THE IRRADIATION EFFECTS ON THE SOLVENT EXTRACTION SYSTEM OF TRIBUTYL FHOSPHATE-DODECANE

by

JOE PASCHAL HOLLAND

B.S., Kansas State University, 1974

A MASTER'S THESIS

submitted in partial fulfillment of the requirements for the degree

MASTER OF SCIENCE

Department of Nuclear Engineering

Kansas State University Manhattan, Kansas 66506

1977

Approved by

ajor Professor

LD 2668 T4 1977 H64 c.2 Document

L'Chaim,

Family,

and

Friends

ILLEGIBLE DOCUMENT

THE FOLLOWING
DOCUMENT(S) IS OF
POOR LEGIBILITY IN
THE ORIGINAL

THIS IS THE BEST COPY AVAILABLE

TABLE OF CONTENTS

<u>Pag</u>	ţе
List of Tables	i
List of Figures	i
Nomenclature	V
Introduction	1
Theory	5
Experimental Procedure	3
Results and Conclusions	7
Bibliography	7
Acknowledgements	9
Appendices	
Appendix A (Physical Properties of the TBP-dodecane	
system)	<u>)</u>
Appendix B (UV Spectrophotomater Results) 43	3
Appendix C (Dose Rate Program) 45	;
Appendix D (Saunders-Taylor Calibration Date) 51	
Appendix E (Gas Chromatograph Data)	,

LIST OF TABLES

		Page
1	Radiolysis Products from Liquid Hexane (${}^{\mathrm{C}}_{6}{}^{\mathrm{H}}_{14}$)	. 8
2	Radiolysis Yield of Pure TBP: Low L.E.T.	
	Irradiation	. 12
A-1	Physical Properties of Butyl Phosphates	. 42
A-2	Physical Properties of Dodecane	. 42
A-3	TBP-Dodecane Mixture Data	. 42
D-1	Saunders-Taylor Calibration Data	. 51
E-1	Varian 90P3 Gas Chromatograph Data	. 52

LIST OF FIGURES

		Page
1.	Molecular Structure of TBP	4
2.	Sketch of the Irradiation Cell	17
3.	Schematic of Sample Cell Holder	18
4.	Schematic View of Saunders-Taylor Apparatus	19
5.	Schematic View of Gas Sampler	20
6.	Titration Curve for a 10 ml sample of H ₂ 0	21
7.	Titration Curve for 2 ml of TBP in 10 ml of H_2^0	22
8.	Titration Curve for 15 ml of 0.1N DBP	23
9.	Titration Curve for 15 ml of 0.1N MBP	24
10.	Titration Curve for 2 ml of irradiated TBP in 10 ml	
	of H ₂ 0. (TBP sample T-182)	25
11.	Titration Curve of 10 ml of 0.01N DBP and 0.002N	
	MBP	26
12.	Plot of Product Yields as a Function of Dose for	
	TBP and Dodecane	34
13.	Plot of $G(H_2)$ as a Function of Electron Fraction TBP	
	in Dodecane, Absorbed Dose, 2 Watt-hr/Liter	35
14.	Plot of G(Acid) as a Function of Electron Fraction	
	TBP in Dodecane, Absorbed Dose, 2 Watt-hr/liter	36
B-1	UV Spectrophotometric Results for Spectral Grade,	
	Purified Practical Grade, and Unpurified Practical	
	Grade Dodecane	44

NOMENCLATURE

Mwd mega-watt days

tonne metric ton, 1000 kilograms

MeV 10⁶ electron volts

keV 10³ electron volts

eV electron volt

G(X) the yield of "X" component in molecules per 100 eV

ε electron fraction

mm millimeter

tor | millimeters of mercury (pressure)

°K degrees Kelvin

N gram equivalent weight of solute per liter of solution

M molecular formula weight per liter of solution

rad 100 ergs absorbed energy per gram of material

min minute

°C degrees Centigrade

ml milliliter, 10⁻³ liter

g gram

mp millipoise, 10⁻³ poise

pK negative log of the ionization constant

v/o volume per cent

1.0 INTRODUCTION

Nuclear fuel is reprocessed to recover fissile and fertile species such as uranium, plutonium, and thorium from the accumulated fission products. Solvent extraction, ion exchange, and pyrometallurgical processes are three reprocessing techniques. Of the three, solvent extraction is the best developed and most common.

A solvent extraction is the separation of various chemical species dissolved in a solvent, by the transfer of certain chemical species to another solvent, immiscible with the first solvent. The transfer takes place due to the greater solubility of the transferred constituents in the second solvent than in the first solvent.

Dilute nitric acid is typically used to dissolve the spent fuel and tributyl phosphate (TBP) is used as the second immiscible solvent in the Purex system [5]. TBP is used as the solvent due to its ability to form a complex with uranium, plutonium, and thorium in the forms, $UO_2(NO_3)_2$. 2TBP, $Pu(NO_3)_4$. 2TBP, and $Th(NO_3)_4$. 2TBP. These complexes are more soluble in the organic phase, TBP, than in the inorganic phase.

TBP is an organic ester of phosphoric acid and the structure is shown in Fig. 1. TBP has tetrahedral symmetry with one double oxygen-phosphorous bond and three single butoxy-phosphorous bonds. Physical properties of TBP are listed in Appendix A. TBP is stable toward oxidation and nitric acid, the usual aqueous phase, and undergoes alkaline hydrolysis [1,2]. The hydrolysis produces dibutyl phosphate (DBP), and monobutyl phosphate (MBP), and phosphoric acid. Since this hydrolysis reaction is slow, it is a minor problem. Pure TBP is viscous and the density is within 3% of water, therefore it must be diluted for solvent extraction use.

The most commonly used diluent is dodecane, generally industrial grade of about 90% purity. Dodecane is used because it is economical, has a density of 0.75 g/cm³, and its radiolytic degradation products don't significantly complex with materials such as zirconium [3]. The physical properties of dodecane are also listed in Appendix A.

The Purex solvent extraction process, using a mixture of dodecane and TBP, dates back to the early post World War II development work to find a replacement for the Hanford bismuth precipation process [4,5].

Due to its use in the production of plutonium for the weapons program, a great deal of experience is available. However, this experience is with low burnup fuel, typically less than 1000 Mwd/tonne. Very little experience is available with high burnup fuel, 30,000 Mwd/tonne or greater, that is produced by current generation light water reactors (LWR). Even less experience is available concerning light water thermal breeder reactors or liquid metal fast breeder reactor fuels, where burnups of greater than 100,000 Mwd/tonne are foreseen.

High fuel burnups not only increase the specific activity of the spent fuel, but also cause an increase in the fraction of energy released in the form of alpha particles. Alpha particles have a higher Linear Energy Transfer (L.E.T.) than beta or gamma radiation, where L.E.T. is defined as the energy deposited per unit length of track [6]. Since high L.E.T. irradiation causes the damage to a medium to be more localized and concentrated, there is the possibility for significantly different chemical reactions to dominate, than dominate for low L.E.T. irradiations.

For low L.E.T. experimental results to be meaningful to the reprocessing problems for the near future, the emphasis should be placed on basic understanding of the chemical mechanism and the reaction rates. This kind of

basic knowledge is necessary to allow reasonable extrapolation to the conditions to be encountered, as opposed to the typical reprocessing literature which is a tabulation of radiolysis products with little information about reaction mechanisms.

In this work irradiations of dodecane, TBP, and mixtures of the two were made and analyzed. Gaseous products were measured by a combination of gas chromatography and pressure-volume-temperature analysis. Acid products were determined by potentiometric titration. This work was performed as a first step in the understanding of the physical and chemical reactions involved in the degradation of reprocessing solvents.

