dB_{n-1}}{ds} \\ \frac{dC_{n-1}}{ds} & \frac{dD_{n-1}}{ds} \end{bmatrix} \dots \begin{bmatrix} A_1 & B_1 \\ C_1 & D_1 \end{bmatrix} \begin{bmatrix} 1 & -R_I \\ 0 & 1 \end{bmatrix} \\ &+ \dots + \begin{bmatrix} 1 & -R_n \\ 0 & 1 \end{bmatrix} \begin{bmatrix} A_n & B_n \\ C_n & D_n \end{bmatrix} \begin{bmatrix} A_{n-1} & B_{n-1} \\ C_{n-1} & D_{n-1} \end{bmatrix} \dots \\ &\dots \begin{bmatrix} \frac{dA_1}{ds} & \frac{dB_1}{ds} \\ \frac{dC_1}{ds} & \frac{dD_1}{ds} \end{bmatrix} \begin{bmatrix} 1 & -R_I \\ 0 & 1 \end{bmatrix}. \end{aligned} \quad (30)$$

Expressions (28), (29), and (30) are used separately and combined to evaluate the constants in expression (26). A subroutine, CONSTS, utilizes these expressions and finds numerical results for the constants p_2 , p_1 , u_2 , and u_1 . These constants are then used by the main program to find the z-coefficients for the transfer functions $R(z)$ and $W(z)$. In this thesis, the main program being referenced will be called Z-Coefficients.

Input to the Z-Coefficients program is N, the number of roots, NLAY, the number of structure layers, DELTA, the size of the time increment, RI, the inner surface resistance, RN, the outer surface resistance, A, the thermal diffusivity of each layer, CON, each layers specific heat, DELX, the thickness of each layer, and BETA, the roots of the function B. Once this data has been read, Z-Coefficients calls the subroutine CONSTS and thus obtains values for p_2 , p_1 , u_2 , and u_1 to be used later. The denominator polynomial is then calculated by looping through a few statements that initialize and then call a polynomial multiplication subroutine, PMPY. When this loop has been executed, the denominator coefficients are printed. Recall that $R(z)$ and $W(z)$ have the same denominators.

Two other sets of constants must be calculated before the numerator coefficients can be evaluated. These are q_m and v_m , and are evaluated at values of the roots as shown.

$$q_m = \left[-\frac{A}{s^2 \frac{dB}{ds}} \right] \bigg|_{s=-\beta_m}, \quad v_m = \left[\frac{1}{s^2 \frac{dB}{ds}} \right] \bigg|_{s=-\beta_m}$$

These constants are found with relative ease as subroutine FIGURE calculates A, B, C or D at any negative real values, subroutine DERIV calculates the derivatives at any negative real value, and the roots are already known.

Once the necessary constants have been found, the numerator coefficients may be calculated. The numerator coefficients may be found by expanding the numerators of the z-transfer functions, see expression (24), but a quicker and clearer approach is suggested in reference [2].

From equation (23),

$$\frac{A}{s^2 B} = \frac{p_2}{s^2} + \frac{p_1}{s} + \sum_{m=1}^{\infty} \left(\frac{q_m}{s + \beta_m} \right) .$$

The inverse Laplace transform of this equation will be called O , some output, and is found to be

$$O(t) = L^{-1} \left[\frac{A}{s^2 B} \right] = p_2 t + p_1 + \sum_{m=1}^{\infty} q_m e^{-\beta_m t} .$$

This equality can be evaluated for $t = \Delta, 2\Delta, \dots, k\Delta$ to find the values of the output at $O_2, O_3, \dots, O_{k+1}$. These values of the output at multiples of Δ may be recognized as the sampled values of the output function. In essence, the above equation is used to find values of the z-transform of the output, $O(z)$.

It has been shown previously that in general

$$O(z) = \frac{N(z)}{D(z)} \cdot I(z) .$$

Here we seek the numerator, $N(z)$, and

$$N(z) = \frac{D(z)}{I(z)} \cdot O(z) .$$

From expression (24), it is known that

$$D(z) = \prod_{m=1}^{\infty} (1 - e^{-\beta_m \Delta} z^{-1}), \text{ and}$$

the z-transform of a ramp input is

$$I(z) = \frac{\Delta}{z(1-z^{-1})^2} .$$

Combining,

$$N(z) = \frac{z(1-z^{-1})^2}{\Delta} \prod_{m=1}^{\infty} (1 - e^{-\beta_m \Delta} z^{-1}) \cdot O(z) .$$

This may be reduced to

$$N(z) = \frac{z(1-z^{-1})^2}{\Delta} (b_1 + b_2 z^{-1} + b_3 z^{-2} + \dots) \cdot O(z)$$

because the denominator may be expressed in the equivalent infinite series form in z^{-1} . The output may be expressed in the same form, so

$$N(z) = \frac{z(1-z^{-1})^2}{\Delta} (b_1 + b_2 z^{-1} + b_3 z^{-2} + \dots)(o_1 + o_2 z^{-1} + o_3 z^{-2} + \dots) .$$

When this equation is expanded it is found to contain a z^1 term. But, because the output at $t = 0$, o_1 is to be zero, the coefficient of this term is zero. Below, $N(z)$ is partially expanded.

$$N(z) = a_1 + a_2 z^{-1} + \dots = (o_2 b_1 + o_1 b_2 - 2o_1 b_1) + (o_3 b_1 + o_2 b_2 + o_1 b_3 - 2o_1 b_2 + o_1 b_1) z^{-1} + \dots$$

The computer program Z-Coefficients uses this concept to evaluate the numerator coefficients for the transfer functions $R(z)$ and $W(z)$. Because both transfer functions have the same denominator, many of the calculations need be performed only once. To take full advantage of the likenesses, a subroutine called THENUM was constructed. THENUM finds the coefficients for the output polynomial according to constants passed to it and then finds the numerator coefficients. A listing of Z-COEFFICIENTS is in Appendix D. The z-coefficients are punched onto cards as well as printed when the program is executed.

It would be a simple task to combine the Rootfinder and Z-Coefficient programs into a single program. However, they were not merged because roots

of a particular wall may be used with any size step in time. In other words, to obtain z-coefficients for a variety of stepsizes for one wall, the roots only need to be calculated once. If the programs were combined, the roots would have to be found each time a run was made to obtain z-coefficients for a different stepsize.

Calculation of Heat Flux

When the z-coefficients for a particular structure and stepsize have been attained, they are applied in a short iterative subprogram called FCALC that uses the equations from Table 2 to figure the heat flux at multiples of the time stepsize, Δ . Input to the subroutine is the z-coefficients, A, B, and C, the number of coefficients in the individual numerators and denominator, ITHETA, the initial wall temperature, TGO, the sampled inside temperature, TIN, the sampled outside temperature, TOUT, and the surface area of the structure, SAREA.

It has been theoretically proven that there is an infinite set of negative real roots of the function B, and therefore there is also an infinite set of numerator and denominator coefficients. Fortunately, the values of the coefficients quickly converge to zero and so those coefficients beyond some finite number of coefficients may be truncated. The resulting error will of course depend on the magnitude of the truncated numbers but should be negligible.

The FCALC subroutine is constructed in a manner such that it truncates those coefficients beyond the initial ITHETA coefficients of a numerator or denominator polynomial. The subroutine FCALC is located in Appendix E.

CHAPTER IV

APPLICATIONS

The programs described in Chapter III are quite general in nature and may be exercised on a variety of problems. This chapter deals with a few of those applications.

Two-Layer Wall

As an example, consider the case of a layered wall as described in Table 3. This particular wall was used by Kusuda [5], and also Mitalas

Table 3. Double-Layer Wall

Layer r	Material	Thermal Diffusivity (ft ² /hr)	Thermal Conductivity ($\frac{\text{BTU}}{\text{hr-ft-}^\circ\text{F}}$)	Thickness (ft)	Resistance ($\frac{\text{ft}^2\text{-}^\circ\text{F-hr}}{\text{BTU}}$)
-	Inside Surface Resistance	-	-	-	.83333
1	Common Brick	.09014	.42	.3333	-
2	Face Brick	.028	.77	.333	-
-	Outside Surface Resistance	-	-	-	.33333

and Stephenson [2]. It was used here so that this work could be verified.

When the data from Table 3 is entered into the Rootfinder program, the roots are printed, as shown in Table 4, and are also punched onto computer cards to be used by the z-coefficients program.

The z-coefficients for various time stepsizes may be computed. Tables 5 and 6 contain the z-coefficients for stepsizes of 0.1 hr and 0.2 hr, respectively for this particular wall. The z-coefficients are punched onto cards as well as printed when the z-coefficients program is executed.

Table 4. Roots of Double-Layer Wall.

RCOT S		VALUE OF FUNCTION B	DERIVATIVE OF FUNCTION B
-0.1743564895101859D	00	-0.00000000000000001	8.8940418637566510
-0.8432694983033066D	00	0.00000000000000000	-3.7797504691904740
-0.2565017965951630D	01	-0.00000000000000002	2.7572451845512920
-0.4852721524718708D	01	-0.00000000000000000	-2.5754774155284310
-0.8846706295323562D	01	-0.00000000000000004	2.4213817385476553
-0.1283071051485510D	02	-0.000000000000000040	-2.3854502222884680
-0.1912259905218523D	02	-0.000000000000000048	2.3768087035232910
-0.2497022678074264D	02	-0.000000000000000005	-2.3312875410609280
-0.3328366468070444D	02	-0.0000000000000000161	2.3970685043904460
-0.4138646432284575D	02	0.0000000000000000182	-2.3223570635453210
-0.5128558483671618D	02	-0.0000000000000000504	2.4108819580441560
-0.6208162611280464D	02	0.0000000000000000139	-2.3141199866501440
-0.7319013223035003D	02	-0.0000000000000000354	2.3854942408267920
-0.8692650202388925D	02	0.000000000000000054	-2.2977240581664350
-0.9915817991364163D	02	-0.000000000000000008	2.3341394989424200
-0.1157024765087853D	03	0.0000000000000000109	-2.2983109016393630
-0.1294076826596802D	03	-0.0000000000000000186	2.2961333670992520
-0.1482046885839709D	03	0.000000000000000057	-2.3327806523320460
-0.1641155307097936D	03	0.0000000000000000681	2.2915965398418360
-0.184355897140548D	03	-0.000000000000000017	-2.3777534023878680

ILLEGIBLE DOCUMENT

**THE FOLLOWING
DOCUMENT(S) IS OF
POOR LEGIBILITY IN
THE ORIGINAL**

**THIS IS THE BEST
COPY AVAILABLE**

Table 5. z-Coefficients for DELTA = 0.1 hr.

STEP SIZE = 0.1 HR

	NUMERATOR P(Z)	DENOMINATOR R(Z) AND W(Z)	NUMERATOR W(Z)
A(1)=	0.25914236533883D 01	B(1)=	0.163000000000000D 01
A(2)=	0.113524291856483D 02	B(2)=	0.427180655026772D 01
A(3)=	0.207224272373034D 02	B(3)=	0.759163932323560D 01
A(4)=	0.204644366666667D 02	B(4)=	0.788406950462800D 01
A(5)=	0.118955175213249D 02	B(5)=	0.410162191933619D 01
A(6)=	0.416751611747650D 01	B(6)=	0.134701357969296D 01
A(7)=	0.86886260549359D 00	B(7)=	0.274005151065630D 00
A(8)=	0.10301660234659D 00	B(8)=	0.215055550602069D 00
A(9)=	0.673334156684703D 00	B(9)=	0.193609937362597D 00
A(10)=	0.216001813894225D 00	B(10)=	0.563576423140930D 00
A(11)=	0.316777866433300D 00	B(11)=	0.786666666666666D 00
A(12)=	0.227575121022926D 00	B(12)=	0.308360465532131D 00
A(13)=	0.537970000000000D 00	B(13)=	0.705920035109217D 00
A(14)=	0.635327536463271D 00	B(14)=	0.417143451571720D 00
A(15)=	0.157790938945652D 00	B(15)=	0.685630233387361D 00
A(16)=	0.544765648484136D 00	B(16)=	0.303959580210331D 00
A(17)=	0.158724951676457D 00	B(17)=	0.203666666666666D 00
A(18)=	0.436613568666350D 00	B(18)=	0.635491522615850D 00
A(19)=	0.206253564553716D 00	B(19)=	0.234338309173647D 00
A(20)=	0.455684652276781D 00	B(20)=	0.553557439565157D 00
A(21)=	0.216646815378502D 00	B(21)=	0.600000000000000D 00
A(22)=	0.375874646301808D 00	B(22)=	0.300000000000000D 00
A(23)=	0.155489430527134D 00	B(23)=	0.600000000000000D 00
A(24)=	0.573711665571667D 00	B(24)=	0.600000000000000D 00
A(25)=	0.293073597881109D 00	B(25)=	0.600000000000000D 00
A(26)=	0.136324483017053D 00	B(26)=	0.600000000000000D 00
A(27)=	0.317273586754729D 00	B(27)=	0.600000000000000D 00
A(28)=	0.1010676294642511D 00	B(28)=	0.600000000000000D 00
A(29)=	0.297043096085012D 00	B(29)=	0.600000000000000D 00
A(30)=	0.295127603064600D 00	B(30)=	0.600000000000000D 00
A(31)=	0.175627703001091D 00	B(31)=	0.600000000000000D 00
A(32)=	0.1312473654565312D 00	B(32)=	0.600000000000000D 00
A(33)=	0.1001945310068952D 00	B(33)=	0.600000000000000D 00
A(34)=	0.1924336029988720D 00	B(34)=	0.600000000000000D 00
A(35)=	0.578895848103166D 00	B(35)=	0.600000000000000D 00
A(36)=	0.1844717681827835D 00	B(36)=	0.600000000000000D 00
A(37)=	0.0625474817126713D 00	B(37)=	0.600000000000000D 00
A(38)=	0.1374823048627084D 00	B(38)=	0.600000000000000D 00
A(39)=	0.1130006424861726D 00	B(39)=	0.600000000000000D 00
A(40)=	0.1213511748146360D 00	B(40)=	0.600000000000000D 00
A(41)=	0.1216024702296580D 00	B(41)=	0.600000000000000D 00
A(42)=	0.2057601177897362D 00	B(42)=	0.600000000000000D 00
A(43)=	0.1083856425752450D 00	B(43)=	0.600000000000000D 00
C(1)=	0.3108624468950438D -13	C(1)=	0.611799402796359D -13
C(2)=	0.2030505626872313D -12	C(2)=	0.763731654278504D -13
C(3)=	0.4150546957673754D -09	C(3)=	0.777303559149453D -13
C(4)=	0.5581915512964143D -07	C(4)=	0.793683357633766D -13
C(5)=	0.9493934405823400D -06	C(5)=	0.555063245631210D -13
C(6)=	0.4149225112678310D -05	C(6)=	0.942171405318103D -14
C(7)=	0.6189386643005929D -05	C(7)=	0.3675660476613196D -13
C(8)=	0.358129522364245D -05	C(8)=	0.5931171537338149D -13
C(9)=	0.8474771621565848D -06	C(9)=	0.665947802682597D -13
C(10)=	0.8266966236811380D -07	C(10)=	0.675157860954550D -13
C(11)=	0.3284293644661146D -08	C(11)=	0.5041649686307438D -13
C(12)=	0.4404973251167957D -10	C(12)=	0.1272486464951851D -13
C(13)=	0.3946476681534245D -12	C(13)=	0.4024591276704920D -13
C(14)=	0.1603354441777731D -12	C(14)=	0.6546626229543737D -13
C(15)=	0.1409376999264748D -12	C(15)=	0.1157095520111936D -12
C(16)=	0.8084157357513477D -13	C(16)=	0.1584587136516545D -12
C(17)=	0.199750014721717D -13	C(17)=	0.0191176921193659D -13
C(18)=	0.2094370237161521D -13	C(18)=	0.32753475305205197D -13
C(19)=	0.1732917679433173D -13	C(19)=	0.3206073697465442D -14
C(20)=	0.611799402796359D -13	C(20)=	0.163023522458466D -13
C(21)=	0.763731654278504D -13	C(21)=	0.1114127847231920D -14
C(22)=	0.777303559149453D -13	C(22)=	0.50669094522973C -14
C(23)=	0.793683357633766D -13	C(23)=	0.3065775857569649D -13
C(24)=	0.555063245631210D -13	C(24)=	0.538245115916717D -13

Table 6. z-Coefficients for DELTA = 0.2 hr.