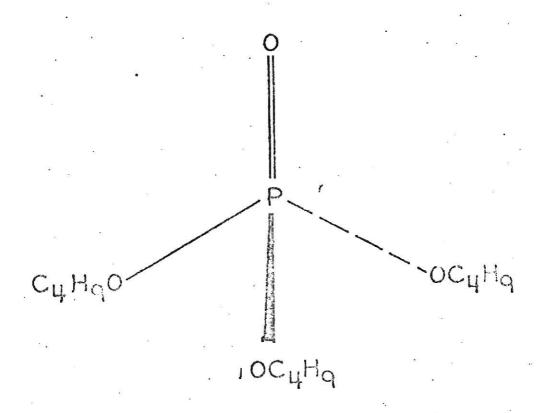


Fig. 1: Molecular Structure of TBP.

2.0 THEORY

2.1 Types of Radiation

Radiation encountered in the reprocessing of spent nuclear fuel will be gamma, beta, and alpha. In the following, the types and significance of primary interactions of these radiations will be discussed.

2.1.1 Beta Particles

Beta particles are energetic electrons produced by the decay of an unstable nucleus. The betas encountered in nuclear fuel reprocessing have an average energy of about 0.5 MeV and are the result of fission product decay. Due to the low penetrating capability of beta particles, essentially all the energy of the beta particles is deposited in the processing stream.

The three major types of interaction of an electron with matter are bremstrahlung, elastic scattering, and inelastic scattering. The atomic mass of dodecane or tributyl phosphate (TBP) is too low for significant bremstrahlung and too high for significant elastic scattering. Inelastic scattering will dominate.

Inelastic scattering occurs when an electron undergoes a coulombic interaction with the electrons in the irradiated material, producing ionized and excited molecular states. The electron ejected from the molecules by the beta particle will have sufficient energy to cause further ionization and excitation. Cascades of second, third, and higher order electrons can be produced [7]. The excited states produced by the beta particles and subsequent electrons are similar to those produced by optical transitions, however more triplet states are observed due to a relaxation of the optical selection rules [8].

2.1.2 Gamma Rays

Since the source of gamma radiation in nuclear fuel reprocessing is fission product decay, almost all gamma rays produced will have an energy of less than 10 MeV [9]. Below 10 MeV the two major photon interaction mechanisms are Compton scattering and the photoelectric effect.

In Compton scattering, the incident photon interacts with an electron of the medium, causing the electron to be accelerated and the incident photon to be scattered at a lower energy. The energy of the scattered photon and electron can be calculated from the energy of the incident photon (see almost any introductory physics text such as "Nuclear Physics," by I. Kaplan). For example, a 0.661 MeV incident gamma ray will produce a scattered electron of approximately 0.5 MeV maximum energy. This scattered electron undergoes inelastic scattering with the electrons of the medium.

Photoelectric effect is the process of absorption of an incident photon by an atom which then ejects an inner shell electron with an energy equal to the incident photon energy minus the electron binding energy. This leaves the atom ionized and in an excited state. However this mechanism is of secondary importance to Compton scattering except for photon energies of less than 100 keV [7,10].

The result of photon absorption is the same for both Compton scattering and photoelectric effect, energetic electrons, ionization, and excited states. Beta particles produce these same species, therefore beta radiation can be simulated by gamma radiation. However, gamma and beta radiation can not be treated identically due to the much greater penetrating power of gamma radiation, which allows significant energy to escape the reprocessing stream.

2.1.3 Alpha Particles

Alpha particles are heavy, energetic, charged particles (He²⁺), produced from the decay of an unstable nucleus. They interact with matter much the same way as beta particles, bremstrahlung, elastic scattering, and inelastic scattering. However, since the alpha particle is more massive than a beta particle, the alpha particles move more slowly and inelastic scattering is the only significant interaction.

The alpha particle has a much higher Linear Energy Transfer (L.E.T.)

resulting in a shorter interaction track and a higher density of inter
actions than a beta or gamma. These interactions have the same intermediate

products as beta or gamma particles, but the much higher density can lead

to a different distribution of final reaction products.

2.1.4 Relative Importance

Traditionally, the only significant radiation encountered in nuclear fuel reprocessing was beta and gamma rays. High burnup fuel however, has significant transuranic isotopes present that are very active alpha emmitters, so the effect of high L.E.T. radiation should be considered.

2.2 Radiolysis Products

Alkane radiolysis results in hydrogen production, olefin generation, dimerization, and generation of fragments \mathbf{C}_1 to \mathbf{C}_n which can then combine in pairs. The major species evolved are hydrogen, dimer, and olefin.

Hexane, ${}^{C}_{6}{}^{H}_{14}$, has been studied in considerable detail and the following, Table 1, is a tabulation of radiolysis products [11]. The G value is defined as the number of that species produced per 100 eV of absorbed energy. These types of results are typical for alkane radiolysis. However, alkane structure

Table 1. Radiolysis Products from Liquid Hexane (C_6H_{14})

85	Product	G Value	
	н ₂	5.0	
	cii ₄	0.12	
	$c_2^H_2$	0.3	
	c ₂ H ₄	0.3	
	с ₃ н ₆	0.13	
	с ₃ н ₈	0.42	
	$c_4^{H_8}$	0.03	
	C4H ₁₀	0.50	
	i-C4H ₁₀	0	
	C ₅ H ₁₂	0.30	
	trans-C ₆ H ₁₂	0.2	
	i-C ₆ H ₁₄	0	
SI#Y	c ₇	0.15	
		0.53	
	с ₈ с ₉	0.45	
	c ₁₀	0.43	
	c_{11}	0.02	
	c_{12}	2.0	

does effect the final product yield. Branched alkanes with more tertiary carbon hydrogen bonds generally have greater methane yields and long chain alkanes have a definite tendency to cleave carbon-carbon bonds toward the middle of the chain. This leads to a final radiolysis product yield shifted toward species with a greater number of carbon atoms than the parent.

Numerous mechanisms have been proposed to account for these observed results, the one currently favored is a sequence of radical reactions. Excited states, produced directly by ionizing radiation or as a result of geminate ion recombination, are the source of radical species. Ion

mechanisms in a nonpolar medium, such as an alkane, are thought to be quite limited due to the rapid geminate recombination rate. Conductivity measurements on aliphatic hydrocarbons indicate that less than 3% of the electrons produced as a result of ionization, diffuse into the bulk medium before recombination with the parent ion [12].

The radical reaction mechanism can be represented by the following reaction sequence:

Where R, R', R'', R''', and R'''' are alkyl groups of differing length.

Product yields (G_m) from the irradiation of a homogeneous mixture of two materials would be expected to be equal to the yield from a single component (G_a) times its electron fraction (E_a) plus the yield from the second component (G_b) times its electron fraction (E_b) , this is called the mixture law. However, significant deviation from this situation has been observed in binary solutions such as cyclohexane/benzene.

^{*}Mathematically, $G_m = G_A E_A + G_B E_B$.

The cyclohexane/benzene system is one of the best studied mixture law deviations and there is still considerable disagreement concerning the mechanism. The deviation mechanism has been suggested to be excitation transfer, chemical scavenging, or charge transfer.

The presence of benzene suppresses the yield of hydrogen, cyclohexyl radical, and the dicyclohexyl radical [13]. This result can be interpeted as excitation transfer from excited cyclohexane to benzene, which would undergo a radiative or a nonradiative transition to the ground state. This excitation transfer would have prevented the formation of radical species from the excited state of cyclohexane [13,14,15]. Since benzene can undergo electronic transition without breaking chemical bonds, the total number of radical species has decreased. Another interpetation is that of Dyne [13], who suggested that the benzene quenched ${\rm C_6H_{12}^+}$ and ${\rm e^-}$ prior to geminate recombination of the ions which would lead to excited state cyclohexane. A case can be made for chemical quenching by radical addition to benzene, since phenylcyclohexane and dicyclohexadienyl have been observed [13] in cyclohexane/benzene mixtures and not in irradiations of the pure components.

The mixture of TBP and dodecane has considerable potential for deviation from mixture law. The combination of nonpolar dodecane and polar TBP opens the possibility of significant ion reactions since the increased polarity of the solute could reduce the geminate recombination rate of the parent alkane ions.

The literature concerning TBP/dodecane mixture law deviations is limited and conflicting. Barelko [16] and Williams [17] observed mixture law deviations. However Burger [18] did not observe deviation from the mixture law with a mixture of TBP and iso-octane. Differences in experimental techniques of dosimetry, sample purification, and duration and rate of radiation exposure makes evaluation of the literature difficult.

Another difficulty in looking at mixture law deviations of the TBP/dodecane system is that the literature of the single components is poor. For example, the reported radiolysis yields of gaseous products from TBP range from a G value (number of molecules/100 eV) of less than 0.24 [19] to 3.1 [20]. The dodecane literature is almost nonexsistent; Barelko [16] reports a gas yield, volatile at an unknown temperature, of G = 3.8 and Dewhurst [21] reports a $G(H_2) = 4.9$ and $G(CH_4) = 0.05$. TBP radiolysis yields and products are tabulated in Table 2.

Table 2. Radiolysis Yields of Pure TEP: Low L.E.T. Irradiation

G(H ₂)	G(DBP)	G(H ₂) G(DBP) G(MBP) G(G(Acid)	С(СН ₄)	G(BuOH)	G(Total Hydrolysis)	Reference
2.02			3.71	0.032		•	[this work]
1.72	2.44	0.14	2.58	0.072			[20]
2.5	1.9	0.3	2.2		0.65		[27]
1.11	1.52	0.12	1.64	0.05	0.0		[17]
						0.24	[19]
1.5 (total gas)	1.86				0.78		[16]
1.59	2.25	0.39	2.64	0.07	0.13		[28]

3.0 EXPERIMENTAL PROCEDURE

The preparation and irradiation of samples and the determination of product yields are discussed in this section.

3.1 Sample Preparation

The samples consisted of dodecane, tributyl phosphate (TBP), and mixtures of these two components. Preparation consisted of sample purification and degassing. These steps are outlined below.

3.1.1 Sample Purification

The tributyl phosphate (TBP) (Matheson, Coleman & Bell Inc., white label grade) was found, from potentiometric titrations, to have less than 0.1% acid impurities and was used as received. The dodecane (Matheson, Coleman and Bell, Inc., practical grade) was treated with fuming sulfuric acid (30% SO₃) to remove unsaturated impurities and then the remaining unreacted acid and impurities were removed. Residual acid was neutralized by the addition of a 2% sodium carbonate solution. Next the dodecane was passed through approximately 24 inches of 28-200 mesh silica gel at about one drop per second. This step was performed twice. The resulting dodecane was analyzed on a Cary 14 UV spectrophotometer and found to be near manufacturers specifications for spectral grade dodecane. UV spectrometry results are shown in Appendix B.

3.1.2 Degassing

The samples were degassed in two steps. The first was to pass dry clean helium through the sample for a period of four to eight hours. This reduced the concentration of atmospheric gases, which shortened the time and improved the results of the cell degassing.

The irradiation cell (Fig. 2) was attached to the high vacuum manifold by means of a "butt" joint using 10 mm, thick wall glass tubing. The cell was evacuated and held at 10^{-6} torr for at least 24 hours to outgas the cell walls. The cell was then repressurized to slightly greater than one atmosphere with clean dry helium. The side arm of the cell was then flame cracked open, allowed to cool, and a five ml sample injected using a syringe with a four inch needle. Care was exercised to minimize the amount of sample material deposited on wall of side arm to reduce the chance of pyrolysis. Carbon monoxide and other unidentified substances found in some of the early irradiations are attributed to pyrolysis. The sample was frozen to 195 °K with a dry ice/ethanol bath, side arm resealed, and the cell evacuated. The dry ice/ethanol bath was used instead of liquid nitrogen (77 °K) to remove possible gaseous pyrolysis products. Once the cell was evacuated to under 10⁻⁵ torr, the cell was isolated from the vacuum system and thawed to room temperature. The freeze-pump-thaw cycle was repeated until the system pressure increased to less than 10^{-5} torr upon opening the cell to the vacuum system.

At this time the 10 mm thick wall glass tubing connecting the cell to the vacuum system manifold was gently flamed to drive off residual sample material. The tube wall was then heated to softening temperature of glass, allowing the tube walls to collapse inward, making a vacuum seal and was then removed.

3.2 Irradiation and Dosimetry

The irradiations were performed in a Gammacell (AECL 220) with repeatable positioning provided by an aluminum sample holder shown in Fig. 3. Dosimetry was done with the Fricke Dosimeter (Fe⁺² in 0.8N H₂SO₄) [22]. Due to strong axial and radial variations in dose rates, care was

exercised to have the dosimeter solution and the sample occupy the same position in the sample holder. This was done by using the same diameter glass tubing for the dosimeter cell as was used in sample cell and filling both cells to the same height.

Eighteen irradiations of dosimeters were done in each of the twelve positions of the sample holder, over an eight month period. The dose rates were normalized to the date of the first irradiation and the mean and standard deviation were determined. This dose rate, approximately 1100 rad/m, with a decay correction was used to calculate the dose absorbed by the dosimeter solution. A computer program was written to handle these calculations and a sample output and the program listing are shown in Appendix C. Dose correction factors were applied to correct for the difference in absorbed dose in dosimeter and organic sample solutions. These correction factors were calculated on an electron density basis and are found in Appendix A, Table A-3.

3.3 Gas Analysis

Analysis of the gaseous radiolytic products was done in two steps; determination of the total amount of gas and then the species of gases present. The total number of moles of gas volatile at 161 °K was determined by a pressure-volume-temperature (PVT) analysis on a Saunders-Taylor apparatus [23], shown in Fig. 4. Saunders-Taylor calibration data is given in Appendix D. A sample of the gas extracted was collected in a gas sampler, shown in Fig. 5. This gas sample was analyzed at 40 °C on a Varian 90P3 gas chromatograph, using a six foot, 60-80 mesh, molecular sieve 5A column, and a thermal conductivity detector. The gases were identified by the elution time and the relative amounts were determined by comparison

to calibration data for known amounts of nitrogen, oxygen, hydrogen, methane and carbon monoxide. Varian 90P3 calibration data are found in Appendix E. Detection of less than 0.1 micromoles was achieved.

3.4 Acid Determination: Potentiometric Titration

The yield of dibutyl phosphate (DBP) and monobutyl phosphate (MBP) was determined by titrating the irradiated solution with 0.012 M KOH. The equivalence point was determined with a Fisher model 38 pH meter equipped with a combination electrode. Two or four ml of the irradiated sample was pipetted into 10 ml of distilled water. The sample was mixed until broken down to an emulsion, at which time the water soluble DBP and MBP were in contact with the distilled water and were dissolved. The sample was then titrated with constant mixing. Titrations were made on unirradiated TBP, dodecane, distilled water, DBP, MBP, and a mixture of DBP and MBP. The purified MBP and DBP were produced by the procedure in Reference [30]. Correction factors for the residual acid concentration in TBP and water were applied. The dodecane was found to have insignificant acid impurities. A 90% DBP - 10% MBP mixture was prepared and titrated. The second proton from the diprotic MBP was detected and the MBP fraction was found to agree with the known value. However, the break in the titration curve was such that any lower concentration of MBP would not be resolved. Therefore, a yield of MBP, 10% of the DBP yield, seems to be the limit of resolution with potentiometric analysis. Sample plots of the titration curves are shown in Fig. 6 thru Fig. 11.