STEP SIZE = 0.2 HR

NUMERATOR R(Z)		DENOMINATOR R(Z) AND W(Z)		NUMERATOR W(Z)	
A(1) = -0.2450318060473588D-01	A(2) = -0.7865982686652078D-01	B(1) = 0.1000000000000000D-01	B(2) = -0.3065565245174912D-01	C(1) = -0.4440892098500626D-14	C(2) = -0.2924669523143679D-07
A(3) = -0.673942252886042D-01	A(4) = -0.5856843658313248D-01	B(3) = 0.350695287650774D-01	B(4) = -0.2046433192552689D-01	C(3) = -0.5576220854313998D-05	C(4) = -0.701798763699347D-04
A(5) = -0.1777315781653922D-01	A(6) = -0.2603736619315713D-00	B(5) = 0.5795113025576784D-00	B(6) = -0.7767681174270152D-01	C(5) = -0.1788315042999248D-03	C(6) = -0.1271018409726776D-03
A(7) = -0.166499132164803D-01	A(8) = -0.4019948293106532D-03	B(7) = 0.443368345464300D-02	B(8) = -0.4522096338270362D-04	C(7) = -0.3757711814163929D-04	C(8) = -0.148669163064615D-05
A(9) = -0.3365630574504596D-05	A(10) = -0.8687345131826319D-09	B(9) = 0.4084134503388209D-06	B(10) = -0.5561494460117314D-07	C(9) = -0.3632228236882170D-07	C(10) = -0.175407673965812D-09
A(11) = -0.6259785420175267D-11	A(12) = -0.4256488951925910D-13	B(11) = 0.143434554025281D-12	B(12) = -0.473615336444310D-17	C(11) = -0.194017363953727D-12	C(12) = -0.2743461734647493D-13
A(13) = -0.152708857454231D-13	A(14) = -0.1576707517606712D-14	B(13) = 0.940655949931645D-22	B(14) = -0.7057341303644797D-29	C(13) = -0.452799189989213D-13	C(14) = -0.4052807534661126D-13
A(15) = -0.3506124476015112D-13	A(16) = -0.1636582041676212D-13	B(15) = 0.77457884191326D-36	B(16) = -0.2209426433588194D-73	C(15) = -0.353915250656492D-13	C(16) = -0.190955529119161D-13
A(17) = -0.3541456433690103D-13	A(18) = -0.670278366155314D-14	B(17) = 0.0300000000000000D-00	B(18) = 0.0300000000000000D-00	C(17) = 0.1532608603477875D-14	C(18) = -0.946122515742293D-14
A(19) = -0.1151465779380793D-13	A(20) = -0.323864504752375D-13	B(19) = 0.0000000000000000D-00	B(20) = 0.0000000000000000D-00	C(19) = 0.359145970192019D-14	C(20) = -0.30544030213331624D-14
A(21) = -0.19054460667335D-13	A(22) = -0.210467015436922D-13	B(21) = 0.0000000000000000D-00	B(22) = 0.0000000000000000D-00	C(21) = -0.23739255276655D-14	C(22) = 0.774391173939197D-15
A(23) = -0.3953576465271005D-13	A(24) = -0.22895707169746D-13	B(23) = 0.0000000000000000D-00	B(24) = 0.0000000000000000D-00	C(23) = 0.3557336213328458D-14	C(24) = -0.6929485902963416D-14
A(25) = -0.77963071470700D-13	A(26) = -0.306702747404664D-13	B(25) = 0.0000000000000000D-00	B(26) = 0.0000000000000000D-00	C(25) = 0.7917030241681344D-14	C(26) = -0.1140153746363018D-13
A(27) = -0.1477253466260343D-15	A(28) = -0.2656766464336019D-13	B(27) = 0.0000000000000000D-00	B(28) = 0.0000000000000000D-00	C(27) = 0.1212015467568196D-13	C(28) = -0.1567451452762477D-13
A(29) = -0.1224102884073722D-14	A(30) = -0.56045276165181D-13	B(29) = 0.0000000000000000D-00	B(30) = 0.0000000000000000D-00	C(29) = 0.2266225587434549D-13	C(30) = -0.2757015610577618D-13
A(31) = -0.228773658503176D-13	A(32) = -0.4274036527005435D-13	B(31) = 0.0000000000000000D-00	B(32) = 0.0000000000000000D-00	C(31) = 0.1954447479542794D-13	C(32) = -0.1530076448624841D-13
A(33) = -0.2746629366761267D-13		B(33) = 0.0000000000000000D-00	B(34) = 0.0000000000000000D-00	C(33) = 0.1442447175563824D-13	

Once the z -coefficients have been obtained, the heat flux at the inside surface, f_I may be found with the FCALC subroutine where the inside and outside temperatures are input. For this example, Figures 6 and 7 demonstrate the inside and outside temperatures. The wall was considered to have been at

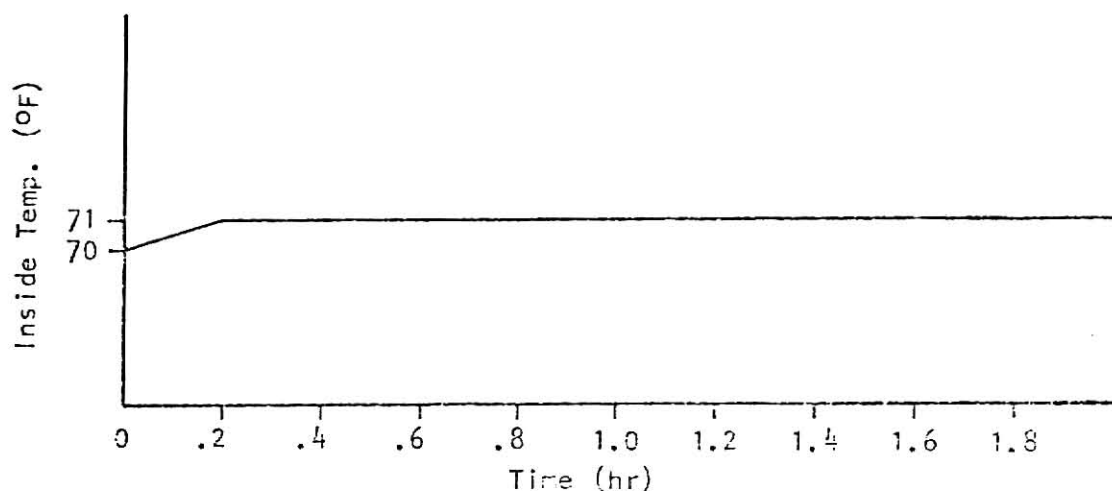


Figure 6. Inside Temperature.

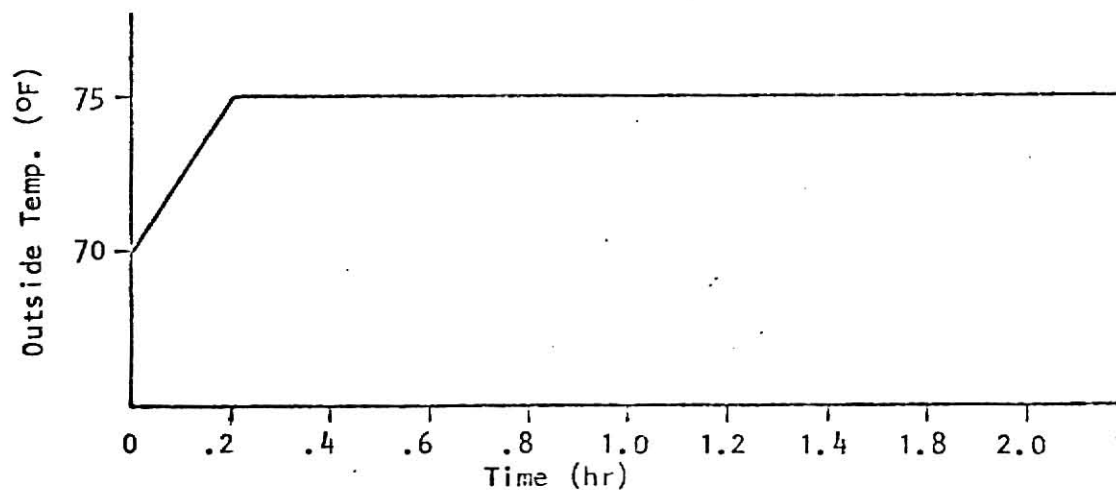


Figure 7. Outside Temperature.

an initial temperature of 70°F. Tables 7 and 8 contain the output from the FCALC subroutine for the 0.1 hr and 0.2 hr stepsizes. It may be seen that the two sets of data agree very well at the same points in time. Figure 8 is a plot of the data. As expected, the inside heat flux is immediately positive and eventually falls to negative values because of the higher outside temperature.

3-Layer Wall

For comparison, consider the three-layer wall as described by Table 9. The rootfinder program was used to obtain the roots, then the z-coefficients were obtained, and finally an output was obtained from the FCALC subroutine for the inputs used on the other wall as shown in Figures 6 and 7. The wall

Table 9. Triple-Layer Wall.

Layer	Material	Thermal Diffusivity (ft ² /hr)	Thermal Conductivity ($\frac{\text{BTU}}{\text{hr-ft-}^\circ\text{F}}$)	Thickness (ft)	Resistance ($\frac{\text{ft}^2\text{-}^\circ\text{F-hr}}{\text{BTU}}$)
-	Inside Surface Resistance	-	-	-	.83333
1	Gypsum Board	.012375	.25	.0416667	-
2	Insulation	.3015873	.19	.5	-
3	Gypsum Board	.012375	.25	.0416667	-
-	Outside Surface Resistance	-	-	-	.33333

was again assumed to have been at an initial temperature of 70°F. Table 10 contains the output of the FCALC subroutine. The responses of both walls are plotted in Figure 9. From Figure 9, it may be seen that the 3-layer wall responds faster than the 2-layer wall, and that it has a higher overall thermal resistance because of the lower heat flow at steady-state.

Table 7. Heat Flux for DELTA = 0.1 hr.

F(11) = 0.00000000000000000000 00	F(57) = 0.394276153555252790-02	F(113) = -0.10365173613266640 01	F(169) = -0.14322766415761010 01
F(21) = 0.12957119249721580 01	F(58) = -0.243440549237684980-01	F(114) = -0.10374864136262640 01	F(170) = -0.143664111081441020 01
F(31) = 0.24503180604558930 01	F(59) = -0.1582628262933190-01	F(115) = -0.10387864136262640 01	F(171) = -0.144047411613184000 01
F(41) = 0.22310621952935980 01	F(60) = -0.79617031306000960-01	F(116) = -0.10693604137676950 01	F(172) = -0.14444669012683490 01
F(51) = 0.22034581114187610 01	F(61) = -0.100660729480108360 00	F(117) = -0.1079217681616360 01	F(173) = -0.14483904764510180 01
F(61) = 0.11943726485557030 01	F(62) = -0.133178060734173730 00	F(118) = -0.1085035542663680 01	F(174) = -0.1452246634727210 01
F(71) = 0.15109043787377930 01	F(63) = -0.15232596157566120 00	F(119) = -0.1095958916873750 01	F(175) = -0.1456335549520380 01
F(81) = 0.16437717318021600 01	F(64) = -0.10505756710396980 00	F(120) = -0.11094039591504790 01	F(176) = -0.1459757658751030 01
F(91) = 0.177992115546641600 01	F(65) = -0.21333117516154660 00	F(121) = -0.11191318761377730 01	F(177) = -0.1464712227943350 01
F(101) = 0.17257301150114550 01	F(66) = -0.23528936713671080 00	F(122) = -0.11286955570660320 01	F(178) = -0.1469712430622350 01
F(111) = 0.1675495577555120 01	F(67) = -0.259779845003524140 00	F(123) = -0.11380745333857040 01	F(179) = -0.14705454813379520 01
F(121) = 0.16133313130101070 01	F(68) = -0.28160945035103650 00	F(124) = -0.114729162743226670 01	F(180) = -0.1474234494266330 01
F(131) = 0.1581767335476030 01	F(69) = -0.30762709311171410 00	F(125) = -0.1156396160603440 01	F(181) = -0.14774763257157730 01
F(141) = 0.1525573620533000 01	F(70) = -0.33355628622017750 00	F(126) = -0.11652512246311550 01	F(182) = -0.148108535400730 01
F(151) = 0.15054713103363600 01	F(71) = -0.35303293558424730 00	F(127) = -0.117399413541816980 01	F(183) = -0.148408512633856230 01
F(161) = 0.1467334752665300 01	F(72) = -0.37666921160536410 00	F(128) = -0.11829029516597210 01	F(184) = -0.1487324340765450 01
F(171) = 0.14284653501066380 01	F(73) = -0.35626210685405080 00	F(129) = -0.1191347036721140 01	F(185) = -0.149206351865383760 01
F(181) = 0.1398552555677110 01	F(74) = -0.42364882513147260 00	F(130) = -0.1199347036721140 01	F(186) = -0.14967053362937360 01
F(191) = 0.13515335050363420 01	F(75) = -0.44155132079833540 00	F(131) = -0.1207506202102650 01	F(187) = -0.14977301553652750 01
F(201) = 0.1313113278873350 01	F(76) = -0.4613559102920350 00	F(132) = -0.12155254670236210 01	F(188) = -0.15026887618269240 01
F(211) = 0.131746331835639610 01	F(77) = -0.48360745331605790 00	F(133) = -0.12236042419875470 01	F(189) = -0.1505616258255650 01
F(221) = 0.12363513827609840 01	F(78) = -0.50621112552561880 00	F(134) = -0.1231474145916630 01	F(190) = -0.1505616258255650 01
F(231) = 0.11471595526754410 01	F(79) = -0.52747276111717350 00	F(135) = -0.12390254451265660 01	F(191) = -0.1505616258255650 01
F(241) = 0.1158645549843170 01	F(80) = -0.54393635608493920 00	F(136) = -0.1246236236607600 01	F(192) = -0.15113025227143600 01
F(251) = 0.111543127003180 01	F(81) = -0.5633371747635650 00	F(137) = -0.1253585755878570 01	F(193) = -0.15147068726387450 01
F(261) = 0.103394115046440 01	F(82) = -0.582517963511000 00	F(138) = -0.12609470616325450 01	F(194) = -0.1517479630797640 01
F(271) = 0.10212185843720230 01	F(83) = -0.60119448630872750 00	F(139) = -0.126790254451265660 01	F(195) = -0.1519463562468100 01
F(281) = 0.10333045606737610 01	F(84) = -0.61761793930661250 00	F(140) = -0.1274804754581510 01	F(196) = -0.1522090527361510 01
F(291) = 0.9545571040533980 01	F(85) = -0.63772940500115710 00	F(141) = -0.12817834801396080 01	F(197) = -0.15246730441934950 01
F(301) = 0.9239102423444400 00	F(86) = -0.6555342100667060 00	F(142) = -0.12884700616325450 01	F(198) = -0.1527219533647250 01
F(311) = 0.8944028937553990 00	F(87) = -0.67333516384671130 00	F(143) = -0.12950470616325450 01	F(199) = -0.15257064157691360 01
F(321) = 0.8640693136201140 00	F(88) = -0.6932402355281850 00	F(144) = -0.1301584865919300 01	F(200) = -0.1532154842214900 01
F(331) = 0.8103382138146730 00	F(89) = -0.707151276257100 00	F(145) = -0.1307985016336620 01	F(201) = -0.15367296318014230 01
F(341) = 0.7713413617135130 00	F(90) = -0.72371739771841260 00	F(146) = -0.1314270876720620 01	F(202) = -0.15367296318014230 01
F(351) = 0.7254252745434540 00	F(91) = -0.743711392239649060 00	F(147) = -0.1320444430326260 01	F(203) = -0.15367296318014230 01
F(361) = 0.6905518239480740 00	F(92) = -0.7541307726415430 00	F(148) = -0.13265111846476060 01	F(204) = -0.1541543495575750 01
F(371) = 0.6601443668753320 00	F(93) = -0.77154985935823350 00	F(149) = -0.133267641460379610 01	F(205) = -0.1543736432100750 01
F(381) = 0.625422321221590 00	F(94) = -0.78747413594963440 00	F(150) = -0.1338333417163690 01	F(206) = -0.1545993554060350 01
F(391) = 0.5874364457005000 00	F(95) = -0.802721235148563740 00	F(151) = -0.1344034143675450 01	F(207) = -0.1548162528742950 01
F(401) = 0.5519343555051390 00	F(96) = -0.81771280920084050 00	F(152) = -0.134974499530653490 01	F(208) = -0.15502560131285360 01
F(411) = 0.516310363561030 00	F(97) = -0.834565966547180 00	F(153) = -0.1355319642199150 01	F(209) = -0.155231855571490 01
F(421) = 0.4810768740650360 00	F(98) = -0.8534052337070580 00	F(154) = -0.1360773187995580 01	F(210) = -0.1554447394933170 01
F(431) = 0.4442424351214140 00	F(99) = -0.86115498327093120 00	F(155) = -0.13661455163396050 01	F(211) = -0.1556465552217920 01
F(441) = 0.411027336533300 00	F(100) = -0.8714146166470500 00	F(156) = -0.13714272907167270 01	F(212) = -0.1558457468312920 01
F(451) = 0.3774227415675760 00	F(101) = -0.88308722567206320 00	F(157) = -0.1376820095555640 01	F(213) = -0.1560411383764750 01
F(461) = 0.342467033224420 00	F(102) = -0.902394146141170 00	F(158) = -0.138170646200750 01	F(214) = -0.1562311532756320 01
F(471) = 0.3111027198464440 00	F(103) = -0.9196761157217620 00	F(159) = -0.1386716116760720 01	F(215) = -0.1564717740660530 01
F(481) = 0.2749351032439860 00	F(104) = -0.9272613003864590 00	F(160) = -0.1391635023550660 01	F(216) = -0.1566717193304120 01
F(491) = 0.2451262512151290 00	F(105) = -0.9415515103133410 00	F(161) = -0.1396499530653490 01	F(217) = -0.15687393652964230 01
F(501) = 0.215022545733250 00	F(106) = -0.9541566427444840 00	F(162) = -0.140126183730320 01	F(218) = -0.1568626954175050 01
F(511) = 0.1832517432432620 00	F(107) = -0.9665443573066420 00	F(163) = -0.14059512292115720 01	F(219) = -0.1568626954175050 01
F(521) = 0.1511792573674680 00	F(108) = -0.977132726830490 00	F(164) = -0.14106413648422660 01	F(220) = -0.1573172674562480 01
F(531) = 0.1214854687937290 00	F(109) = -0.9866333675957160 00	F(165) = -0.14149997345353770 01	F(221) = -0.1574817471834550 01
F(541) = 0.9143676242112630-01	F(110) = -0.1002449340634270 01	F(166) = -0.14194318702329070 01	F(222) = -0.1576541699357320 01
F(551) = 0.6133097054227340-01	F(111) = -0.10133999771502410 01	F(167) = -0.1423782827675970 01	F(223) = -0.157818266433310 01
F(561) = 0.3268696762768390-01	F(112) = -0.10253539147786870 01	F(168) = -0.14280669461357860 01	F(224) = -0.1579792668471140 01

Table 8. Heat Flux for DELTA = 0.2 hr.