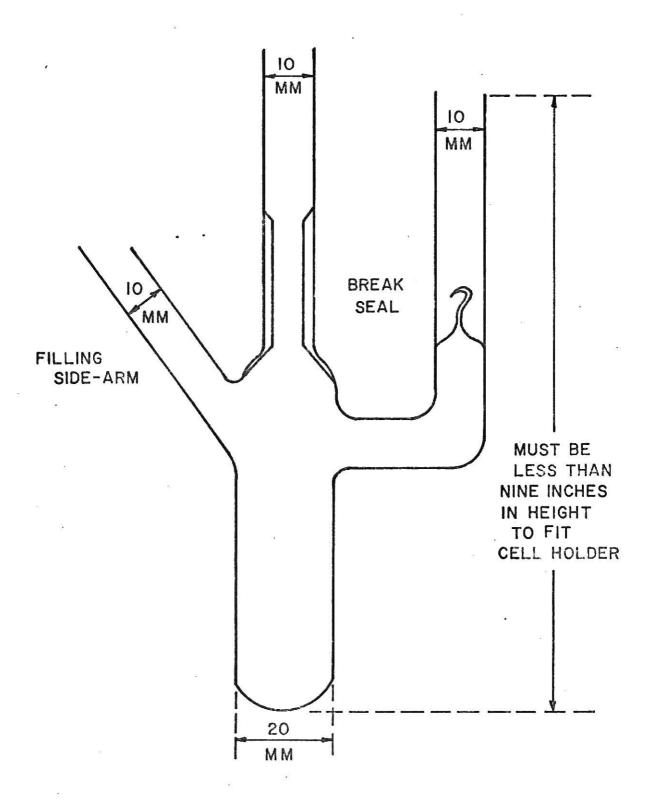


Fig. 2: Sketch of the irradiation cell[29]

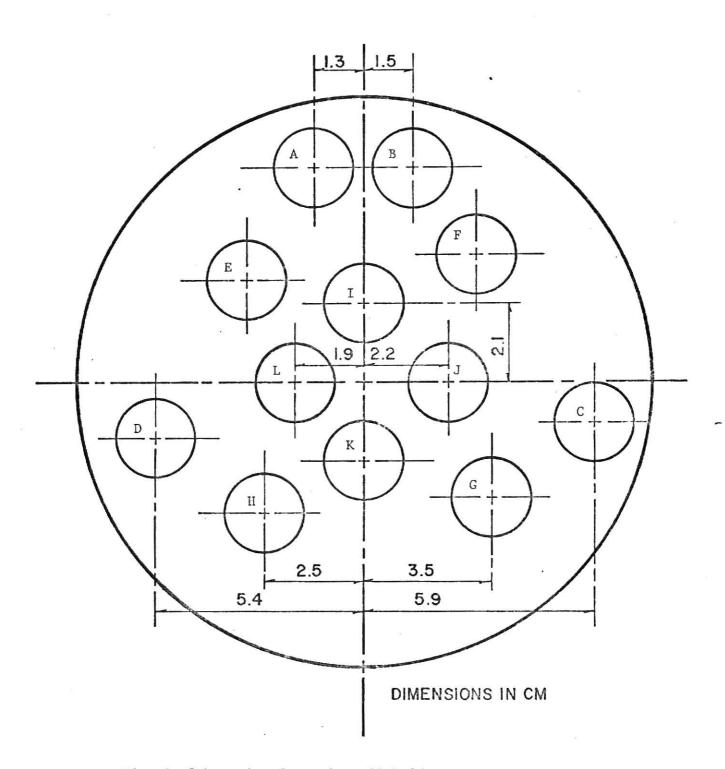


Fig. 3: Schematic of sample cell holder.