F(1) = 0.0000000000000000 00	F(57) = -0.10365173595231490 01	F(113) = -0.15813799538655110 01	F(169) = -0.16586969661442890 01
F(2) = 0.2450330530828740 01	F(58) = -0.1058263527612240 01	F(114) = -0.15844677517365200 01	F(170) = -0.1659135045056490 01
F(3) = 0.20599451199913750 01	F(59) = -0.1079217663333600 01	F(115) = -0.15874496913576540 01	F(171) = -0.16595581187436640 01
F(4) = 0.1410404977378180 01	F(60) = -0.10995593800334000 01	F(116) = -0.15903296393130460 01	F(172) = -0.1659566685689320 01
F(5) = 0.17789024966656800 01	F(61) = -0.111511516682510610 01	F(117) = -0.1594110471019200 01	F(173) = -0.1660361258759100 01
F(6) = 0.16764825477932220 01	F(62) = -0.1133074515283010 01	F(118) = -0.15975706247622960 01	F(174) = -0.166074623058581700 01
F(7) = 0.15977625733569430 01	F(63) = -0.115343626031489900 01	F(119) = -0.15983395566610430 01	F(175) = -0.16611132944027920 01
F(8) = 0.1506473103577770 01	F(64) = -0.11739915743004600 01	F(120) = -0.16000947785719350 01	F(176) = -0.16614756714931510 01
F(9) = 0.1423663501511540 01	F(65) = -0.11910443673004160 01	F(121) = -0.1603313555331110 01	F(177) = -0.1661735287277330 01
F(10) = 0.13515332526950390 01	F(66) = -0.12075352053112470 01	F(122) = -0.16056498413347680 01	F(178) = -0.16621403373876960 01
F(11) = 0.12746418088562410 01	F(67) = -0.12234342356791350 01	F(123) = -0.1607058649471970 01	F(179) = -0.16624603595616560 01
F(12) = 0.1197095852781110 01	F(68) = -0.12387473739441710 01	F(124) = -0.1609059735393100 01	F(180) = -0.1662765465347355 01
F(13) = 0.11149312356633710 01	F(69) = -0.12535855735347450 01	F(125) = -0.16121056180327520 01	F(181) = -0.1663062114554490 01
F(14) = 0.10321235252134830 01	F(70) = -0.12678454431963170 01	F(126) = -0.16142205358826670 01	F(182) = -0.16633562573364710 01
F(15) = 0.96455710465061230 00	F(71) = -0.12817347956477320 01	F(127) = -0.1616182456303930 01	F(183) = -0.1663641315576740 01
F(16) = 0.90743338872731140 00	F(72) = -0.12950004165511150 01	F(128) = -0.161813779126892480 01	F(184) = -0.1663935667273770 01
F(17) = 0.85193335443476330 00	F(73) = -0.1307582495682990 01	F(129) = -0.16206274060609470 01	F(185) = -0.166413725725780 01
F(18) = 0.79340677513552370 00	F(74) = -0.13204447110672170 01	F(130) = -0.162316754142419500 01	F(186) = -0.16644139725725780 01
F(19) = 0.73610134753207130 00	F(75) = -0.13324741146595950 01	F(131) = -0.1625332736427930 01	F(187) = -0.1664661315576740 01
F(20) = 0.6819366061536380 00	F(76) = -0.13460914367830360 01	F(132) = -0.1627333236427930 01	F(188) = -0.1664939924679250 01
F(21) = 0.6310026472160920 00	F(77) = -0.135951106802451160 01	F(133) = -0.16294645966392780 01	F(189) = -0.16651153835082600 01
F(22) = 0.5848255433784660 00	F(78) = -0.137361455135501110 01	F(134) = -0.16317373251635020 01	F(190) = -0.166533537767710 01
F(23) = 0.54178227905410780 00	F(79) = -0.13876035940110630 01	F(135) = -0.1633957395736450 01	F(191) = -0.16655455763554260 01
F(24) = 0.5011233576151730 00	F(80) = -0.13967141367167620 01	F(136) = -0.16361373251635020 01	F(192) = -0.166574736521470 01
F(25) = 0.4612667655343550 00	F(81) = -0.14064729159314910 01	F(137) = -0.16383755213194210 01	F(193) = -0.1665945161556350 01
F(26) = 0.4219174847373750 00	F(82) = -0.14163507273712950 01	F(138) = -0.16406181170645080 01	F(194) = -0.16661434089957390 01
F(27) = 0.3826453673387820 00	F(83) = -0.1426345732534660 01	F(139) = -0.16428755213194210 01	F(195) = -0.1666341545545530 01
F(28) = 0.3433751649579150-01	F(84) = -0.14364382476760870 01	F(140) = -0.16451281170645080 01	F(196) = -0.16665455763554260 01
F(29) = 0.30407631159474740-02	F(85) = -0.1446537665551710 01	F(141) = -0.16473755213194210 01	F(197) = -0.166674736521470 01
F(30) = 0.2647748487263930-01	F(86) = -0.1456636663031770 01	F(142) = -0.16496181170645080 01	F(198) = -0.1666945161556350 01
F(31) = 0.22547748487263930-01	F(87) = -0.14667356764327570 01	F(143) = -0.16518755213194210 01	F(199) = -0.16671434089957390 01
F(32) = 0.1861850571233240 00	F(88) = -0.147683459663031770 01	F(144) = -0.16541281170645080 01	F(200) = -0.1667341545545530 01
F(33) = 0.21037717448113740 00	F(89) = -0.148693345220153320 01	F(145) = -0.16563755213194210 01	F(201) = -0.1667541606450350 01
F(34) = 0.22547748487263930-01	F(90) = -0.1497034792797990 01	F(146) = -0.16586181170645080 01	F(202) = -0.16677434089957390 01
F(35) = 0.24057705176159370 00	F(91) = -0.15071353855446450 01	F(147) = -0.16608615268367120 01	F(203) = -0.1667942135528280 01
F(36) = 0.25567705176159370 00	F(92) = -0.15172363274416440 01	F(148) = -0.16631081170645080 01	F(204) = -0.16681434089957390 01
F(37) = 0.27077705176159370 00	F(93) = -0.15273373525116440 01	F(149) = -0.1665350566769540 01	F(205) = -0.1668341545545530 01
F(38) = 0.28587705176159370 00	F(94) = -0.15374383824427430 01	F(150) = -0.1667593438945790 01	F(206) = -0.16685455763554260 01
F(39) = 0.30097705176159370 00	F(95) = -0.15475394132416440 01	F(151) = -0.1669836306660610 01	F(207) = -0.166874736521470 01
F(40) = 0.31607705176159370 00	F(96) = -0.15576404429445370 01	F(152) = -0.1672079505877110 01	F(208) = -0.1668945161556350 01
F(41) = 0.33117705176159370 00	F(97) = -0.15677414736474740 01	F(153) = -0.167432579477760 01	F(209) = -0.16691434089957390 01
F(42) = 0.34627705176159370 00	F(98) = -0.15778424932445370 01	F(154) = -0.1676568361145450 01	F(210) = -0.1669341545545530 01
F(43) = 0.36137705176159370 00	F(99) = -0.15879435129445370 01	F(155) = -0.167880515268367120 01	F(211) = -0.166953952527110 01
F(44) = 0.37647705176159370 00	F(100) = -0.15980445324445370 01	F(156) = -0.16810481365367120 01	F(212) = -0.166973752527110 01
F(45) = 0.39157705176159370 00	F(101) = -0.16081455619445370 01	F(157) = -0.1683290566769540 01	F(213) = -0.166993552527110 01
F(46) = 0.40667705176159370 00	F(102) = -0.16182465914445370 01	F(158) = -0.168553257947760 01	F(214) = -0.167013352527110 01
F(47) = 0.42177705176159370 00	F(103) = -0.16283476209445370 01	F(159) = -0.1687775081266570 01	F(215) = -0.167033152527110 01
F(48) = 0.43687705176159370 00	F(104) = -0.16384486504445370 01	F(160) = -0.16899975947760 01	F(216) = -0.167052952527110 01
F(49) = 0.45197705176159370 00	F(105) = -0.16485496799445370 01	F(161) = -0.1692219473643150 01	F(217) = -0.167072752527110 01
F(50) = 0.46707705176159370 00	F(106) = -0.16586507094445370 01	F(162) = -0.1694439361145450 01	F(218) = -0.167092552527110 01
F(51) = 0.48217705176159370 00	F(107) = -0.16687517389445370 01	F(163) = -0.1696659257947760 01	F(219) = -0.167112352527110 01
F(52) = 0.49727705176159370 00	F(108) = -0.16788527684445370 01	F(164) = -0.16988791664218460 01	F(220) = -0.167132152527110 01
F(53) = 0.51237705176159370 00	F(109) = -0.16889537979445370 01	F(165) = -0.1701099052504270 01	F(221) = -0.167151952527110 01
F(54) = 0.52747705176159370 00	F(110) = -0.16990548274445370 01	F(166) = -0.170331852527110 01	F(222) = -0.167171752527110 01
F(55) = 0.54257705176159370 00	F(111) = -0.17091558569445370 01	F(167) = -0.170553794445370 01	F(223) = -0.167191552527110 01
F(56) = 0.55767705176159370 00	F(112) = -0.17192568864445370 01	F(168) = -0.170775736445370 01	F(224) = -0.167211352527110 01

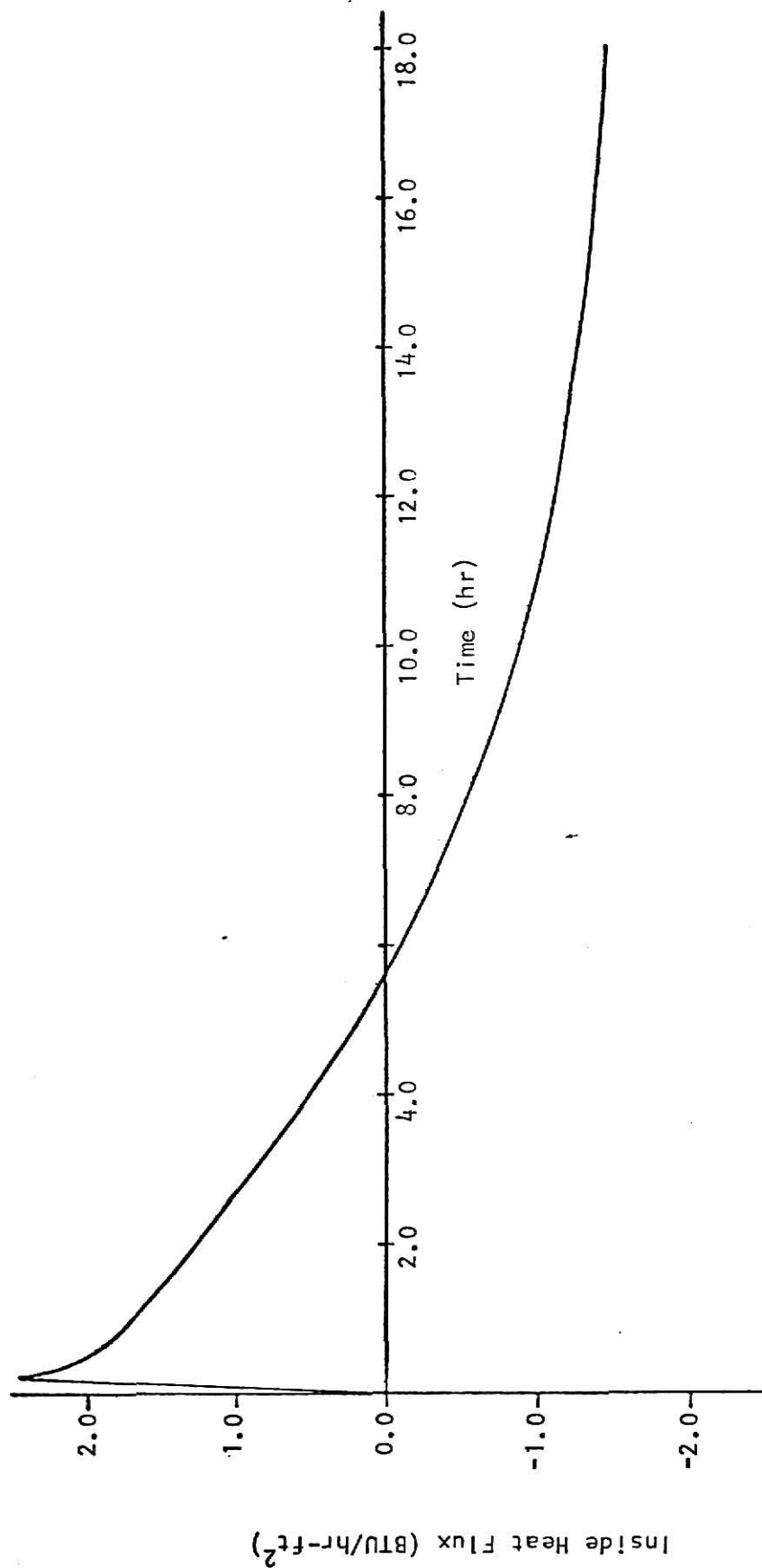


Figure 8. Heat Flux Response of Double-Layer Wall.

Table 10. Heat Flux for 3-Layer Wall.

F1	11	0.000000000000000000	F1	57	-0.96680528567491660	F1	113	-0.9681538596520080	F1	169	-0.96815436576585470
F1	21	0.11207930717809500	F1	58	-0.96693254569331460	F1	114	-0.96915392644488210	F1	170	-0.96815436576585470
F1	31	0.14575795473286550	F1	59	-0.96711305149065500	F1	115	-0.96815392644488210	F1	171	-0.96815436576585470
F1	41	0.14614663691193850	F1	60	-0.96727025338461220	F1	116	-0.96815392644488210	F1	172	-0.96815436576585470
F1	51	0.11226333439555990	F1	61	-0.96728864158936020	F1	117	-0.96815392644488210	F1	173	-0.96815436576585470
F1	61	0.04111831166114300	F1	62	-0.9673473273101900	F1	118	-0.96815392644488210	F1	174	-0.96815436576585470
F1	71	0.00375613525204900	F1	63	-0.96737496761541170	F1	119	-0.96815392644488210	F1	175	-0.96815436576585470
F1	81	0.39757559926959710	F1	64	-0.96746765656554830	F1	120	-0.96815392644488210	F1	176	-0.96815436576585470
F1	91	0.39757559926959710	F1	65	-0.96746765656554830	F1	121	-0.96815392644488210	F1	177	-0.96815436576585470
F1	101	0.39757559926959710	F1	66	-0.96746765656554830	F1	122	-0.96815392644488210	F1	178	-0.96815436576585470
F1	111	-0.19747123447162460	F1	67	-0.96746765656554830	F1	123	-0.96815392644488210	F1	179	-0.96815436576585470
F1	121	-0.19747123447162460	F1	68	-0.96746765656554830	F1	124	-0.96815392644488210	F1	180	-0.96815436576585470
F1	131	-0.19747123447162460	F1	69	-0.96746765656554830	F1	125	-0.96815392644488210	F1	181	-0.96815436576585470
F1	141	-0.19747123447162460	F1	70	-0.96746765656554830	F1	126	-0.96815392644488210	F1	182	-0.96815436576585470
F1	151	-0.47359115525204900	F1	71	-0.96746765656554830	F1	127	-0.96815392644488210	F1	183	-0.96815436576585470
F1	161	-0.53313790715664110	F1	72	-0.96746765656554830	F1	128	-0.96815392644488210	F1	184	-0.96815436576585470
F1	171	-0.53313790715664110	F1	73	-0.96746765656554830	F1	129	-0.96815392644488210	F1	185	-0.96815436576585470
F1	181	-0.6374763072475570	F1	74	-0.96746765656554830	F1	130	-0.96815392644488210	F1	186	-0.96815436576585470
F1	191	-0.5927333750358610	F1	75	-0.96746765656554830	F1	131	-0.96815392644488210	F1	187	-0.96815436576585470
F1	201	-0.733345437011600	F1	76	-0.96746765656554830	F1	132	-0.96815392644488210	F1	188	-0.96815436576585470
F1	211	-0.75293713064633070	F1	77	-0.96746765656554830	F1	133	-0.96815392644488210	F1	189	-0.96815436576585470
F1	221	-0.70122903506713120	F1	78	-0.96746765656554830	F1	134	-0.96815392644488210	F1	190	-0.96815436576585470
F1	231	-0.3376336341191100	F1	79	-0.96746765656554830	F1	135	-0.96815392644488210	F1	191	-0.96815436576585470
F1	241	-0.273345437011600	F1	80	-0.96746765656554830	F1	136	-0.96815392644488210	F1	192	-0.96815436576585470
F1	251	-0.447154635773615	F1	81	-0.96746765656554830	F1	137	-0.96815392644488210	F1	193	-0.96815436576585470
F1	261	-0.3613123939106450	F1	82	-0.96746765656554830	F1	138	-0.96815392644488210	F1	194	-0.96815436576585470
F1	271	-0.273345437011600	F1	83	-0.96746765656554830	F1	139	-0.96815392644488210	F1	195	-0.96815436576585470
F1	281	-0.273345437011600	F1	84	-0.96746765656554830	F1	140	-0.96815392644488210	F1	196	-0.96815436576585470
F1	291	-0.273345437011600	F1	85	-0.96746765656554830	F1	141	-0.96815392644488210	F1	197	-0.96815436576585470
F1	301	-0.273345437011600	F1	86	-0.96746765656554830	F1	142	-0.96815392644488210	F1	198	-0.96815436576585470
F1	311	-0.273345437011600	F1	87	-0.96746765656554830	F1	143	-0.96815392644488210	F1	199	-0.96815436576585470
F1	321	-0.273345437011600	F1	88	-0.96746765656554830	F1	144	-0.96815392644488210	F1	200	-0.96815436576585470
F1	331	-0.273345437011600	F1	89	-0.96746765656554830	F1	145	-0.96815392644488210	F1	201	-0.96815436576585470
F1	341	-0.273345437011600	F1	90	-0.96746765656554830	F1	146	-0.96815392644488210	F1	202	-0.96815436576585470
F1	351	-0.273345437011600	F1	91	-0.96746765656554830	F1	147	-0.96815392644488210	F1	203	-0.96815436576585470
F1	361	-0.273345437011600	F1	92	-0.96746765656554830	F1	148	-0.96815392644488210	F1	204	-0.96815436576585470
F1	371	-0.273345437011600	F1	93	-0.96746765656554830	F1	149	-0.96815392644488210	F1	205	-0.96815436576585470
F1	381	-0.273345437011600	F1	94	-0.96746765656554830	F1	150	-0.96815392644488210	F1	206	-0.96815436576585470
F1	391	-0.273345437011600	F1	95	-0.96746765656554830	F1	151	-0.96815392644488210	F1	207	-0.96815436576585470
F1	401	-0.273345437011600	F1	96	-0.96746765656554830	F1	152	-0.96815392644488210	F1	208	-0.96815436576585470
F1	411	-0.273345437011600	F1	97	-0.96746765656554830	F1	153	-0.96815392644488210	F1	209	-0.96815436576585470
F1	421	-0.273345437011600	F1	98	-0.96746765656554830	F1	154	-0.96815392644488210	F1	210	-0.96815436576585470
F1	431	-0.273345437011600	F1	99	-0.96746765656554830	F1	155	-0.96815392644488210	F1	211	-0.96815436576585470
F1	441	-0.273345437011600	F1	100	-0.96746765656554830	F1	156	-0.96815392644488210	F1	212	-0.96815436576585470
F1	451	-0.273345437011600	F1	101	-0.96746765656554830	F1	157	-0.96815392644488210	F1	213	-0.96815436576585470
F1	461	-0.273345437011600	F1	102	-0.96746765656554830	F1	158	-0.96815392644488210	F1	214	-0.96815436576585470
F1	471	-0.273345437011600	F1	103	-0.96746765656554830	F1	159	-0.96815392644488210	F1	215	-0.96815436576585470
F1	481	-0.273345437011600	F1	104	-0.96746765656554830	F1	160	-0.96815392644488210	F1	216	-0.96815436576585470
F1	491	-0.273345437011600	F1	105	-0.96746765656554830	F1	161	-0.96815392644488210	F1	217	-0.96815436576585470
F1	501	-0.273345437011600	F1	106	-0.96746765656554830	F1	162	-0.96815392644488210	F1	218	-0.96815436576585470
F1	511	-0.273345437011600	F1	107	-0.96746765656554830	F1	163	-0.96815392644488210	F1	219	-0.96815436576585470
F1	521	-0.273345437011600	F1	108	-0.96746765656554830	F1	164	-0.96815392644488210	F1	220	-0.96815436576585470
F1	531	-0.273345437011600	F1	109	-0.96746765656554830	F1	165	-0.96815392644488210	F1	221	-0.96815436576585470
F1	541	-0.273345437011600	F1	110	-0.96746765656554830	F1	166	-0.96815392644488210	F1	222	-0.96815436576585470
F1	551	-0.273345437011600	F1	111	-0.96746765656554830	F1	167	-0.96815392644488210	F1	223	-0.96815436576585470
F1	561	-0.273345437011600	F1	112	-0.96746765656554830	F1	168	-0.96815392644488210	F1	224	-0.96815436576585470