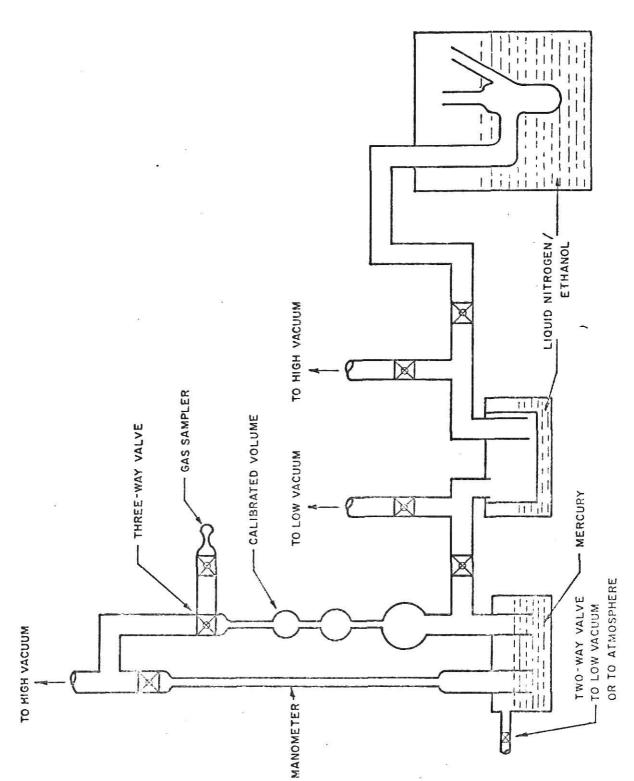


Fig. 4: Schematic view of Saunders-Taylor apparatus

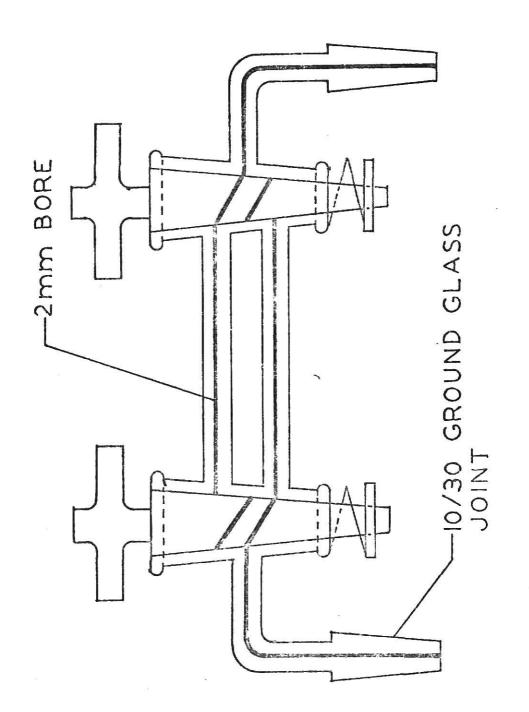


Fig. 5: Schematic view of gas sampler

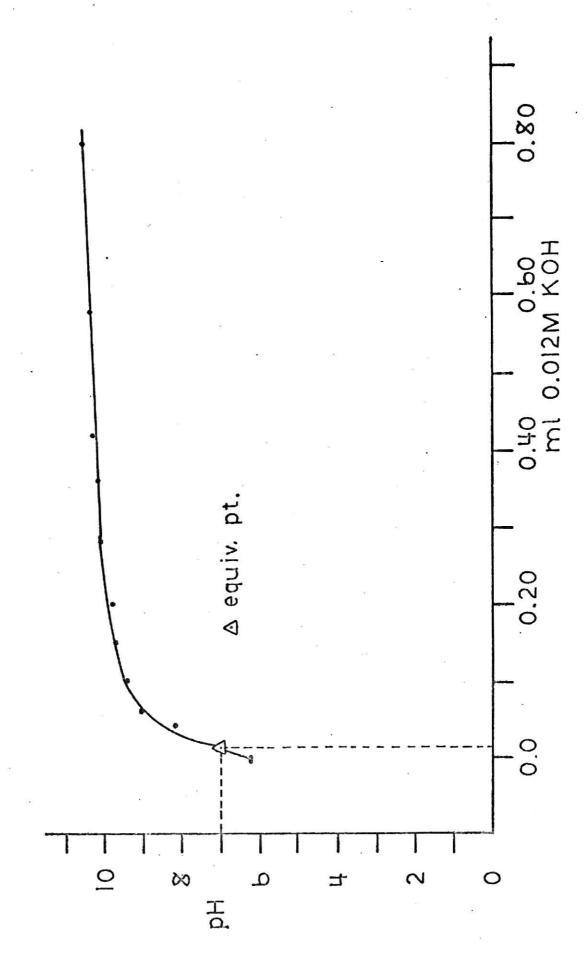


Fig. 6: Titration curve for a 10 ml sample of $\mathrm{H}_2^{\,\mathrm{O}}$.

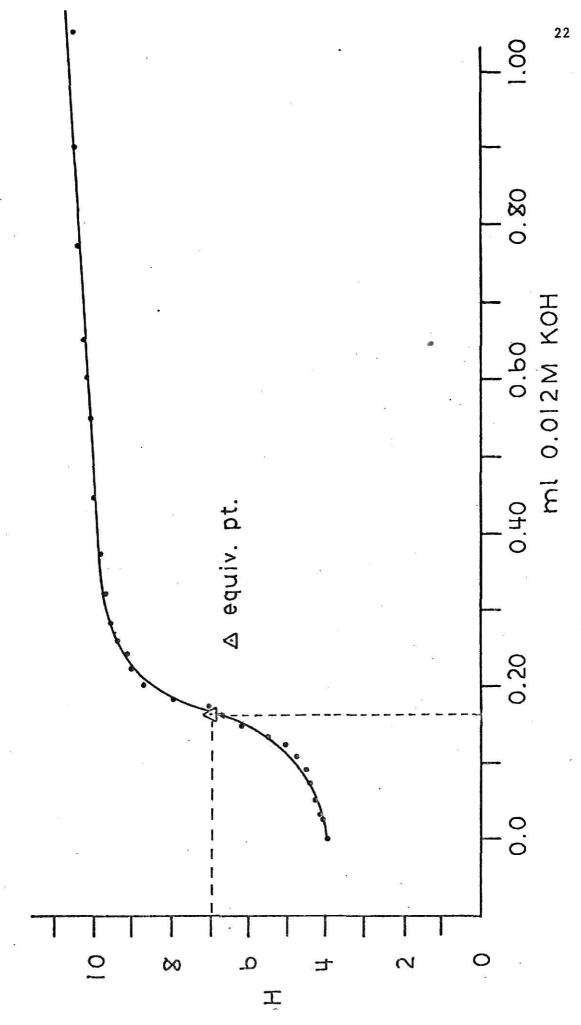


Fig. 7: Titration curve for 2 ml of TBP in 10 ml of H_2^{0} .

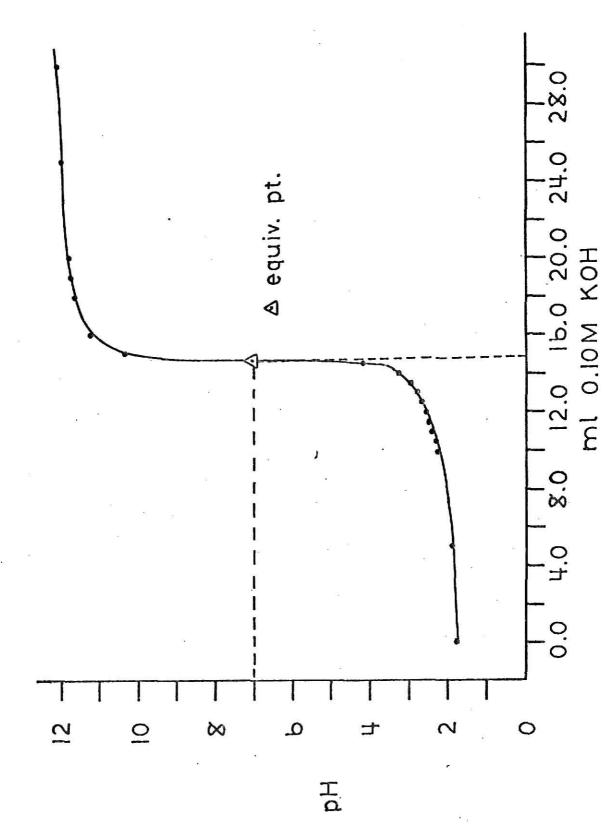


Fig. 8: Titration curve for 15 ml of 0.1N DBP.

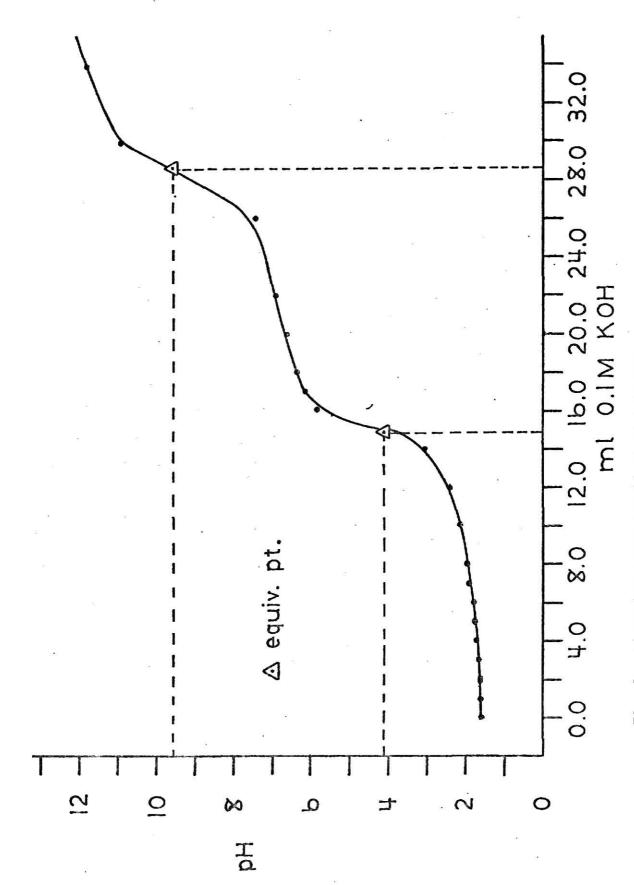
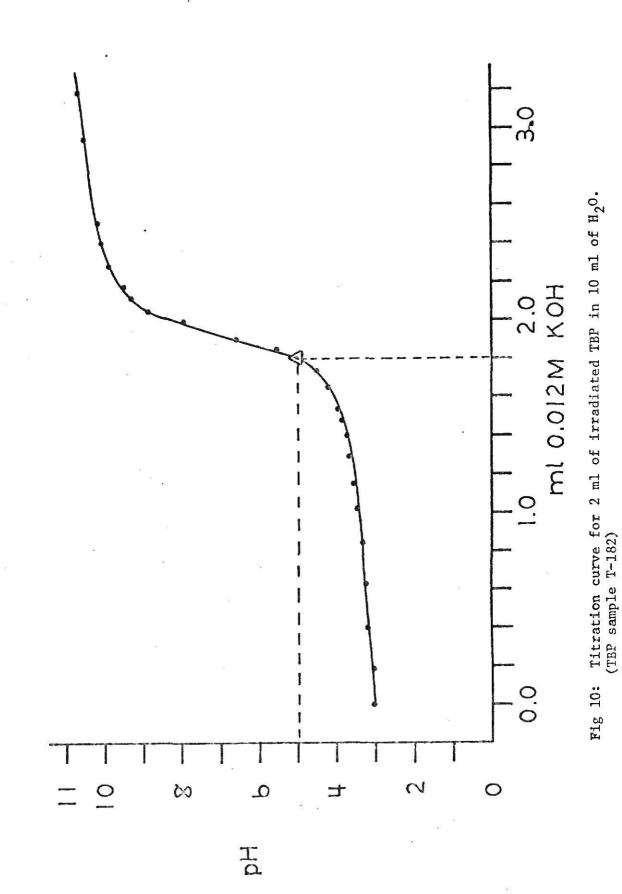
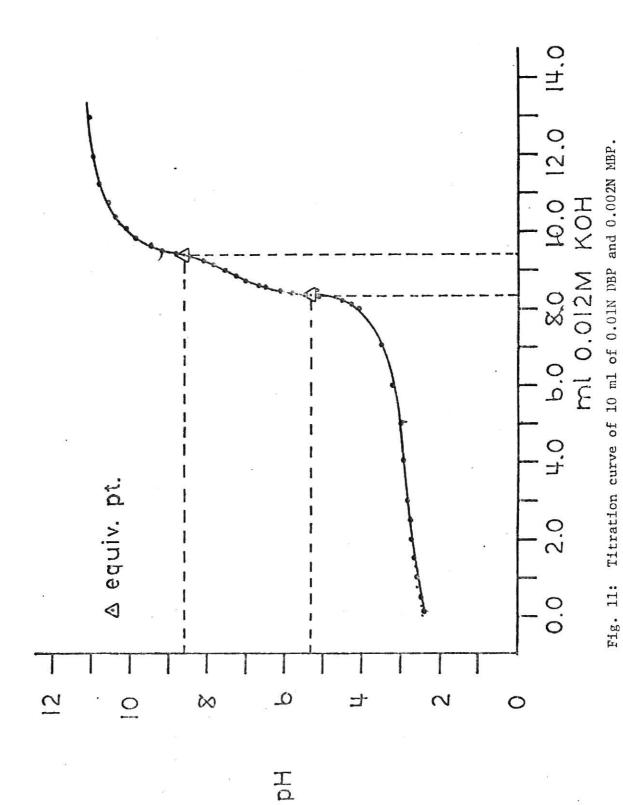