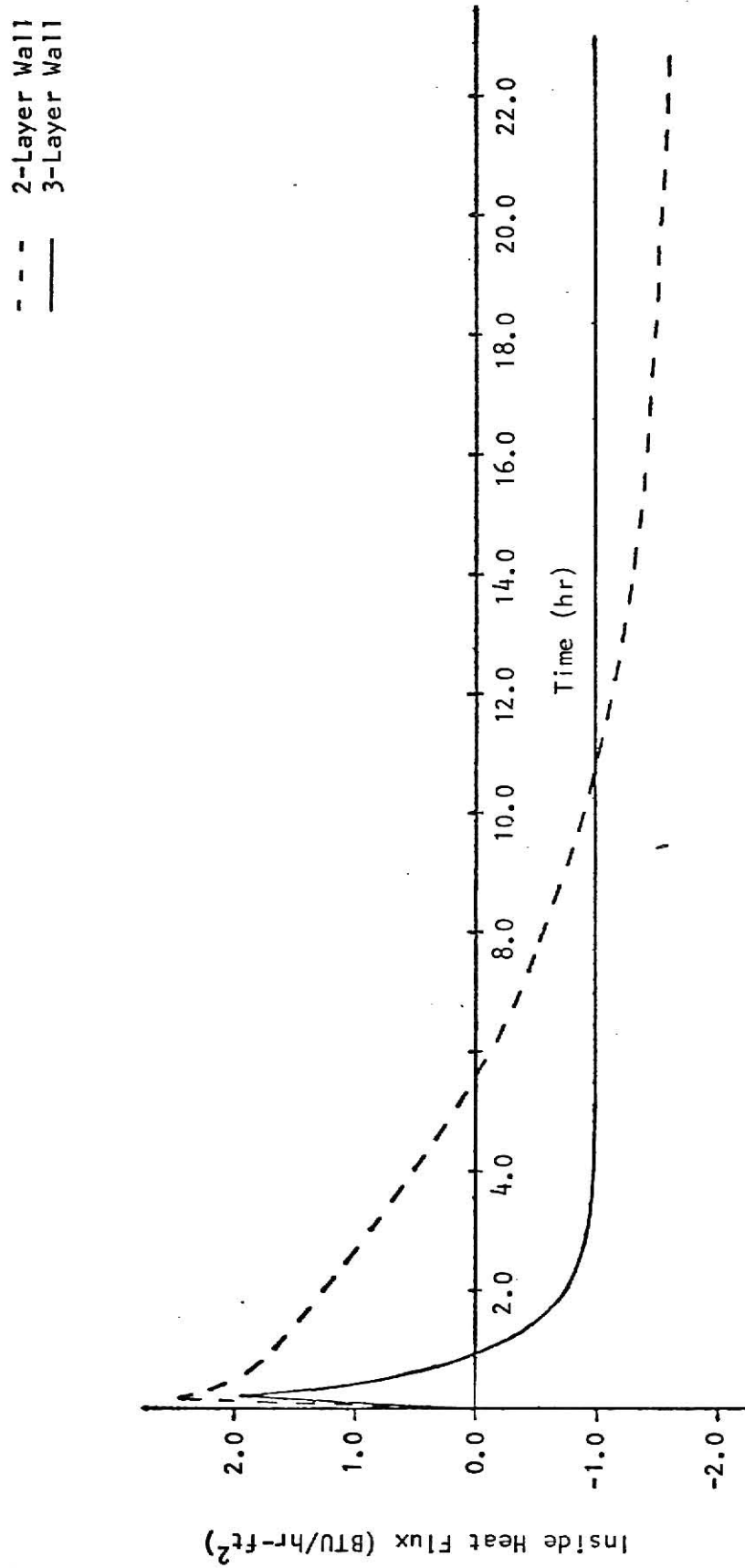


Figure 9. Heat Fluxes of 2-Layer and 3-Layer Walls.

Temperature Control System

As a final application the heat conduction transfer functions will be used in the model of the temperature control system illustrated in Figure 10.

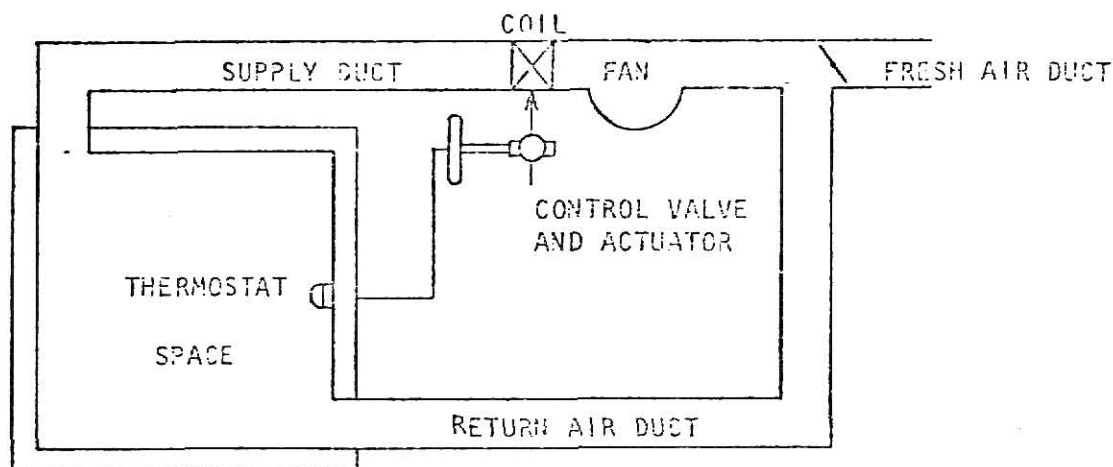


Figure 10. Air Conditioning Control System.

The transfer functions are used to simulate the walls while the rest of the model is developed in Appendix F. The time delays considered in this demonstration are the thermal lag at the coil, the space lag, and the lag of the walls. Other time delays are considered negligible. A simplified block diagram of the system is shown in Figure 11. The heat flow deviation into the space, F_I , and the space temperature deviation, V_R , are the desired responses. To obtain these values, a Runge-Kutta numerical integration technique is employed [13]. The heat flux at the wall is simultaneously calculated with the heat conduction transfer function algorithm. Steady-state values are used to initialize the variables of the control system. The system is excited by changing some parameter, most probably the thermostatic setpoint or the outside temperature. Subroutine FCALC is

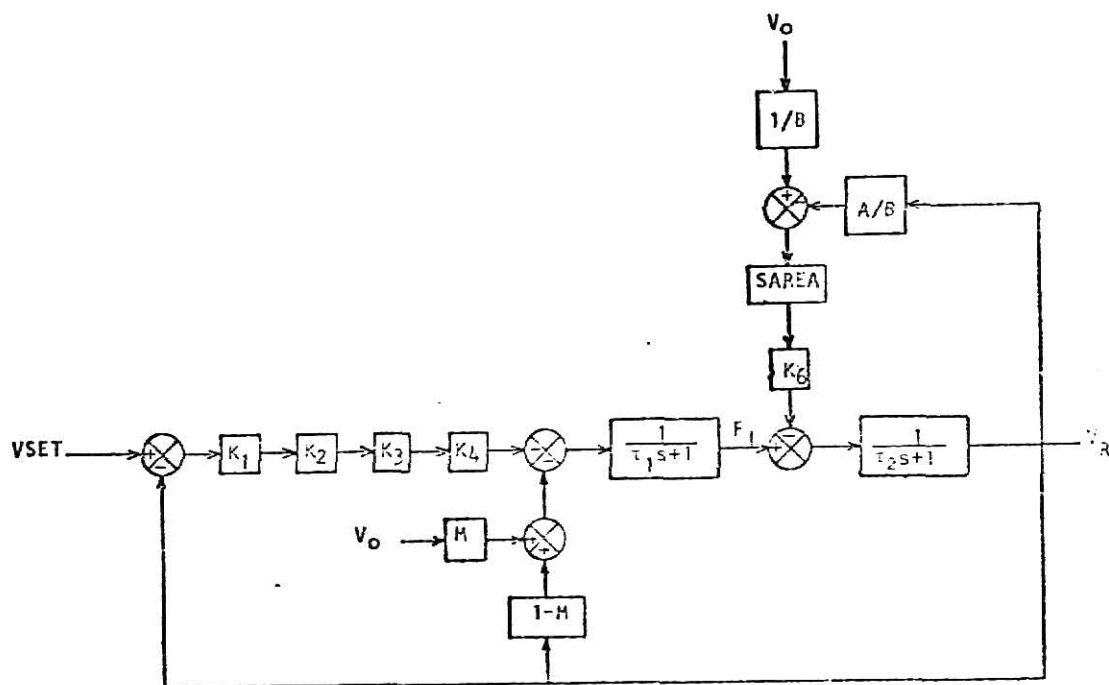


Figure 11. Air Conditioning Control System Block Diagram.

executed to derive an inside heat flux. This value is used by the subroutine FCT to calculate values for the derivatives of the variables being integrated during a finite time stepsize which is specified by the user. A new heat flux is calculated at the beginning of each step to be used for the calculation of the derivatives during that step. The time stepsizes may be split into an integral number of smaller stepsizes. The Runge-Kutta integration is then operated over these smaller stepsizes for increased stability. Stepsize depends on the system constants and the input. For small time constants and rapidly changing input, small stepsizes for the calculation of the heat flux are necessary. These steps may be broken into four to ten smaller steps for the integration technique. Larger increments may be used for less stringent systems and inputs. Appendix G contains a listing of the computer simulation for the above system.

Constants were derived according to Appendix F and references [14] and [15]. The constants used for the following examples are for a 9' x 12' x 20' room with one exterior wall. Values of the constants used are shown below. Constant values may vary widely, but care should be exercised as the Runge-Kutta integration scheme may become unstable for some sets of constants, as previously discussed. The walls are comprised of the materials as described in Table 3.

Table 11. Air Conditioning Control System Constants.

Description	Constant	Value
Thermostat gain	K_1	6.5 psi/°F
Actuator gain	K_2	0.15 in/psi
Valve gain	K_3	2481.75 BTU/hr/in
Coil gain	K_4	2.273×10^{-3} °F-hr/BTU
Gain of room	K_6	2.273×10^{-3} °F-hr/BTU
Make-up air ratio	M	$0.2 \text{ ft}^3/\text{ft}^3$
Exterior wall surface area	SAREA	250.0 ft^2
Time constant of coil	τ_1	0.022 hr
Time constant of room	τ_2	0.08 hr

It is most convenient to start the simulation with steady-state values and then allow some parameter, R, the set point, or θ_o , the outside temperature, to deviate from its initial value. Steady-state values may be obtained as follows.

The differential equations describing the system in Figure 11 may be written as

$$\frac{df_I}{dt} = [(1-M)V_R + MV_o + \text{CON}(V_{\text{SET}} - V_R) - f_I]/\tau_1 \quad \text{and} \quad \frac{dV_R}{dt} = (f_I - k_6 F_o - V_R)/\tau_2 .$$

f_I - heat flow deviation into the air space supplied from the inlet duct

$$CON = K_1 K_2 K_3 K_4$$

In the steady-state, the derivatives are equal to zero and the differential equations reduce to

$$f_I = (1-M)V_R + MV_O + CON(VSET - V_R) \quad \text{and} \quad f_I = k_6 F_O + V_R .$$

It is also known that in the steady-state

$$f_O = u(\theta_R - \theta_O) , \quad \text{where}$$

u - overall thermal conductance of the wall.

The overall thermal conductance may be calculated for a multi-layer structure and surface resistances with the equation

$$u = \frac{1}{R_1 + \frac{\Delta x_1}{k_1} + \frac{\Delta x_2}{k_2} + \dots + \frac{\Delta x_n}{k_n} + R_n} . \quad [8]$$

Once values of the constants have been selected, steady-state values of f_I , θ_R , and f_O may be calculated.

For the first example, the simulation was started from the steady-state condition where the inside temperature, outside temperature, and set point all equal 70°F. The thermostat set point is then increased to 75°F. Figure 12 is a plot of the room temperature deviation from the initial 70°F. It may be observed that the room temperature increases quickly, falls slightly, and then very gradually increases to a new steady-state condition.

As a final example, the system was started from the same steady-state at 70°F. This time the outside temperature was reduced to 50°F according to Figure 13 and held constant. Figure 14 is a plot of f_I , the heat input to the space, and f_O , the heat loss through the walls. Both responses have

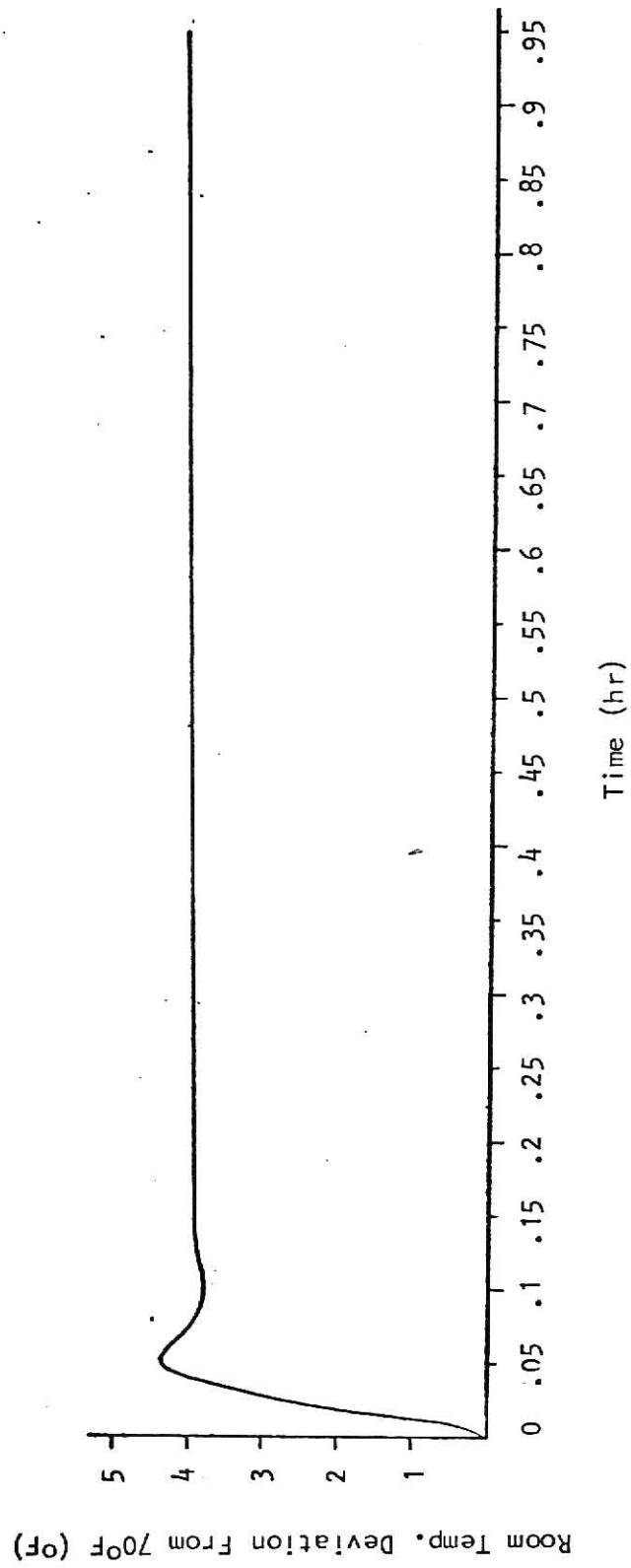


Figure 12. Room Temperature Deviation for 75°F Setpoint.

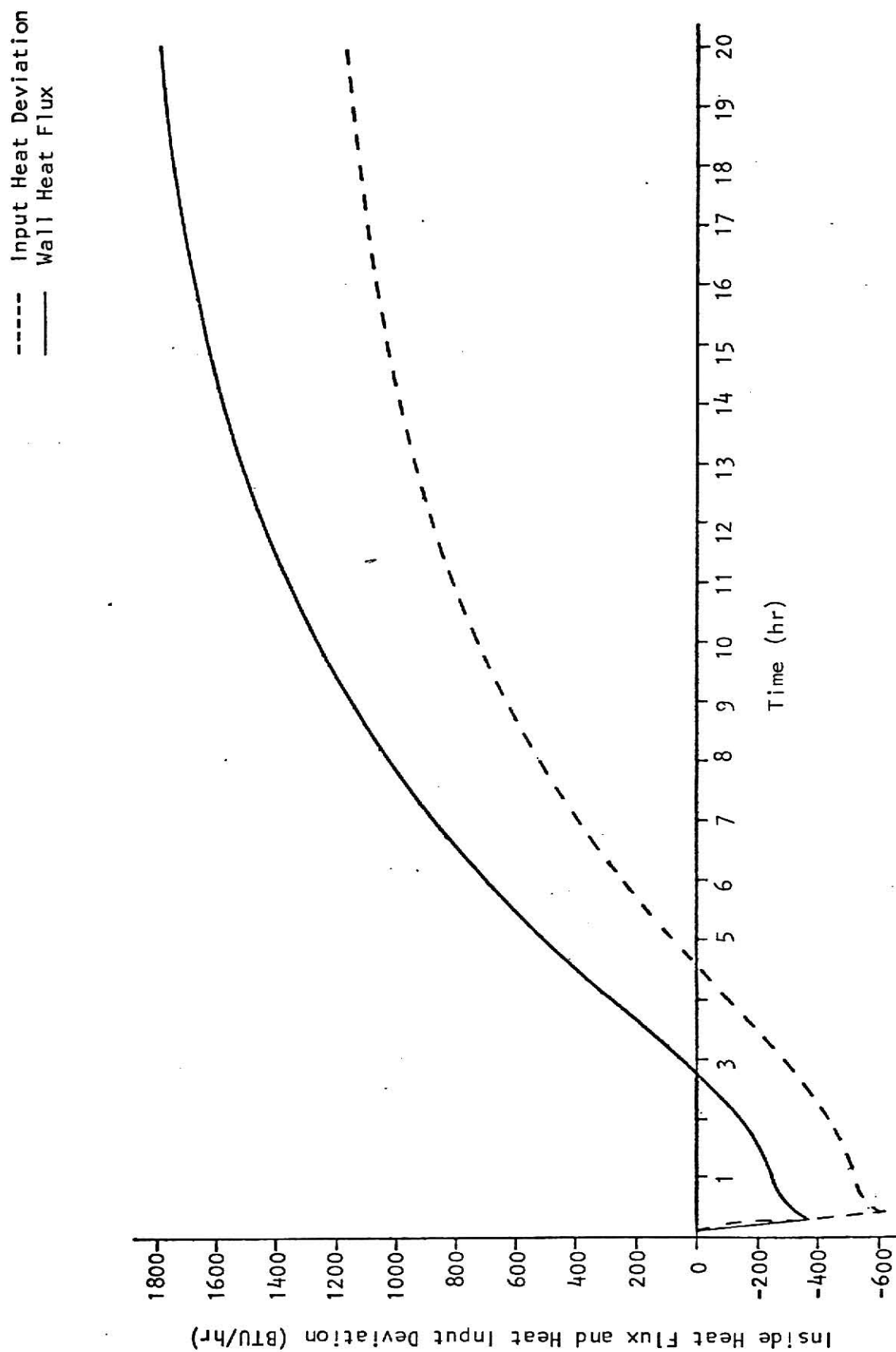


Figure 14. Inside Heat Flux and Heat Input Deviation for 50°F Outside Temperature.

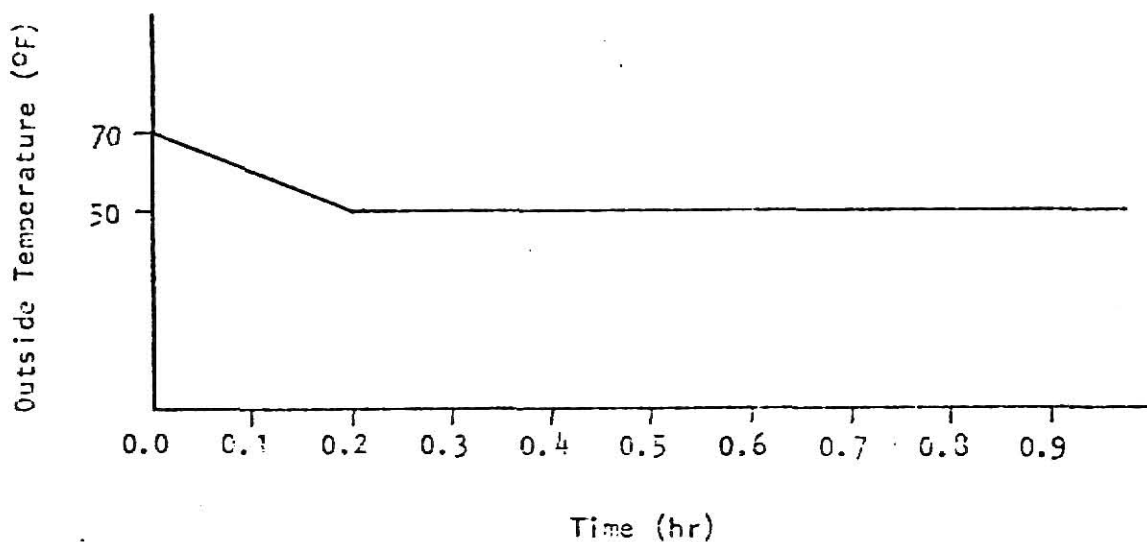


Figure 13. Outside Temperature Profile.

the same general form, and both immediately fall to negative values before reaching positive steady-state values. The heat input to the room is initially negative because the air being supplied to the rooms consists partly of 50°F outside air as well as return air. This air mixture is not as warm as the air being removed resulting in a cooler inside space temperature. The walls are initially at 70°F and begin to transfer stored heat to the cooler air resulting in negative values of f_o . Eventually, the stored heat in the walls is exhausted and heat begins to flow from the room to the walls. Meanwhile, the drop in room temperature is sensed and the heating system is activated resulting in positive values of f_i . The inside temperature deviation from the initial 70°F is plotted in Figure 15. The temperature immediately drops because of the cooler mixed air pouring into the room, and shows a slight increase as the coil starts to heat the cool air. Eventually, the temperature levels to a lower steady-state

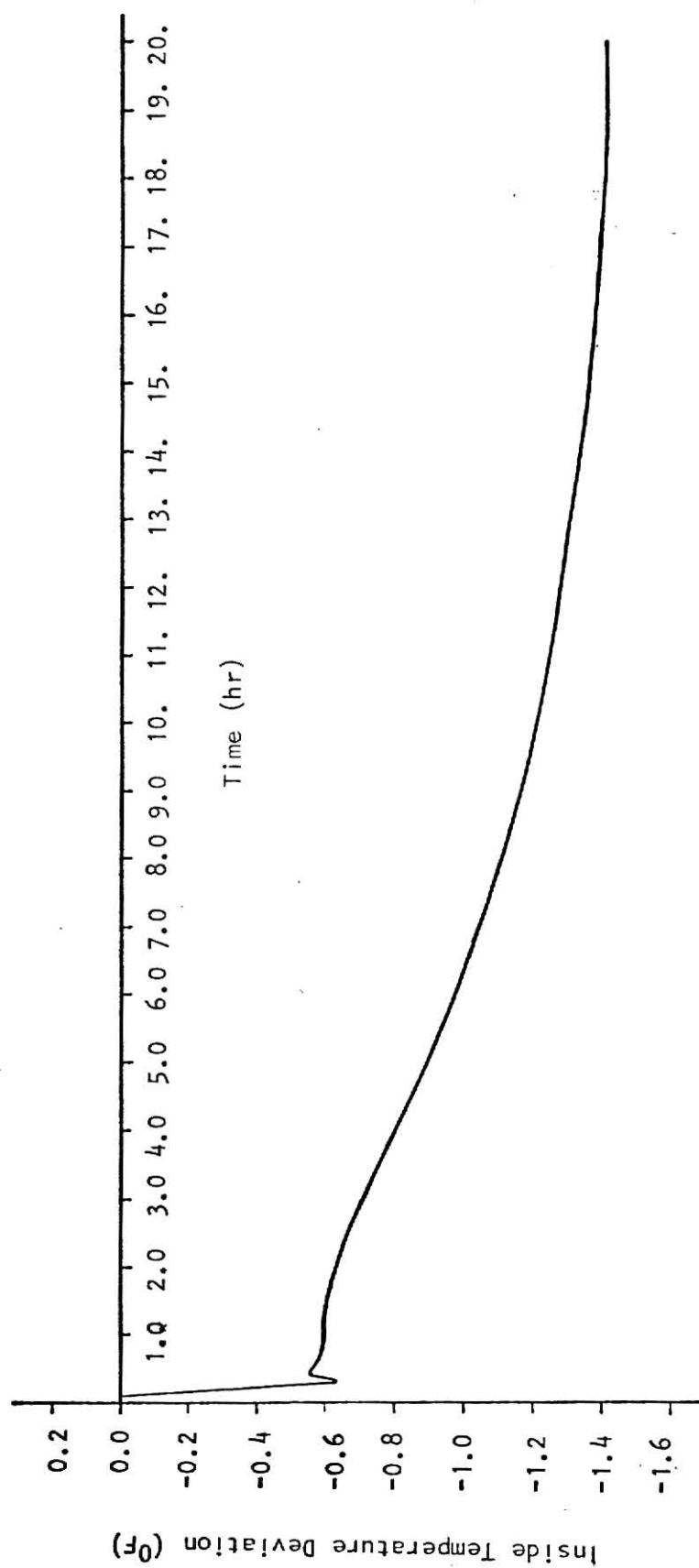


Figure 15. Room Temperature Deviation for 50°F Outside Temperature.

temperature, demonstrating approximately 1.5°F offset. The heat flow into the space, the heat loss through the walls, and the space temperature all approach new steady-state values.

These applications have been included to demonstrate the usefulness of the heat conduction algorithm. Constant input temperatures as employed in the examples are not necessary. Practically all input forms could be accurately approximated by discrete values with small time increments.

CHAPTER V

CONCLUSION

An algorithm for the calculation of heat conduction in multi-layer structures has been derived, calculated, and demonstrated in this thesis. This algorithm may be applied to walls of any number of layers and may include thermal resistances at the inner and outer surfaces of the wall. The algorithm has a variable time increment and has been tested for increments as small as 0.025 hr. Input to the algorithm is discrete values of the inside and outside surface temperatures at multiples of the time increment. Accuracy may be specified by the user and depends primarily upon truncation errors. The algorithm's strongest point is speed. For time stepsizes of reasonable size, 0.1 hr - 1.0 hr., the algorithm requires little computing time and is therefore inexpensive to use. The algorithm is well suited for applications in which a wall or set of walls are to be studied a number of times. This advantage makes it recommendable for use in the modeling of buildings and simulation of control systems. The algorithm is easily applied to the analysis of dynamic control systems to obtain system responses quickly and cheaply, where the time stepsize is quite small. The stepsize may be adjusted according to the dynamics of the system. For instance, a system with large time constants could be analyzed with a larger stepsize than one with short time constants. As smaller stepsizes are required, the number of z-coefficients must be increased to keep truncation errors to a minimum. If too few coefficients are employed or too large a stepsize is used, results may be erratic. As the time stepsize is decreased, more roots are necessary to calculate the z-coefficients to sustain good accuracy. The larger sets of

z-coefficients for very small stepsizes require extra computing time, and thus the algorithm's advantages diminish. It has been found that stepsizes smaller than 0.025 hr may produce unreasonable results with too few roots, and the computing time required makes other techniques more enticing. However, for many practical problems stepsizes smaller than 0.1 hr are unnecessary and so the heat conduction transfer function algorithm may be quite advantageous.

LIST OF REFERENCES

1. "Controls Seen as Quickest Energy Retrofit Payback," Air Cond., Heating, and Refrigeration News, February, 1977.
2. Mitalas, G. P., and D. G. Stephenson, "Calculation of Heat Conduction Transfer Functions for Multi-Layer Slabs," ASHRAE Transactions, Vol. 77, Part II, 1971.
3. Nessi, A. and L. Nisolle, "Régimes variables de fonctionnement dans les installations de chauffage central," DUNOD, 1925; and "Résolution pratique des problèmes de discontinuité de fonctionnement dans les installations de chauffage central," DUNOD, 1933.
4. Mackey, C. O. and L. T. Wright, "Periodic Heat Flow - Composite Walls or Roofs," ASHRAE Transactions, Vol. 52, 1946.
5. Kusuda, T., "Thermal Response Factors for Multi-Layer Structures of Various Heat Conduction Systems," ASHRAE Transactions, Vol. 75, Part I, 1969.
6. Mitalas, G. P., and J. G. Arseneault, Fortran IV Program to Calculate Heat Flux Response Factors for Multi-Layer Slabs, National Research Council of Canada, Division of Building Research, 1967.
7. Schenck, Hilbert J., Fortran Methods in Heat Flow, The Ronald Press Company, New York, New York, 1963.
8. Holman, J. P., Heat Transfer, 3rd ed., McGraw-Hill, New York, 1972.
9. Dorf, Richard C. Modern Control Systems, 2nd ed., Addison-Wesley, Reading, Mass., 1974.
10. Churchill, R. V., Fourier Series and Boundary Value Problems, 2nd ed., McGraw-Hill, New York, 1963.
11. Carslaw, H. S., and J. C. Jaeger, Conduction of Heat in Solids, 2nd ed., Oxford University Press, Ely House, London, 1973.
12. Ogata, Katsuhiko, Modern Control Engineering, Prentice-Hall, Inc., Englewood Cliffs, N.J., 1970.
13. Ralston, A. and H. S. Wilf, Mathematical Methods for Digital Computers, Wiley, New York, London, 1960.
14. Shih, H. Y., "Control Systems and Principals," Powers Regulator Company, Northbrook, Ill., 1970.
15. Pearson, J. T., Leonard, R. G., and McCutchan, R. D., "Gain and Time Constant for Finned Serpentine Crossflow Heat Exchangers," ASHRAE Transactions, Vol. 80, Part II, 1974.

APPENDIX A - ROOTS OF B=0.

An indication as to the position of the roots of the function B may be gained by observing the stability of a multi-layer walls response. Obviously, a wall displays extremely stable characteristics. Therefore, it may be deduced that there are no roots in the right-half of the s-plane [12].

The possible root locations may be narrowed further by algebraically investigating the function B. B is composed of a series of sinh and cosh terms and depends on the number of layers in the wall. Initially, the values of the individual terms of the 2x2 matrices composing B were examined by allowing s to be zero, a positive real, complex, and a negative real variable. A function B was then expanded for a multi-layer wall and s was again allowed to be zero, positive real, etc. Cancellation of terms due to sign differences was also probed.

For a two-layer wall the hyperbolic function B is

$$B = -\frac{\sqrt{\alpha_2}}{k_2 \sqrt{s}} \cosh\left(\frac{\Delta x_1}{\sqrt{\alpha_1}} \sqrt{s}\right) \sinh\left(\frac{\Delta x_2}{\sqrt{\alpha_2}} \sqrt{s}\right) - \frac{\sqrt{\alpha_1}}{k_1 \sqrt{s}} \cosh\left(\frac{\Delta x_2}{\sqrt{\alpha_2}} \sqrt{s}\right) \sinh\left(\frac{\Delta x_1}{\sqrt{\alpha_1}} \sqrt{s}\right) .$$

And, when B=0, to find the roots, the following equation is found.

$$\frac{k_1}{k_2} \tanh\left(\frac{\Delta x_2}{\sqrt{\alpha_2}} \sqrt{s}\right) + \frac{\alpha_1}{\alpha_2} \tanh\left(\frac{\Delta x_1}{\sqrt{\alpha_1}} \sqrt{s}\right) = 0$$

If s were some complex variable, the square root of s is also a complex variable which will be called c+id. Then

$$\frac{k_1}{k_2} \tanh\left[\frac{\Delta x_2}{\sqrt{\alpha_2}} (c+id)\right] + \frac{\alpha_1}{\alpha_2} \tanh\left[\frac{\Delta x_1}{\sqrt{\alpha_1}} (c+id)\right] = 0 .$$

From this, it may be shown that values of c and d cannot be found so that s could be a complex variable. The other variable cases were examined in

like manner. It was concluded that the function B has an infinite set of roots all of which lie on the negative real axis in the s -plane.

APPENDIX B - EQUIVALENT Z-TRANSFORMATION TECHNIQUES

In this Appendix it will be demonstrated that the output of a simple transfer function, $G(s)$, with a triangular pulse input is equivalent to the output of a transfer function developed from $G(s)$ by assuming a ramp input and using a weighted impulse input instead.

A triangular pulse input, v , is pictured below.

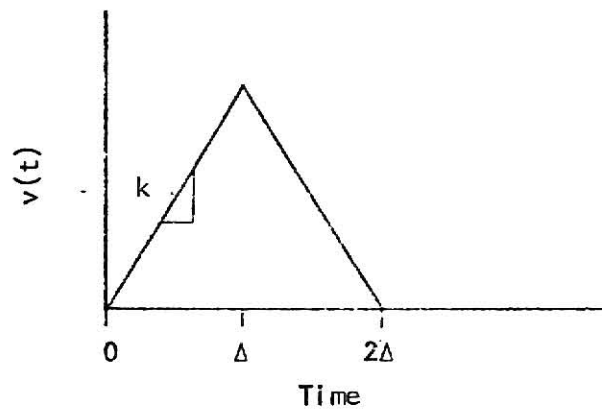


Figure 16. Triangular Pulse.

$$v(t) = \begin{cases} kt & \text{for } 0 \leq t < \Delta \\ k\Delta - k(t - \Delta) & \text{for } \Delta \leq t < 2\Delta \\ 0 & \text{for } t \geq 2\Delta \end{cases}$$

The Laplace transform of the triangular pulse, V , is found to be

$$V = k \left(\frac{e^{-s\Delta} - 1}{s} \right)^2 .$$

For this demonstration, the transfer function is

$$G(s) = \frac{2}{(s+1)(s+2)} .$$

The Laplace transform of the output, O , is found to be

$$O = G(s) \cdot V = \frac{2k(e^{-s\Delta} - 1)^2}{s^2(s+1)(s+2)} .$$

Expanding,

$$O = \frac{2ke^{-2s\Delta}}{s^2(s+1)(s+2)} - \frac{4ke^{-s\Delta}}{s^2(s+1)(s+2)} + \frac{2k}{s^2(s+1)(s+2)} . \quad (31)$$

Each of these three terms have the term

$$\frac{2k}{s^2(s+1)(s+2)}$$

in common. This term may be expressed in partial fractions as

$$\frac{2k}{s^2(s+1)(s+2)} = \frac{k}{s^2} - \frac{3k}{2s} + \frac{sk}{(s+1)} - \frac{k}{2(s+2)} .$$

This expansion aids in finding the z-transform of O, the output. The z-transform of each of the three terms in equation (31) is then found. The equality may then be manipulated to the form

$$O(z) = \frac{k(z-1)^2}{z^2} \left[\frac{\Delta z}{(z-1)^2} - \frac{3z}{2(z-1)} + \frac{2z}{z - e^{-\Delta}} - \frac{z}{2(z - e^{-2\Delta})} \right] , \quad (32)$$

the z-transform of the output.

Now assume the input to be a ramp. The Laplace transform of the output is then

$$O = \frac{1}{s^2} G(s) = \frac{2}{s^2(s+1)(s+2)}$$

This equation may now be expressed in partial fraction form as

$$O = \frac{1}{s^2} - \frac{3}{2s} + \frac{2}{(s+1)} + \frac{1}{2(s+2)} .$$

The z-transform of this is

$$O(z) = \frac{\Delta z}{(z-1)^2} - \frac{3z}{2(z-1)} + \frac{2z}{z - e^{-\Delta}} - \frac{z}{2(z - e^{-2\Delta})} .$$

R(z), the z-transfer function, may be obtained by dividing this output by the z-transform of the ramp input. The z-transform of a ramp, I(z) is

$$I(z) = \frac{\Delta z}{(z-1)^2} .$$

It follows that

$$R(z) = \frac{O(z)}{I(z)} = \frac{(z-1)^2}{\Delta z} \left[\frac{\Delta z}{(z-1)^2} - \frac{3z}{2(z-1)} + \frac{2z}{z - e^{-\Delta}} - \frac{z}{2(z - e^{-2\Delta})} \right] .$$

This transfer function is now multiplied by a weighted impulse input. The impulse is weighted by a constant such that the magnitude of the impulse is equal to the height of the triangular pulse input displayed in Figure 14. The impulse also occurs at the same point in time, Δ , that the triangular pulse reaches its peak. Below, the impulse is drawn with a solid line while the triangular pulse is pictured with dashed lines.

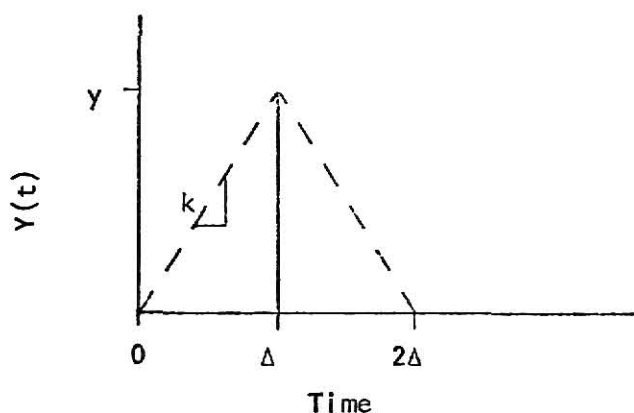


Figure 17. Weighted Impulse.