Fig. 9: Titration curve for 15 ml of 0.1N MBP.





4.0 RESULTS AND CONCLUSIONS

This section deals with the results of the irradiation of dodecane, tributyl phosphate (TBP), and mixtures of the two and an analysis of the results of the irradiations. A reaction mechanism inferred by these results is proposed.

4.1 Dodecane

There is little reported data on the yields of hydrogen and methane from dodecane. Uncertainties concerning the effects of different experimental techniques also confuse the evaluation of the literature. For these reasons, the yield of hydrogen and methane from dodecane were determined. Degassed 5 ml samples were irradiated at absorbed dose rates varying from 4.1 x 10^{16} eV/g-min to 4.9 x 10^{16} eV/g-min and to absorbed doses varying from 6.1 x 10^{18} eV/g to 1.75 x 10^{20} eV/g.

A plot of G (hydrogen) as a function of dose is shown in Fig. 12. The solid lines shown on Fig. 12 are results of a least squares fit and the dashed lines are the standard deviation. No statistically significant dose dependence was observed for the hydrogen yield. Therefore, the yield of hydrogen was averaged over all doses. The average yield of hydrogen was $G(H_2) = 6.71$ with a standard deviation of 0.23. The methane yield was detectable, but no conclusion concerning dose dependence could be made. The average methane yield was, $G(CH_2) = 0.051$ and a standard deviation of 0.017.

4.2 TBP

Degassed 5 ml samples were irradiated at absorbed dose rates varying from 5.2 x 10^{16} eV/g-min to 6.0 x 10^{16} eV/g-min and to absorbed doses varying from 2.2 x 10^{19} eV/g to 1.75 x 10^{20} eV/g. A plot of G(H₂) as a function of dose is shown in Fig. 12. No statistically significant dose dependence was observed for the hydrogen yield. Therefore, averaging over

doses, $G(H_2)$ = 2.02 with a standard deviation of 0.13. Methane was also observed, but the yield was less than from dodecane. The average methane yield, $G(CH_A)$, was 0.032 with a standard deviation of 0.008.

A titration was performed on each irradiated sample of TBP to determine the yield of dibutyl phosphate (DBP) and monobutyl phosphate (MBP). At no absorbed dose was the MBP fraction of the total acid yield greater than 10%, which was determined to be the limit of MBP resolution for the titrimetric analysis (see Section 3.4). Since the DBP and MBP could not be resolved, the results of the titrations are reported as the yield of total acid. A plot of G(acid) as a function of dose is shown in Fig. 12.

A slight dose dependence was observed for the yield of acid but was statistically insignificant. Therefore, averaging over all doses, acid yield, G(acid), was 3.71 with a standard deviation of 0.21.

4.3 Mixtures

Mixtures of TBP and dodecane, with electron fractions of dodecane of 40%, 70%, 80%, 90%, and 95% were prepared. Degassed 5 ml samples were irradiated at absorbed dose rates varying from 4.1 x 10^{16} eV/g-min to 6.0×10^{16} eV/g-min and to absorbed doses varying from 1.0×10^{19} eV/g to 5.0×10^{19} eV/g. These samples were analyzed for gases volatile at 161 °K and amount of acid. Hydrogen and methane were the observed gaseous products and MBP was not resolvable from DBP.

Plots of G(H₂) and G(acid) as a function of electron fraction of dodecane of TBP are shown in Fig. 13 and Fig. 14 respectively. These plots are nonlinear, indicating a significant deviation from the mixture law. The yield of hydrogen is less than would be predicted by the mixture law and the yield of acid is greater. The depressed hydrogen yield and increased

acid yield indicates that the two components are interacting and that TBP is being decomposed as a result.

4.4 Discussion

The depressed hydrogen yields and increased acid yields in the dodecane/TBP mixtures indicates that sensitized decomposition of TBP is taking place and that there is the possibility of a dodecane protection reaction occurring.

The dodecane protection reaction is inferred by the decrease in hydrogen yield in the presence of TBP. Confirmation of protection of dodecane by measurement of dodecene degradation products such as dodecene, dodecanol, and dodecane dimer was not done. This was due to the lack of a gas chromatograph capable of separating high molecular weight alkanes, olefins, and alchols. However, all samples were saved for future analysis.

The yield of dodecane degradation products and how they are affected by sensitized decomposition or protection reactions is quite important to the Purex process since they radically effect process efficiency and are quite difficult to remove. Dodecene could be a particular problem with high burn up fuels where a significant amount of radioiodine, a prevalent fission product, would be present. Iodine readily adds across the double bounds of an olefin like dodecene and the halogenated dodecene's effect on the process is not known. It might interfere with decontamination of the fissile species or the presence of the halogen group might be exploitable as a means to scrub the solvent stream of dodecene prior to solvent recycle.

The effect of sensitized TBP decomposition on a Purex process could also be important, due to increased DBP and MBP yield.

DBP, a strong monoprotic acid, causes a reduction in the attainable decontamination factor due to the zirconium and niobium complexes which are not scrubbed out by nitric acid washes [24].