The z-transform of this weighted impulse input, $Y(z)$, is

$$Y(z) = Z[y S(t - \Delta)] = yz^{-1} .$$

"y" is the magnitude of the constant that "weights" the impulse. In terms of the slope of the dashed input it is found that

$$y = k\Delta .$$

The z-transform of the output, $O(z)$, from a transfer function developed with a ramp due to a weighted impulse input is

$$O(z) = R(z) \cdot Y(z) = \frac{k(z-1)^2}{z^2} \left[\frac{\Delta z}{(z-1)^2} - \frac{3z}{2(z-1)} + \frac{2z}{z - e^{-\Delta}} - \frac{z}{2(z - e^{-2\Delta})} \right] .$$

It may be seen that this is the same output as found in equation (32). Thus, it has been demonstrated that equivalent outputs may be obtained by 1) using a triangular pulse input, or 2) finding a transfer function with a ramp input and then using a weighted unit impulse as an actual input.

APPENDIX C - ROOTFINDER PROGRAM.

```

$JOB          TDH,TIME=(0,30),PUNCH,ACLIST
              IMPLICIT REAL*8(A-H,O-Z)
C*****
C    THIS PROGRAM IS A ROOTFINDER.  IT LOCATES NEGATIVE REAL ROOTS OF
C    THE FUNCTION B FOR THE VARIABLE S.  IT DOES SO BY OBSERVING SIGN
C    CHANGES IN THE VALUE OF THE FUNCTION B AS THE VARIABLE S IS
C    DECREMENTED.
C*****
      2 FORMAT('1',34X,1(65(' ')))
      3 FORMAT(' ',33X,'|',9X,'ROOT',10X,'|',6X,'VALUE OF',6X,'|',4X,
        1'DERIVATIVE',6X,'|')
      4 FORMAT(' ',33X,'|',10X,'S',12X,'|',5X,'FUNCTION B',5X,'|',3X,'OF F
        1UNCTION B',4X,'|')
      5 FORMAT('+',34X,1(65(' ')))
      6 FORMAT(' ',33X,'|',D23.16,'|',F20.16,'|',F20.16,'|')
     10 FORMAT(I5)
     11 FORMAT(F20.16)
     13 FORMAT('0','A ROOT HAS BEEN LOCATED AT S=',F10.4,5X,'B=',F10.4,
        15X,'DER=',I2)
     15 FORMAT('0','IT BLOWS UP AT X=',F10.6,5X,'B=',E15.4,5X,'DERF=',
        1E15.4,5X,'DER=',I2)
     16 FORMAT(D23.16)
        DIMENSION A(4),CON(4),DELX(4),H(2,2),HT(2,2),HTMX(2,2)
C*****
C    N    - NUMBER OF LAYERS
C    R1   - INNER SURFACE RESISTANCE
C    RN   - OUTER SURFACE RESISTANCE
C    A    - THERMAL DIFFUSIVITY
C    CON  - SPECIFIC HEAT
C    DELX- LAYER THICKNESS
C*****
      READ(5,10) N
      READ(5,11) R1
      READ(5,11) RN
      DO 20 M=1,N
     20 READ(5,11) A(M)
      DO 21 M=1,N
     21 READ(5,11) CON(M)
      DO 22 M=1,N
     22 READ(5,11) DELX(M)
      WRITE(6,2)
      WRITE(6,3)
      WRITE(6,4)
      WRITE(6,5)
C    THE VARIABLE S IS INITIALIZED TO THE FOLLOWING VALUE.
      S=0.0001D0
      S=DABS(S)
     34 CONTINUE
      CALL FIGURE(S,N,R1,A,CON,DELX,RN,F)
      IF (F)37,31,38
     37 CONTINUE
     30 S=S+0.01D0
      IF (S.CE.5.00D1)GO TO 35

```

```

      CALL FIGURE(S,N,R1,A,CCN,DELX,RN,F)
      IF (F)30,31,33
38 CONTINUE
32 S=S+0.0100
   IF (S.GE.5.0001)GO TO 35
   CALL FIGURE(S,N,R1,A,CCN,DELX,RN,F)
   IF (F)33,31,32
33 CONTINUE
   XST=S
C   EPS IS THE VALUE OF THE MAXIMUM ALLOWABLE ERROR IN A ROOT.
   EPS=1.0D-14
   IEND=100
   CALL BETA(X,F,DERF,R1,A,CCN,DELX,RN,XST,EPS,IEND,IER,N)
   IF (X)42,42,43
42 WRITE(6,15)X,F,DERF,IER
   GO TO 36
43 CONTINUE
   W=-X
   WRITE(6, 6) W,F,DERF
   PUNCH16,W
   S=S+0.0100
   IF (S.LT.5.0001)GO TO 34
   GO TO 36
31 WRITE(6,13) S,F,IER
   PUNCH16,S
   S=S+0.0100
   IF (S.LT.5.0001)GO TO 34
   GO TO 36
35 WRITE(6,5)
36 CONTINUE
   WRITE(6,2)
   STOP
   END
   SUBROUTINE FIGURE(S,N,R1,A,CCN,DELX,RN,F)
   IMPLICIT REAL*8(A-H,O-Z)
C *****
C   SUBROUTINE FIGURE FINDS NUMERICAL VALUES FOR EACH ELEMENT OF THE
C   2X2 MATRIX, MATRIX (12), FOR A SPECIFIC VALUE OF S. VALUES ARE
C   FOUND FOR ANY N LAYER STRUCTURE BY CALLING A MATRIX MULTIPLICATION
C   SUBROUTINE.
C *****
   DIMENSION A(N),CCN(N),DELX(N),H(2,2),HT(2,2),HTMX(2,2)
   M=0
   H(1,1)= 1.00
   H(1,2)= R1
   H(2,1)= 0.00
   H(2,2)= 1.00
23 CONTINUE
   M=M+1
   HT(1,1)=DCOS(DSQRT(S/A(M))*DELX(M))
   HT(1,2)=(-1.00/COS(M))*DSQRT(A(M)/S)*DSIN(DSQRT(S/A(M))*DELX(M))
   HT(2,1)=CCN(M)+DSQRT(S/A(M))*DSIN(DSQRT(S/A(M))*DELX(M))
   HT(2,2)=DCOS(DSQRT(S/A(M))*DELX(M))

```

```

      CALL MATMUL(H,HT,HTMX,2,2,2)
      DO 24 I=1,2
      DO 25 J=1,2
      FAKEX=HTMX(I,J)
      H(I,J)=FAKEX
25 CONTINUE
24 CONTINUE
      IF (M.LT.N)GO TO 23
      HT(1,1)= 1.00
      HT(1,2)= RN
      HT(2,1)= 0.00
      HT(2,2)= 1.00
      CALL MATMUL(H,HT,HTMX,2,2,2)
      F=HTMX(1,2)
      RETURN
      END
      SUBROUTINE BETA(X,F,DERF,R1,A,CON,DELX,RN,XST,EPS,IEND,IER,N)
      IMPLICIT REAL*8(A-H,C-Z)
C*****
C      BETA SUBROUTINE IS USED TO QUICKLY AND ACCURATELY CONVERGE ON A
C      ROOT ONCE THE GENERAL LOCATION OF THE ROOT HAS BEEN DETERMINED.
C      IT NEEDS THE VALUE OF THE FUNCTION AS WELL AS ITS DERIVATIVE AT
C      PARTICULAR VALUES OF S.
C*****
      DIMENSION A(N),CON(N),DELX(N)
      PREPARE ITERATION
      IER=0
34 CONTINUE
      X=XST
      TOL=X
      CALL FIGURE(TOL,N,R1,A,CON,DELX,RN,F)
      CALL DERIV(TOL,N,R1,A,CON,DELX,RN,DERF)
      TOLF=1.002*EPS
C      START ITERATION LOOP
      DO 6 I=1,IEND
      IF (F)1,7,1
C      EQN. NOT SATISFIED BY X
1      IF (DERF)2,3,2
C      ITERATION IS POSSIBLE
2      DX=F/DERF
      X=X-DX
      IF (X)30,30,31
30 CONTINUE
      XST=XST-1.00-2
      GO TO 34
31 CONTINUE
      TOL=X
      CALL FIGURE(TOL,N,R1,A,CON,DELX,RN,F)
      CALL DERIV(TOL,N,R1,A,CON,DELX,RN,DERF)
C      TEST ON SATISFACTORY ACCURACY
      TOL=EPS

```

```

      G=DABS(X)
      IF (G-1.000)4,4,3
3     TOL=TCL*G
4     IF (DABS(OX)-TCL)5,5,6
5     IF (DABS(F)-TOLF)7,7,6
6     CONTINUE
C     END OF ITERATION LOOP
C     NO CONVERGENCE AFTER IEND ITERATION STEPS. ERROR RETURN.
      IER=1
7     RETURN
C     ERROR RETURN IN CASE OF ZERO DIVISOR
8     IER=2
      RETURN
      END
      SUBROUTINE DERIV(S,N,R1,A,CON,DELX,RN,DERF)
      IMPLICIT REAL*8(A-H,C-Z)
C*****
C     SUBROUTINE DERIV FINDS NUMERICAL VALUES FOR THE DERIVATIVE OF
C     EACH ELEMENT OF THE 2X2 MATRIX, MATRIX (12), FOR A SPECIFIC
C     VALUE OF S.
C*****
      DIMENSION A(N),CON(N),DELX(N),H(2,2),HT(2,2),HHT(2,2),DH(2,2),
      1HDH(2,2),H-H(2,2),HTMX(2,2),HNEW(2,2),HNEWER(2,2),RHTMX(2,2)
      L=0
67    L=L+1
      M=1
      H(1,1)=1.00
      H(1,2)=R1
      H(2,1)=0.00
      H(2,2)=1.00
      IF (M.EQ.L)GO TO 68
54    HT(1,1)=DCOS(DSQRT(S/A(M))*DELX(M))
      HT(1,2)=(-1.00/CON(M))*DSQRT(A(M)/S)*DSIN(DSQRT(S/A(M))*DELX(M))
      HT(2,1)=CON(M)*DSQRT(S/A(M))*DSIN(DSQRT(S/A(M))*DELX(M))
      HT(2,2)=DCOS(DSQRT(S/A(M))*DELX(M))
      CALL MATMUL(H,HT,HHT,2,2,2)
      DO 55 I=1,2
      DO 56 J=1,2
      FAKE=HHT(I,J)
      H(I,J)=FAKE
56    CONTINUE
55    CONTINUE
      M=M+1
      IF (M.NE.L)GO TO 54
68    DH(1,1)=- (DELX(M)/(2.00*DSQRT(A(M)*S)))*DSIN(DSQRT(S/A(M))
      1*DELX(M))
      DH(1,2)=-(DELX(M)/(2.00*CON(M)*S))*DCOS(DSQRT(S/A(M))*DELX(M))+
      1(1.00/(2.00*CON(M)))*DSQRT(A(M)/(S**3))*DSIN(DSQRT(S/A(M))
      1*DELX(M))
      DH(2,1)=((CON(M)*DELX(M))/(2.00*A(M)))*DCOS(DSQRT(S/A(M))*
      1DELX(M))+ (CON(M)/(2.00*DSQRT(A(M)*S)))*DSIN(DSQRT(S/A(M))*
      1DELX(M))

```

```

      DH(2,2)=- (DELX(M)/(2.DO*DSQRT(A(M)*S)))*DSIN(DSQRT(S/A(M))*
1 DELX(M))
      CALL MATMUL(H,DH,HDH,2,2,2)
      IF (M.NE.1)GO TO 69
      GO TO 59
69  CONTINUE
      IF (M.EQ.N)GO TO 70
59  M=M+1
      HH(1,1)=DCOS(DSQRT(S/A(M))*DELX(M))
      HH(1,2)=(-1.DO/CCN(M))*DSQRT(A(M)/S)*DSIN(DSQRT(S/A(M))*DELX(M))
      HH(2,1)=CCN(M)*DSQRT(S/A(M))*DSIN(DSQRT(S/A(M))*DELX(M))
      HH(2,2)=DCOS(DSQRT(S/A(M))*DELX(M))
      CALL MATMUL(HDH,HH,HTMX,2,2,2)
      DO 57 I=1,2
      DO 58 J=1,2
      DUM=HTMX(I,J)
      HDH(I,J)=DUM
58  CONTINUE
57  CONTINUE
      IF (M.LT.N)GO TO 59
70  H(1,1)=1.DO
      H(1,2)=RA
      H(2,1)=0.DO
      H(2,2)=1.DO
      CALL MATMUL(HDH,H,HTMX,2,2,2)
      IF (L.GT.1)GO TO 60
      DO 61 I=1,2
      DO 62 J=1,2
      DUMM=HTMX(I,J)
      HNEW(I,J)=DUMM
62  CONTINUE
61  CONTINUE
      IF (L.EQ.1)GO TO 67
60  CONTINUE
      DO 63 I=1,2
      DO 64 J=1,2
      DUMMI=HTMX(I,J)
      HNEW(I,J)=DUMMI
64  CONTINUE
63  CONTINUE
      CALL HYADD(HNEW,HNEWER,RHTMX,2,2)
      DO 65 I=1,2
      DO 66 J=1,2
      DUMMIE=RHTMX(I,J)
      HNEW(I,J)=DUMMIE
66  CONTINUE
65  CONTINUE
      IF (L.LT.N)GO TO 67
      DERF=HNEW(1,2)
      RETURN
      END

```

```

      SUBROUTINE MATMUL(A,B,C,M,N,L)
      IMPLICIT REAL*8(A-H,O-Z)
C     THIS SUBROUTINE PERFORMS MATRIX MULTIPLICATION.
      DIMENSION A(M,N), B(N,L), C(M,L)
      DO 300 I=1,M
      DO 200 J=1,L
      SUM=0.000
      SUM=0.0
      DO 100 K=1,N
100    SUM=SUM+A(I,K)*B(K,J)
200    C(I,J)=SUM
300    CONTINUE
      RETURN
      END
      SUBROUTINE HMADD(A,B,R,M,N)
      IMPLICIT REAL*8(A-H,O-Z)
C     THIS SUBROUTINE PERFORMS MATRIX ADDITION.
      DIMENSION A(N,N), B(N,N), R(N,N)
      DO 10 I=1,2
      DO 11 J=1,2
      R(I,J)=A(I,J)+B(I,J)
11    CONTINUE
10    CONTINUE
      RETURN
      END
$ENTRY

```

APPENDIX D - Z-COEFFICIENTS PROGRAM

```

$JOB          TDH,TIME=(0,09),PUNCH,NCLIST
              IMPLICIT REAL*8(A-H,C-Z)
C*****
C    THIS PROGRAM FINDS THE NUMERATOR AND DENOMINATOR COEFFICIENTS OF
C    POLYNOMIALS IN  $Z^{-1}$  FOR THE Z- TRANSFER FUNCTIONS R(Z) AND W(Z).
C*****
      DIMENSION A(10),CON(10),DELX(10),X(70),Y(70),Z(70),RZ(70),
      1AN(70),DN(70),AUP(70),CUP(70),BETA(70),BOTM(70)
      50 FORMAT(I5)
      51 FORMAT(D23.16)
      52 FORMAT(' ',BEE2=' ',F20.16)
      53 FORMAT(' ',BEE1=' ',F20.16)
      54 FORMAT(' ',CEE2=' ',F20.16)
      55 FORMAT(' ',CEE1=' ',F20.16)
      56 FORMAT(' ',B(' ',I2,' ')=' ',D24.16)
      57 FORMAT(' ',AN(' ',I2,' ')=' ',F20.16,10X,DN(' ',I2,' ')=' ',F20.16)
      58 FORMAT(' ',A(' ',I2,' ')=' ',D24.16,10X,C(' ',I2,' ')=' ',D24.16)
      59 FORMAT(D24.16)
      60 FORMAT('1',55X,'STEPSIZE=' ',F4.1,1X,'HR')
      61 FORMAT('1',25X,'NUMERATOR',24X,'DENOMINATOR',24X,'NUMERATOR')
      62 FORMAT(' ',27X,'R(Z)',26X,'R(Z) AND W(Z)',25X,'W(Z)')
      63 FORMAT('0')
      64 FORMAT(' ',15X,'A(' ',I2,' ')=' ',D23.16,5X,'B(' ',I2,' ')=' ',D23.16,5X,
      1'C(' ',I2,' ')=' ',D23.16)
      65 FORMAT('1')
C*****
C    INPUT TO THIS PROGRAM IS:
C    N      - NUMBER OF ROOTS
C    NLAY   - NUMBER OF LAYERS
C    DELTA  - STEPSIZE IN TIME
C    R1     - INNER SURFACE RESISTANCE
C    RN     - OUTER SURFACE RESISTANCE
C    A      - THERMAL DIFFUSIVITY
C    CON    - SPECIFIC HEAT
C    DELX   - LAYER THICKNESS
C    BETA   - ROOTS OF THE FUNCTION B
C*****
      READ(5,50) N
      READ(5,50) NLAY
      READ(5,51) DELTA
      READ(5,51) R1
      READ(5,51) RN
      DO 10 J=1,NLAY
10  READ(5,51) A(J)
      DO 11 J=1,NLAY
11  READ(5,51) CON(J)
      DO 12 J=1,NLAY
12  READ(5,51) DELX(J)
      DO 13 J=1,N
13  READ(5,51) BETA(J)
      CALL CCNSTS(CEE2,CEE1,BEE2,BEE1,R1,A,CON,DELX,RN,NLAY)
      WRITE(6,52) BEE2
      WRITE(6,53) BEE1

```

```

WRITE(6,54) CEE2
WRITE(6,55) CEE1
NI=N+1
C*****
C   THE  $(1-\exp(-\text{BETA}(M)\text{DELTA}))Z^{**}-1$  TERMS ARE NOW MULTIPLIED
C   TOGETHER AND THE RESULTING POLYNOMIAL IS THE DENOMINATOR OF BOTH
C   Z-TRANSFER FUNCTIONS.
C*****
      IDIMX=2
      X(1)=1.00
      X(2)=-DEXP(BETA(1)*DELTA)
      M=1
22  M=M+1
      Y(1)=1.00
      Y(2)=-DEXP(BETA(M)*DELTA)
      IDIMY=2
      CALL PMPY(Z, IDIMZ, X, IDIMX, Y, IDIMY, NI)
      DO 21 I=1, IDIMZ
        DUM=Z(I)
        X(I)=DUM
21  CONTINUE
      IDIMX=IDIMZ
      IF (M.LT.N) GO TO 22
      DO 23 I=1, IDIMX
        FAKE=X(I)
        BOTM(I)=FAKE
        PUNCH59, X(I)
23  WRITE(6,56) I, X(I)
C*****
C   THIS FINDS  $((1-Z^{**}-1)**2)*(THE DENOMINATOR POLYNOMIAL)$  TO BE
C   USED IN EVALUATION OF THE NUMERATOR COEFFICIENTS FOR EACH TRANSFER
C   FUNCTION.
C*****
      Y(1)=1.00
      Y(2)=-2.00
      Y(3)=1.00
      IDIMY=3
      N2=N+2
      N3=N+3
      CALL PMPY(RZ, IDIMR, X, IDIMX, Y, IDIMY, N3)
C*****
C   THE CONSTANTS Q(M) AND V(M) ARE EVALUATED HERE.
C*****
      DO 25 I=1, N
        S=DABS(BETA(I))
        CALL FIGURE(S, NLAY, R1, A, CON, DELX, RN, APE)
        CALL DERIV(S, NLAY, R1, A, CCN, DELX, RN, BARK)
        BARK=-BARK
        AN(I)=APE/((S**2)*BARK)
        DN(I)=1.00/((S**2)*BARK)
25  WRITE(6,57) I, AN(I), I, DN(I)
      CALL THENUM(RZ, BEE2, BEE1, AN, AUP, DELTA, BETA, N3)

```

```

      CALL THENUM(RZ,CEE2,CEE1,DN,CUP,DELTA,BETA,N3)
      DO 26 I=1,N3
        PUNCH59,AUP(I)
        PUNCH59,CUP(I)
26    WRITE(6,58) I,AUP(I),I,CUP(I)
        WRITE(6,60) DELTA
        WRITE(6,61)
        WRITE(6,62)
        WRITE(6,63)
        BOTM(N2)=0.000
        BOTM(N3)=0.000
      DO 27 I=1,N3
27    WRITE(6,64) I,AUP(I),I,BOTM(I),I,CUP(I)
        WRITE(6,65)
      STOP
      END
      SUBROUTINE THENUM(X,BC2,BC1,AD,TCP,DELTA,BETA,N3)
      IMPLICIT REAL*8(A-H,C-Z)
C*****
C      SUBROUTINE THENUM CALCULATES THE NUMERATOR CCEFFICIENTS FOR THE
C      Z- TRANSFER FUNCTIONS.
C*****
      DIMENSION AD(N3),BETA(N3),O(70),TOP(70),X(70)
      N=N3-3
C*****
C      VALUES OF THE INVERSE LAPLACE TRANSFER FUNCTION ARE CALCULATED
C      AT MULTIPLES OF DELTA.
C*****
      TIME=0.000
      IPHI=1
11    IPHI=IPHI+1
      TIME=TIME+DELTA
      PART=0.000
      DO 10 I=1,N
        SIZE=BETA(I)*TIME
        IF(SIZE.LE.-160.000)GO TO 12
10    PART=PART+AD(I)*(DEXP(SIZE))
12    O(IPHI)=(BC2*TIME)+BC1+PART
        IF(IPHI.LT.N+4) GO TO 11
      NOW IPHI EQUALS N+4
C*****
C      THE NUMERATOR CCEFFICIENTS ARE NOW OBTAINED FROM THE DENOMINATOR,
C      INPUT, AND OUTPUT.
C*****
      IOTA=0
14    IOTA=IOTA+1
      TOP(IOTA)=0.000
      DO 13 L=1,IOTA
        K=IOTA-L+2
13    TOP(IOTA)=TCP(IOTA)+C(K)*X(L)
      TOP(IOTA)=TOP(IOTA)/DELTA
      IF(IOTA.LT.IPHI-1) GO TO 14
      RETURN
      END

```

```

      SUBROUTINE CONSTS(CEE2,CEE1,BEE2,BEE1,R1,A,CON,DELX,RN,N)
C*****
C   CONSTS FINDS THE NUMERICAL VALUES OF P2, P1, V2, AND V1. THESE
C   CONSTANTS ARE ALL EVALUATED AT S=0.
C*****
      IMPLICIT REAL*8(A-H,G-Z)
      DIMENSION A(N),CCN(N),DELX(N)
      DIMENSION H(2,2),HT(2,2),HHT(2,2),DH(2,2),HCH(2,2),HH(2,2)
      DIMENSION HTMX(2,2),HNEW(2,2),HNEWER(2,2),RHTMX(2,2)
C*****
C   (A/B) AND (1./B) ARE CALCULATED AT S=0.
C   A=1. AT S=0.
C*****
      HB0=R1+RN
      DO 90 M=1,N
      HB=-(DELX(M)/CCN(M))
90    HB0=HB0+HB
      BEE2=(1.D0/HB0)
      CEE2=BEE2
C*****
C   THIS SECTION CALCULATES THE VALUE OF THE DERIVATIVE FOR EACH
C   ELEMENT OF THE 2X2 HEAT MATRIX AT S=0.
C*****
      L=0
67    L=L+1
      M=1
      H(1,1)= 1.D0
      H(1,2)= R1
      H(2,1)= 0.000
      H(2,2)= 1.D0
      IF (M.EQ.L)GO TO 68
54    HT(1,1)=1.D0
      HT(1,2)=-(DELX(M)/CCN(M))
      HT(2,1)=0.000
      HT(2,2)=1.D0
      CALL MATMUL(H,HT,HHT,2,2,2)
      DO 55 I=1,2
      DO 56 J=1,2
      FAKE=HHT(I,J)
      H(I,J)=FAKE
56    CONTINUE
55    CONTINUE
      M=M+1
      IF (M.NE.L)GO TO 54
68    DH(1,1)=(DELX(M)**2)/(2.D0*A(M))
      DH(1,2)=-(DELX(M)**3)/(6.D0*CCN(M)*A(M))
      DH(2,1)=-(CCN(M)*DELX(M))/A(M)
      DH(2,2)=(DELX(M)**2)/(2.D0*A(M))
      CALL MATMUL(H,DH,HCH,2,2,2)
      IF (M.NE.1)GO TO 69
      GO TO 59
69    CONTINUE

```

```

      IF (M.EQ.N)GO TO 70
59  M=M+1
      HH(1,1)=1.00
      HH(1,2)=-(DELX(M)/CON(M))
      HH(2,1)=0.000
      HH(2,2)=1.00
      CALL MATMUL(HDH,HH,HTMX,2,2,2)
      DO 57 I=1,2
      DO 58 J=1,2
      DUM=HTMX(I,J)
      HDH(I,J)=DUM
58  CONTINUE
57  CONTINUE
      IF (M.LT.N)GO TO 59
70  H(1,1)=1.00
      H(1,2)=RA
      H(2,1)=0.000
      H(2,2)=1.00
      CALL MATMUL(HDH,H,HTMX,2,2,2)
      IF (L.GT.1)GO TO 60
      DO 61 I=1,2
      DO 62 J=1,2
      DUMM=HTMX(I,J)
      HNEW(I,J)=DUMM
62  CONTINUE
61  CONTINUE
      IF (L.EQ.1)GO TO 67
60  CONTINUE
      DO 63 I=1,2
      DO 64 J=1,2
      DUMMI=HTMX(I,J)
      HNEW(I,J)=DUMMI
64  CONTINUE
63  CONTINUE
      CALL HMADD(HNEW,HNEW,RHTMX,2,2)
      DO 65 I=1,2
      DO 66 J=1,2
      DUMMIE=RHTMX(I,J)
      HNEW(I,J)=DUMMIE
66  CONTINUE
65  CONTINUE
      IF (L.LT.N)GO TO 67
C*****
C  THE DERIVATIVES CALCULATED ABOVE ARE USED TO OBTAIN VALUES FOR
C  P1 AND V1.
C*****
      DACSO=HNEW(1,1)
      DBDSO=HNEW(1,2)
      BDADSO=HBO*DADSO
      ADBDSO=CBDSO
      BEE1=((BCADSO-ADBDSO)/(HBO**2))
      CEE1=(-DBDSO/(HBO**2))
      RETURN
      END

```

```

SUBROUTINE FIGURE(S,N,R1,A,CON,DELX,RN,F)
  IMPLICIT REAL*8(A-H,O-Z)
C*****
C  SUBROUTINE FIGURE FINDS NUMERICAL VALUES FOR EACH ELEMENT OF THE
C  2X2 MATRIX, MATRIX (12), FOR A SPECIFIC VALUE OF S.  VALUES ARE
C  FOUND FOR ANY N LAYER STRUCTURE BY CALLING A MATRIX MULTIPLICATION
C  SUBROUTINE.
C*****
  DIMENSION A(N),CCN(N),DELX(N),H(2,2),HT(2,2),HTMX(2,2)
  M=0
  H(1,1)= 1.00
  H(1,2)= R1
  H(2,1)= 0.00
  H(2,2)= 1.00
23 CONTINUE
  M=M+1
  HT(1,1)=DCOS(DSQRT(S/A(M))*DELX(M))
  HT(1,2)=(-1.00/CCN(M))*DSQRT(A(M)/S)*DSIN(DSQRT(S/A(M))*DELX(M))
  HT(2,1)=CCN(M)*DSQRT(S/A(M))*DSIN(DSQRT(S/A(M))*DELX(M))
  HT(2,2)=DCOS(DSQRT(S/A(M))*DELX(M))
  CALL MATMUL(H,HT,HTMX,2,2,2)
  DO 24 I=1,2
    DO 25 J=1,2
      FAKE=HTMX(I,J)
      H(1,J)=FAKE
    25 CONTINUE
  24 CONTINUE
  IF (M.LT.N)GO TO 23
  HT(1,1)= 1.00
  HT(1,2)= RN
  HT(2,1)= 0.00
  HT(2,2)= 1.00
  CALL MATMUL(H,HT,HTMX,2,2,2)
  F=HTMX(1,1)
  RETURN
END
SUBROUTINE DERIV(S,N,R1,A,CON,DELX,RN,DERF)
  IMPLICIT REAL*8(A-H,C-Z)
C*****
C  SUBROUTINE DERIV FINDS NUMERICAL VALUES FOR THE DERIVATIVE OF
C  EACH ELEMENT OF THE 2X2 MATRIX, MATRIX (12), FOR A SPECIFIC
C  VALUE OF S.
C*****
  DIMENSION A(N),CCN(N),DELX(N),H(2,2),HT(2,2),HHT(2,2),DH(2,2),
  1HDH(2,2),HH(2,2),HTMX(2,2),HNEW(2,2),HNEWER(2,2),RHTMX(2,2)
  L=0
67 L=L+1
  M=1
  H(1,1)=1.00
  H(1,2)=R1
  H(2,1)=0.00
  H(2,2)=1.00
  IF (M.EQ.L)GO TO 68

```

```

54 HT(1,1)=DCOS(DSQRT(S/A(M))*DELX(M))
   HT(1,2)=(-1.00/CCN(M))*DSQRT(A(M)/S)*DSIN(DSQRT(S/A(M))*DELX(M))
   HT(2,1)=CCN(M)*DSQRT(S/A(M))*DSIN(DSQRT(S/A(M))*DELX(M))
   HT(2,2)=DCOS(DSQRT(S/A(M))*DELX(M))
   CALL MATMUL(H,HT,HHT,2,2,2)
   DO 55 I=1,2
   DO 56 J=1,2
   FAKE=FHT(I,J)
   H(I,J)=FAKE
56 CONTINUE
55 CONTINUE
   M=M+1
   IF (M.NE.L)GO TO 54
68 DH(1,1)=- (DELX(M)/(2.00*DSQRT(A(M)*S)))*DSIN(DSQRT(S/A(M))
1*DELX(M))
   DH(1,2)=-(DELX(M)/(2.00*CON(M)*S))*DCOS(DSQRT(S/A(M))*DELX(M))+
1(1.00/(2.00*CON(M)))*DSQRT(A(M)/(S**3))*DSIN(DSQRT(S/A(M))
1*DELX(M))
   DH(2,1)=((CON(M)*DELX(M))/(2.00*A(M)))*DCOS(DSQRT(S/A(M))*
1DELX(M))+(CON(M)/(2.00*DSQRT(A(M)*S))*DSIN(DSQRT(S/A(M))*
1DELX(M))
   DH(2,2)=-(DELX(M)/(2.00*DSQRT(A(M)*S)))*DSIN(DSQRT(S/A(M))*
1DELX(M))
   CALL MATMUL(H,DH,HCH,2,2,2)
   IF (M.NE.1)GO TO 69
   GO TO 59
69 CONTINUE
   IF (M.EQ.N)GO TO 70
59 P=M+1
   HH(1,1)=DCOS(DSQRT(S/A(M))*DELX(M))
   HH(1,2)=(-1.00/CCN(M))*DSQRT(A(M)/S)*DSIN(DSQRT(S/A(M))*DELX(M))
   HH(2,1)=CCN(M)*DSQRT(S/A(M))*DSIN(DSQRT(S/A(M))*DELX(M))
   HH(2,2)=DCOS(DSQRT(S/A(M))*DELX(M))
   CALL MATMUL(HDH,HH,HTMX,2,2,2)
   DO 57 I=1,2
   DO 58 J=1,2
   DUM=HTMX(I,J)
   HDH(I,J)=DUM
58 CONTINUE
57 CONTINUE
   IF (M.LT.N)GO TO 59
70 H(1,1)=1.00
   H(1,2)=RN
   H(2,1)=0.00
   H(2,2)=1.00
   CALL MATMUL(FDH,F,FTMX,2,2,2)
   IF (L.GT.1)GO TO 60
   DO 61 I=1,2
   DO 62 J=1,2
   DUM=FTMX(I,J)
   HNEW(I,J)=DUM
62 CONTINUE
61 CONTINUE

```

```

        IF (L.EQ.1)GO TO 67
60  CONTINUE
    DO 63 I=1,2
    DO 64 J=1,2
        DUMMI=HTMX(I,J)
        HNEW(I,J)=DUMMI
64  CONTINUE
63  CONTINUE
    CALL HMADD(HNEW,HNEW,RHTMX,2,2)
    DO 65 I=1,2
    DO 66 J=1,2
        DUMMIE=RHTMX(I,J)
        HNEW(I,J)=DUMMIE
66  CONTINUE
65  CONTINUE
    IF (L.LT.N)GO TO 67
    DERF=HNEW(1,2)
    RETURN
    END
    SUBROUTINE PMPY(Z, IDIMZ, X, IDIMX, Y, IDIMY, NI)
    IMPLICIT REAL*8(A-H, C-Z)
C*****
C    PMPY PERFORMS POLYNOMIAL MULTIPLICATION. THE IDIM,S ARE
C    DIMENSIONS OF THE POLYNOMIALS. THE COEFFICIENTS OF THE INPUT
C    POLYNOMIALS ARE THE ARRAYS X AND Y AND Z IS THE ARRAY OF
C    COEFFICIENTS OF THE RESULTANT POLYNOMIAL.
C*****
    DIMENSION Z(NI), X(NI), Y(NI)
    20 IDIMZ=IDIMX+IDIMY-1
    DO 30 I=1, IDIMZ
        Z(I)=0.000
    30  DO 40 I=1, IDIMX
        DO 40 J=1, IDIMY
            IF(DABS(X(I)).LE.1.00-40)GO TO 43
            GO TO 42
        43 X(I)=0.000
    42  CONTINUE
        K=I+J-1
    40  Z(K)=X(I)*Y(J)+Z(K)
    50  RETURN
    END
    SUBROUTINE MATMUL(A,B,C,M,N,L)
    IMPLICIT REAL*8(A-H, C-Z)
C    THIS SUBROUTINE PERFORMS MATRIX MULTIPLICATION.
    DIMENSION A(M,N), B(N,L), C(M,L)
    DO 300 I=1,M
    DO 200 J=1,L
        SUM=0.000
    DO 100 K=1,N
        100 SUM=SUM+A(I,K)*B(K,J)
        200 C(I,J)=SUM
    300 CONTINUE
    RETURN
    END

```

```
      SUBROUTINE HMAcc(A,B,R,M,N)
      IMPLICIT REAL*8(A-H,C-Z)
C      THIS SUBROUTINE PERFORMS MATRIX ADDITION.
      DIMENSION A(M,N),B(M,N),R(M,N)
      DO 10 I=1,2
      DO 11 J=1,2
      R(I,J)=A(I,J)+B(I,J)
11  CONTINUE
10  CONTINUE
      RETURN
      END
$ENTRY
```

APPENDIX E - FCALC PROGRAM

\$JOB

```

      IMPLICIT REAL*8(A-H,C-Z)
      DIMENSION A(70),B(70),C(70),TIN(801),TOUT(801),F(801)
51  FORMAT(' ','F(',I4,')=',D23.16)
22  FORMAT(D24.16)
24  FORMAT(15)
      READ(5,24) ITHETA
      DO 8 I=1,ITHETA
8    READ(5,22) A(I)
      DO 9 I=1,ITHETA
9    READ(5,22) B(I)
      DO 10 I=1,ITHETA
10   READ(5,22) C(I)
      SAREA=1.0D0
      IPT=0
      IEND=225
      TGO=70.0D0
      DO 50 I= 4,IEND
      TIN(I)=71.0D0
50   TOUT(I)=75.0D0
      TIN(I)=70.0D0
      TOUT(I)=70.0D0
      DO 61 I=1,2
      TIN(I+1)=(0.500D0*I)+70.0D0
61   TOUT(I+1)=(2.500D0*I)+70.0D0
52   IPT=IPT+1
      CALL FCALC(A,B,C,ITHETA,TGO,TIN,TOUT,IPT,F,SAREA)
      IF(IPT.LT.IEND)GO TO 52
      DO 62 I=1,IEND
62   WRITE(6,51) I,F(I)
      STOP
      END
      SUBROUTINE FCALC(A,B,C,ITHETA,TGO,TIN,TOUT,IPT,F,SAREA)
      IMPLICIT REAL*8(A-H,C-Z)
C*****
C    FCALC FINDS THE HEAT FLUX AT THE INNER SURFACE OF A MULTILAYER
C    STRUCTURE, WHEN IT IS GIVEN THE Z-COEFFICIENTS FOR THE STRUCTURE,
C    A, B, AND C, THE NUMBER OF INDIVIDUAL COEFFICIENTS, ITHETA, THE
C    INITIAL WALL TEMP, TGO, INSIDE TEMP, TIN, OUTSIDE TEMP, TOUT,
C    AND THE SURFACE AREA OF THE STRUCTURE, SAREA. FCALC USES THE
C    EQUATIONS FROM TABLE 2.
C*****
      DIMENSION A(ITHETA),B(ITHETA),C(ITHETA),TIN(IPT),TOUT(IPT),
1F(IPT),FLT( 801),FRT( 801),U( 801),V( 801)
      U(IPT)=TIN(IPT)-TGO
      V(IPT)=TOUT(IPT)-TGO
      IF(IPT.GT.ITHETA)GO TO 11
      IPhi=IPT
      RT=0.0D0
      RTER=0.0D0
      GT=0.0D0
      N=0
10   N=N+1

```

```

      M=IPHI-N+1
      IF (N.EQ.1)GO TO 12
      GT=GT+(F(N)*B(N))
12   FLT(IPHI)=GT
      RT=RT+(U(M)*A(N))
      RTER=RTER+(V(M)*C(N))
      IF (N.LT.IPHI)GO TO 10
      FRT(IPHI)=-RT+RTER
      F(IPHI)=(FRT(IPHI)-FLT(IPHI))
      GO TO 30
11   IFLY=IPT
50   RT=0.000
      GT=0.000
      GTER=0.000
      M=0
      IFLY=IFLY+1
      N=IFLY
51   M=M+1
      N=N-1
      GT=(U(N)*A(M))+GT
      GTER=(V(N)*C(M))+GTER
      IF (M.EQ.1)GO TO 51
      RT=RT+(F(N)*B(M))
      IF (M.LT.ITHETA)GO TO 51
      IGOT=IFLY-1
      F(IGOT)=(-GT-RT+GTER)
30   CONTINUE
      RETURN
      END
$ENTRY

```

APPENDIX F - DERIVATION OF CONTROL SYSTEM EQUATIONS

The development of this air conditioning control system model is based upon the application of heat and mass balance equations to the various components of the system and the implementation of an air temperature sensor feedback to control the input of heat into the controlled environment. In the development of models of this type it is common practice to express the variables of the system in terms of their deviation from an equilibrium condition. In the following development, the equilibrium temperature will be represented by θ_{Go} . As illustrated in Figure 10, the system to be modeled consists of a controlled room air space supplied by heat from a steam coil. The steam flow is controlled by a valve whose action is regulated in response to the temperature difference between the set point temperature and the sensed temperature of the room air. Supply air is made up of return air and fresh air.