At the dose rates encountered in this work, less than 10% of the total acid yield was MBP. However, there is a possible dose rate dependence which could increase the MBP yield significantly at very high fuel activities. This could be quite important since MBP forms a complex with plutonium that is insoluble in both the organic and aqueous phases. Large, high burn up Purex plants could then have considerable problems with accidential nuclear criticality due to deposition of this MBP/Pu complex in the process piping.

4.5 Mechanism

Making the assumption that the energy absorbed by a component is directly proportional to the electron fraction, a reaction scheme is proposed to account for the observed results. The proposed mechanism is in three parts, the pure dodecane reactions, TBP reactions and the reactions coupling TBP and dodecane.

The dodecane reactions are:

$$c_{12}^{H}_{26} \xrightarrow{\checkmark} c_{12}^{H}_{26}^{+} + e^{-}$$

$$c_{12}^{H}_{26} \xrightarrow{\checkmark} c_{12}^{*}_{126}^{*}$$
(2)

$$c_{12}H_{26}^{+} + e^{-} ---> c_{12}H_{26}^{*}$$
 (3)

$$c_{12}^{H_{26}^{*}} ----> c_{12}^{H_{24}} + H_{2}$$
 (4)

$$c_{12}^{*}H_{26}^{*} ----> c_{12}^{*}H_{25}^{\circ} + H^{\circ}$$
 (5)

$$H^{\circ} + C_{12}H_{25}^{\circ} ----> C_{12}H_{26}$$
 (6)

$$c_{12}^{H}_{26} + H^{\circ} ----> c_{12}^{H}_{25}^{\circ} + H_{2}$$
 (7)

Reactions (1) and (2) produce the primary intermediate species. Reactions (4), (5), and (7) are the hydrogen producing reactions. Reaction (6) is the only significant hydrogen consumption reaction in pure dodecane. Disproportionation and dimerization of $C_{12}^{H^{\circ}}$ are not dealt with since the yield of olefins and dimer were not measured in this work. Also, there was insufficient data to include methane production in this reaction mechanism.

The TBP reactions are:

$$TBP \xrightarrow{\hspace{1cm} \hspace{1cm} \hspace{1cm}} TBP^* + e^- \tag{8}$$

$$TBP \xrightarrow{V} TBP^*$$
 (9)

$$TBP^{+} + e^{-} - TBP^{*}$$
 (10)

$$TBP + e^{-} - TBP^{-}$$
 (11)

$$TBP^{+} + TBP^{-} ----- TBP + TBP^{*}$$
 (12)

$$TEP^* ---- (C_4H_9C)_2(C_4H_8O) PO^* + H^*$$
 (13)

$$TBP* ---> (C_4H_9O)_2(C_4H_7O) PO + H_2$$
 (14)

$$TBP* ----> (C_4 H_9 O_2) PO_2^{\circ} + C_4 H_9^{\circ}$$
 (15)

$$(C_4H_9O)_2 (C_4H_8O) PO^{\circ} + H^{\circ} ----> TBP$$
 (16)

$$TBP + H^{\circ} ----> H_2 + (C_4H_9O)_2 (C_4H_8O) PO^{\circ}$$
 (17)

$$(C_4H_0O)_2 PO_2^{\circ} + H^{\circ} ----> DBP$$
 (18)

$$c_4 H_9^{\circ} + H^{\circ} ----> c_4 H_{10}$$
 (19)

Reactions (8) thru (12) are the producers of the primary intermediates.

Reactions (13), (14), and (17) are hydrogen producing. Reactions (16),

(18), and (19) are hydrogen consuming. Methane, TBP dimer, and some TBP radicals are not considered due to lack of data.

Reactions between TBP and dodecane are shown below:

$$TBP^- + C_{12}H_{26}^+ ----> TBP + C_{12}H_{26}$$
 (20)

$$TBP^{-} ---> (C_4 H_9 O)_2 PO_2^{-} + C_4 H_9^{\circ}$$
 (21)

$$(C_4H_9O)_2 PO_2^- + C_{12}H_{26}^+ ----> DBP + C_{12}H_{25}^{\overline{o}}$$
 (22)

If reaction (11) takes place and it utilizes electrons produced from dodecane it can produce an ionized form and depress the amount of excited state dodecane. Also, the resulting TBP can lead to the production of a DBP precursor and a butyl radical that are hydrogen consuming, this is shown in reaction (21). In reaction (22) hydrogen is abstracted from the dodecane, forming a dodecane radical which will consume hydrogen. MBP production was neglected due to the lack of experimental evidence of a diprotic acid in any of the titrations.

4.6 Summary

The average yield of hydrogen from dodecane was found to be, $G(H_2) = 6.71$ with a standard deviation of 0.23, as compared to the $G(H_2) = 4.9$ in Ref. [11]. The yield of hydrogen for TBP was, $G(H_2) = 2.02$ with a standard deviation of 0.13, this falls within the range of values reported in literature. The acid yield was, G(Acid) = 3.71 with standard deviation of 0.21, this was well above literature values. The yield of hydrogen in the mixtures was less than expected by mixture law and the acid yields are greater than expected by mixture law, therefore sensitized decomposition of TBP is taking place.

4.7 Further Work

The identity and the yields of dodecane degradation products need to be investigated. This information would help refine the proposed reaction

mechanisms and confirm or deny dodecane protection. A more sophisticated gas chromatograph than was available for this work may be able to perform this analysis, but it will complicated by the presence of TBP in mixtures.

Gas chromatograph analysis of the gaseous radiolysis products uncovered small air leaks in a few of the samples; however, the measured oxygen fraction was far smaller than the fraction encountered in normal air.

Apparently, oxygen consumption took place during irradiation. Since full scale Purex operations take place in an air saturated environment, this effect should be explored.

Another area needing investigation is that of high Linear Energy Transfer irradiation of dodecane and TBP. A proposed technique is neutron bombardment of boron doped samples of dodecane or TBP to produce in situ alpha irradiation. High Linear Energy Transfer irradiation might have significantly different radiolysis yields due to much higher local dose rates encountered inside the radiation track. MBP yields could be significantly affected.