First a differential equation describing the space temperature, θ_R , will be developed. The space is pictured below with the necessary nomenclature.

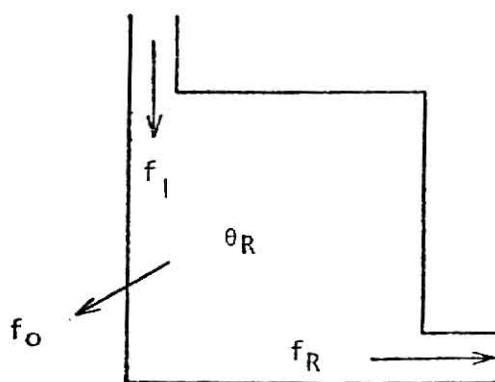


Figure 18. Room Air Space.

- f_I - rate of heat flow into the space (BTU/hr)
 f_O - rate of heat loss from air space through walls (BTU/hr)
 f_R - rate of heat loss from air space through return duct (BTU/hr)
 θ_I - inlet air temperature ($^{\circ}\text{F}$)
 θ_O - outside air temperature ($^{\circ}\text{F}$)
 θ_R - room air temperature ($^{\circ}\text{F}$)
 c - specific heat of air = $0.24 \text{ BTU}/(\text{lb}_m - ^{\circ}\text{F})$
 ρ - density of air (lb_m/ft^3)
 V - volume of room (ft^3)

From a basic heat balance, it is known that the net heat flow into the air space during some time is equal to the change in internal energy of the air during that period. It follows that

$$f_I - f_R - f_O = \rho CV \frac{d\theta_R}{dt} .$$

The heat flow into the room less the heat returned is governed by the flowrate of air into and out of the space times the heat content of the air, so

$$f_I - f_R = \rho CA \dot{x} (\theta_I - \theta_R)$$

where A - area of ducts

$\dot{x}$ - air velocity in the ducts.

It has been assumed that the air density is constant, the room is at a uniform temperature, the return air is at room temperature, and the flowrate into the room equals the flowrate out of the room.

If the equations are combined, and the temperatures are expressed as deviations from the initial, equilibrium temperature then

$$\rho CV \frac{dv_R}{dt} = \rho CA \dot{x} (v_I - v_R) - f_O .$$

$$v_r = \theta_R - \theta_{Go}$$

$$v_i = \theta_I - \theta_{Go}$$

The Laplace transform is

$$(\tau_2 s + 1)V_R = V_I - k_6 F_o$$

where V_R - the Laplace transform of v_R

V_I - the Laplace transform of v_I

F_o - the Laplace transform of f_o

$$\tau_2 = V/A\dot{x} \quad \text{and}$$

$$k_6 = 1/\rho C A \dot{x} \quad .$$

Rearranging yields

$$V_R = \left(\frac{k_6}{\tau_2 s + 1} \right) \left(\frac{1}{k_6} V_I - F_o \right) \quad .$$

The schematic diagram for this relation is

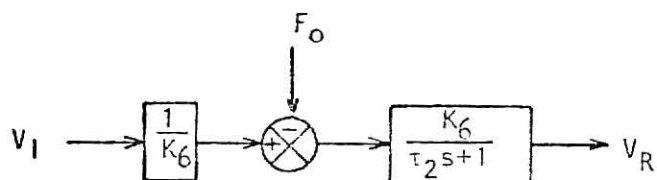


Figure 19. Room Block Diagram.

Applying the heat balance to the heating coil yields

$$f_s = \rho C A \dot{x} (\theta_I - \theta_M) + \rho_E C_E V_E \frac{d\theta_I}{dt}$$

where $\theta_M = M\theta_o + (1-M)\theta_R$ and

f_s - heat flowrate into the coil from the steam (BTU/hr)

θ_M - mixed air temperature entering the coil ($^{\circ}\text{F}$)

M - fraction of outside make-up air

ρ_E - density of exchanger (lb_m/ft^3)

C_E - specific heat of exchanger material ($\text{BTU}/\text{lb}_m\text{-}^{\circ}\text{F}$)

V_E - volume of exchanger (ft^3)

Taking the temperatures as deviations from the equilibrium temperature yields

$$(\tau_1 s + 1)V_I = MV_O + (1-M)V_R + K_4 F_S$$

where F_S - the Laplace transform of f_s

$$\tau_1 = \rho_E C_E V_E / \rho C A \dot{x}$$

and $K_4 = 1/\rho C A \dot{x}$

Rearranging,

$$V_I = \left(\frac{k_4}{\tau_1 s + 1} \right) \left(\frac{M}{k_4} V_O + \frac{(1-M)}{k_4} V_R + F_S \right)$$

In block diagram form, the relation is

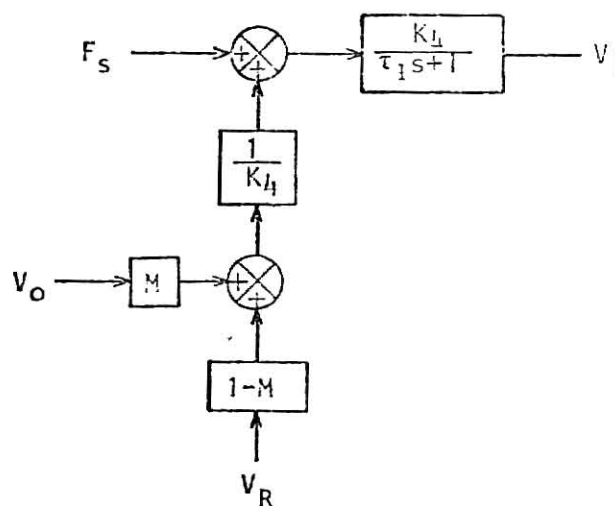


Figure 20. Heating Coil Block Diagram.

The steam flowrate into the coil may be assumed to be proportional to the valve opening, which is proportional to the difference in the setpoint and sensed room temperature, thus

$$F_s = K_1 K_2 K_3 (V_{SET} - V_R)$$

where K_1 - thermostat gain

K_2 - actuator gain

K_3 - valve gain

$$V_{SET} = R - \theta_{Go}$$

R - set point temperature.

In block diagram form,

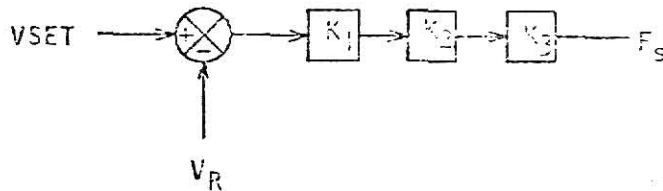


Figure 21. Steam Flow Control Block Diagram.

Heat conduction per unit area through the walls is given by equation (18).

$$F_o = -\frac{A}{B} V_I + \frac{1}{B} V_o$$

When the area of the wall is considered, the total heat loss due to heat conduction through the walls for this development is given by the following relation. Observe that the variable, F_o , is used to signify BTU per hour rather than the previous BTU per hour per square foot.

$$F_o = \text{SAREA} \left(-\frac{A}{B} V_R + \frac{1}{B} V_o \right) .$$

SAREA - surface area of the wall

In block diagram form,

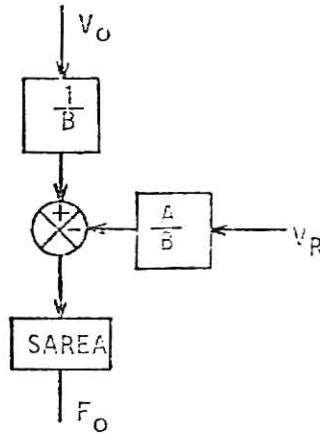


Figure 22. Block Diagram for Multi-Layer Wall.

The block diagrams may be combined and then reduced to obtain the following block diagram for the entire temperature control system including the walls as shown in Figure 10.

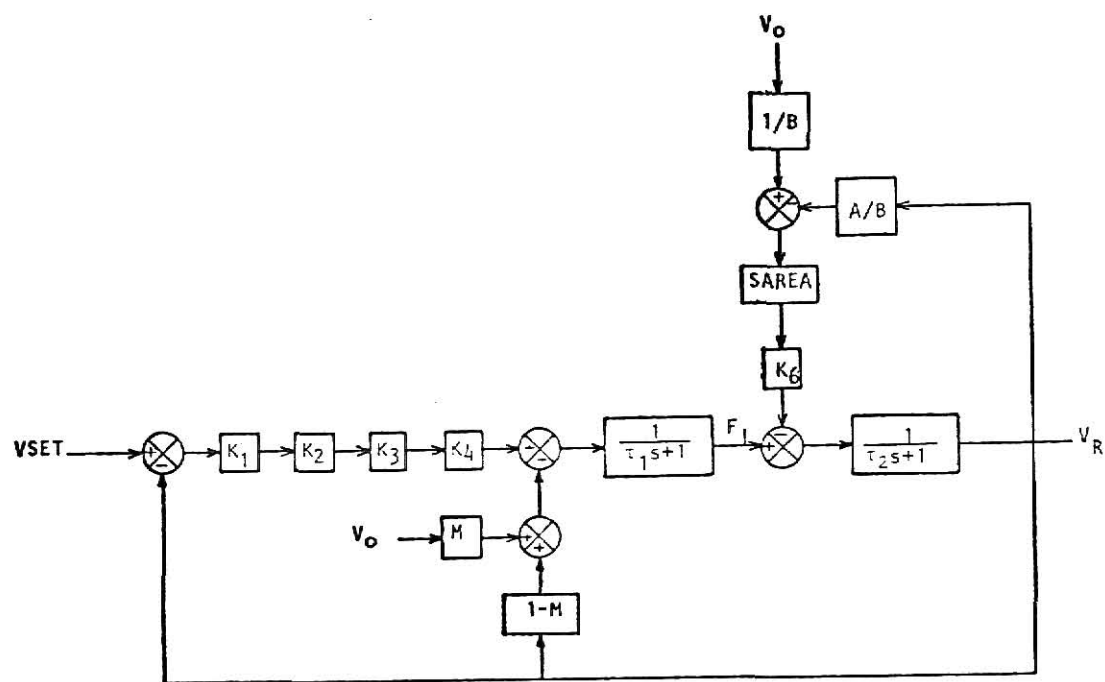


Figure 23. Air Conditioning Control System Block Diagram.

APPENDIX G - SYSTEM SIMULATION PROGRAM

\$JGB

```

    IMPLICIT REAL*8(A-H,C-Z)
    DIMENSION YO(3),Y1(3),Y2(3),Y3(3),Y4(3),Q0(3),Q1(3),Q2(3),
    103(3),Q4(3),DERY(3),A(70),B(70),C(70),U(220),V(220),TOUT(220),
    1F(220)
20  FORMAT('0','X=',F21.16,5X,'Y1=',F25.16,5X,'Y2=',F25.16)
21  FORMAT(' ',25X,'DERY1=',F25.16,5X,'DERY2=',F25.16)
22  FORMAT(F24.16)
23  FORMAT(' ',15X,'IPT=',I5,5X,'F=',F25.16)
24  FORMAT(I5)
    READ(5,24) ITHETA
    DO 8 I=1,ITHETA
      8  READ(5,22) A(I)
      DO 9 I=1,ITHETA
        9  READ(5,22) B(I)
      DO 10 I=1,ITHETA
        10 READ(5,22) C(I)
        SAREA=250.000
        NDIM=2
        XGO=0.000
        XEND=10.500
        H=0.02500
        DELTA=C.1000
        IEND=((2.000*(XEND-XGO))/DELTA)+1.000
        TGO=70.000
        YO(1)=0.000
        YO(2)=0.000
        DERY(1)=0.000
        DERY(2)=0.000
        DO 11 I=1,IEND
          TOUT(I)=50.000
11  V(1)=TOUT(I)-TGO
          V(1)=0.000
          V(2)=-10.000
          X=XGO
          IPT=0
          DO 1 I=1,NDIM
            1  Q0(I)=0.000
13  IPT=IPT+1
          U(IPT)=YO(2)
          CALL FCALC(A,B,C,ITHETA,TGO,J,V,IPT,F)
          F1=YO(1)/2.2730-3
          WRITE(6,20) X,F1,YO(2)
          WRITE(6,21) DERY(1),DERY(2)
          FOUT=F(IPT)*SAREA
          WRITE(6,23) IPT,FOUT
          IF(X.GE.XEND)GO TO 12
          ITRK=0
7  ITRK=ITRK+1
          IF(ITRK.GT. 4) GO TO 13
          CALL FCT(X,YO,DERY,V,TGO,IPT,F,SAREA)
          DO 2 I=1,NDIM
            2  R1=H*DERY(I)

```



```

      SUBROUTINE FCALC(A,B,C,ITHETA,TGO,U,V,IPT,F)
      IMPLICIT REAL*8(A-H,C-Z)
C*****
C      FCALC FINDS THE HEAT FLUX AT THE INNER SURFACE OF A MULTILAYER
C      STRUCTURE, WHEN IT IS GIVEN THE 7-COEFFICIENTS FOR THE STRUCTURE,
C      A, B, AND C, THE NUMBER OF INDIVIDUAL COEFFICIENTS, ITHETA, THE
C      INITIAL WALL TEMP, TGO, INSIDE TEMP, TIA, OUTSIDE TEMP, TJUT,
C      AND THE SURFACE AREA OF THE STRUCTURE, SAREA. FCALC USES THE
C      EQUATIONS FROM TABLE 2.
C*****
      DIMENSION A(ITHETA),E(ITHETA),C(ITHETA),
1      IF(IPT),FLT(120),FRT(120),U(120),V(120)
      IF(IPT.GT.ITHETA)GO TO 11
      IPHI=IPT
      RT=0.000
      RTER=C.000
      GT=0.000
      N=0
10     N=N+1
      M=IPHI-N+1
      IF (N.EQ.1)GO TO 12
      GT=GT+(F(M)*B(N))
12     FLT(IPHI)=GT
      RT=RT+(U(M)*A(N))
      RTER=RTER+(V(M)*C(N))
      IF (N.LT.IPHI)GO TO 10
      FRT(IPHI)=-RT+RTER
      F(IPHI)=(FRT(IPHI)-FLT(IPHI))
      GO TO 30
11     IFLY=IPT
50     RT=0.000
      GT=0.000
      GTER=0.000
      M=0
      IFLY=IFLY+1
      N=IFLY
51     M=M+1
      N=N-1
      GT=(U(N)*A(M))+GT
      GTER=(V(N)*C(M))+GTER
      IF (M.EQ.1)GO TO 51
      RT=RT+(F(N)*B(M))
      IF (N.LT.ITHETA)GO TO 51
      IGOT=IFLY-1
      F(IGOT)=(-GT-RT+GTER)
30     CONTINUE
      RETURN
      END
$ENTRY

```

ACKNOWLEDGEMENTS

The author wishes to extend sincere appreciation to the Mechanical Engineering faculty for very generously giving time and wisdom throughout his education.

A special recognition goes to my wife, Susan, for her faithful encouragement and economic support during this study.

The assistance and inspiration from Dr. J. Garth Thompson are deeply appreciated.

Appreciation is also extended to Dr. Everett E. Haft and Dr. Robert L. Gorton for serving as committee members.

The author also acknowledges the Mechanical Engineering Department for the financial aid it provided.

VITA

Terry Del Hubbs

Candidate for the Degree
Master of Science

THESIS: HEAT CONDUCTION TRANSFER FUNCTIONS FOR MULTI-LAYER STRUCTURES

MAJOR FIELD: Mechanical Engineering

BIOGRAPHICAL:

Personal Data: Born in Salina, Kansas, November 15, 1953; the son of the late Delwin Victor Hubbs and Vivian M. Herbel.

Education: Graduated from Dorrance High School in 1971; received a Bachelor of Science degree in Mechanical Engineering from Kansas State University in May 1975; completed requirements for the Master of Science degree in April 1977.

Honors and Societies: 1975 Mac Short Award recipient; Pi Tau Sigma, mechanical engineering honorary; Triangle Fraternity, engineering, architecture, and science fraternity.

HEAT CONDUCTION TRANSFER FUNCTIONS FOR
MULTI-LAYER STRUCTURES

by

TERRY DEL HUBBS

B.S., Kansas State University, 1975

AN ABSTRACT OF A MASTER'S THESIS

submitted in partial fulfillment of the
requirements for the degree

MASTER OF SCIENCE

Department of Mechanical Engineering

KANSAS STATE UNIVERSITY
Manhattan, Kansas

1977

NAME: Terry D. Hubbs

DATE OF DEGREE: May 20, 1977

INSTITUTION: Kansas State University

LOCATION: Manhattan, Kansas

TITLE OF STUDY: HEAT CONDUCTION TRANSFER FUNCTIONS FOR MULTI-LAYER
STRUCTURES

PAGES IN STUDY: 90

CANDIDATE FOR DEGREE OF MASTER OF SCIENCE

MAJOR FIELD: Mechanical Engineering

To investigate the effect of control system dynamics on energy consumption, a simulation with a time stepsize short enough to manifest the dynamics of the control system is required. The purpose of this thesis is to demonstrate and satisfactorily document an algorithm for transient heat conduction through multi-layer walls that may be used as an element in such a simulation.

The algorithm developed and applied is the response factor technique. Laplace transforms are employed to attain conduction transfer functions that relate inner temperature and heat flux to outer temperature and heat flux for multi-layer structures. The Laplace transforms are inverted with z-transforms, placed in the form of a ratio of infinite power series in z^{-1} , and expanded to acquire solutions as a function of time. A detailed derivation of the concept is included.

Computer programs that evaluate the constants necessary to apply the algorithm are listed and described. One program finds roots of hyperbolic functions that describe the structure, another calculates the coefficients of the z-transfer functions, and a third uses the coefficients to compute heat flux at the inner surface of the wall.

The concept is demonstrated on a double and then a triple-layer wall with identical inputs and the outputs are compared. A room temperature

control system is modeled where the walls are simulated with the response factor algorithm. The model is subjected to various inputs.

This response factor algorithm may be used on walls with any number of layers, with or without surface resistances, and has a variable time stepsize. Accuracy depends primarily upon truncation error. The algorithm's strongest point is speed, resulting in reduced computing expense. This advantage makes it recommendable for applications where a wall or set of walls are to be studied a number of times.