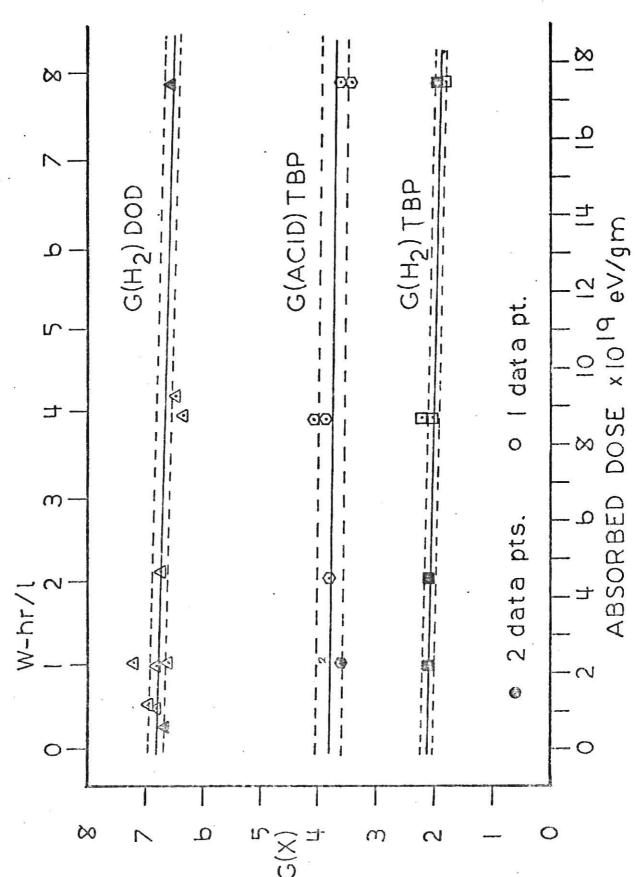
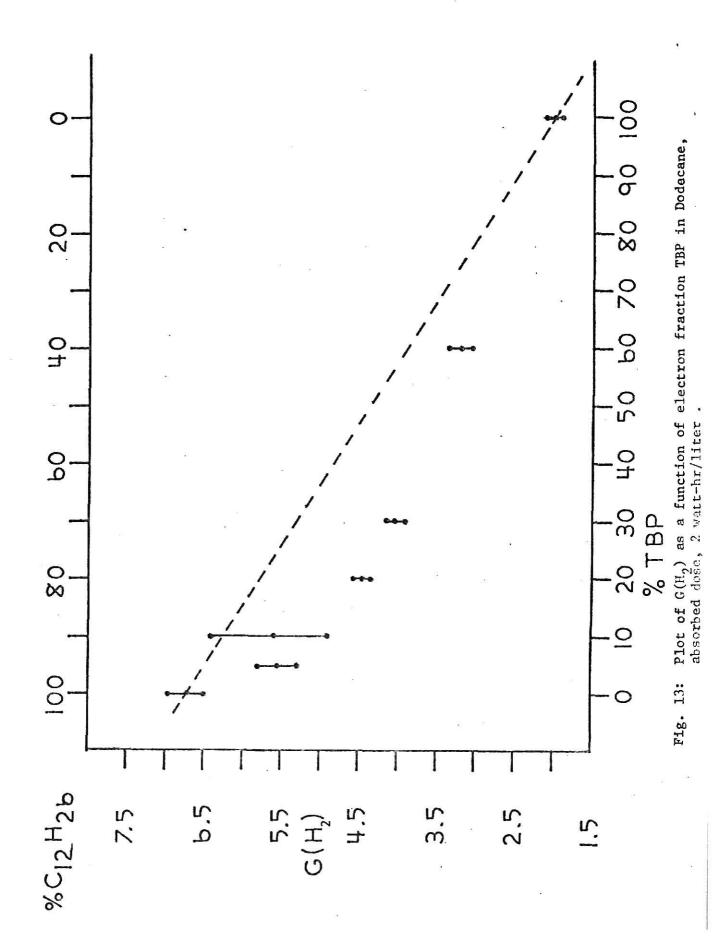
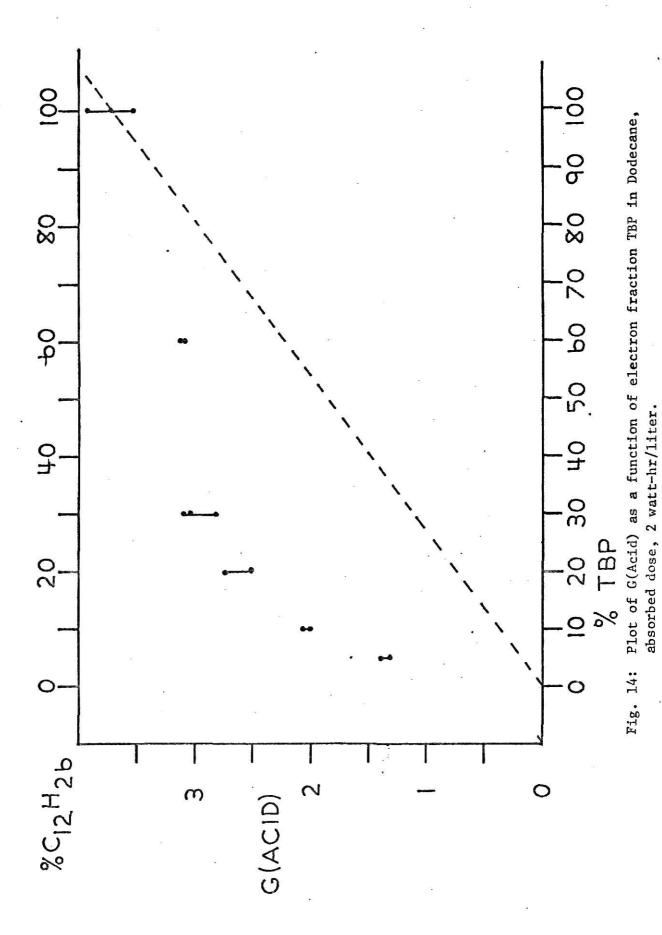


Fig. 12: Plot of product yields as a function of dose for TBP and dodecane.





5. BIBLIOGRAPHY

- 1. E. Wertheim, <u>Textbook of Organic Chemistry</u>, (McGraw-Hill Book, Co., Inc., New York, 1951), Chapt. 19, p. 235.
- 2. R. A. Ewing, S. J. Kiehl, Jr., and A. E. Bearse, "Degradation Products of Tributyl Phosphate," BMI-1073 (1956).
- A. L. Marston, D. L. West, and R. N. Wilhite, "Selection, Cost, and Performance of n-Paraffin Diluents," (AEC)CONF-65018-2(1965).
- R. Stephenson, <u>Introduction to Nuclear Engineering</u>, (McGraw-Hill Book Co., Inc., New York, 1958), Chapt. 10, p. 396.
- S. Glasstone and A. Sesonske, <u>Nuclear Reactor Engineering</u>, (Van Nostrand Reinhold Co., New York, 1967), Chapt. 8, p. 492-499.
- 6. J. O'Donnell and D. Sangster, <u>Principles of Radiation Chemistry</u>, (American Elsevier Publishing Co., New York, 1970), Chapt. 2, p. 19.
- J. O'Donnell and D. Sangster, <u>Principles of Radiation Chemistry</u>
 (American Elsevier Publishing Co., Inc., New York, 1970), Chapt. 2, p. 10.
- R. A. Holroyd, <u>Fundamental Processes in Radiation Chemistry</u>, (Interscience Publishers, New York, 1968), Chapt. 7, p. 435.
- 9. S. Glasstone and A. Sesonske, <u>Nuclear Reactor Engineering</u>, (Van Nostrand Reinhold Co., New York, 1967), Chapt. 10, p. 592.
- J. Spinks and R. Woods, <u>An Introduction to Radiation Chemistry</u>, (John Wiley & Sons, Inc., New York, 1964), Chapt. 2, p. 53.
- H. A. Dewhurst, "Radiolysis of Organic Compounds. V. n-Hexane Vapor," Journal American Chemical Society, 83, p. 1050, (1961).
- 12. J. O'Donnell and D. Sangster, <u>Principles of Radiation Chemistry</u>, (American Elsevier Publishing Co., Inc., New York, 1970), Chapt. 7, p. 104.
- 13. R. A. Holroyd, <u>Fundamental Processes in Radiation Chemistry</u>, (Interscience Publishers, New York, 1968), Chapt. 7, p. 497-499.
- 14. M. Burton and S. Lipsky, "Mechanisms of Protection in Radiolysis of Organic Systems," <u>Journal of Physical Chemistry</u>, 61, 1461 (1957).
- 15. M. Burton, J. Chang, S. Lipsky, and M. P. Reddy, "Radiation Protection in Cyclohexane," <u>Radiation Research</u>, 8, 203 (1958).
- 16. E. P. Barelko, I. P. Solyanin, and Z. I. Tsvetkova, "Radiation-Chemical Stability of TBP in Solutions of Hydrocarbons," <u>Atomnaya Energiya</u>, <u>Vol. 21</u>, No. 4, p 281 (1966).

- 17. T. F. Williams and R. W. Wilkinson, "Radiolysis of Tri-n-alkyl Phosphates," Journal of the Chemical Society, 4098 (1961).
- 18. L. L. Burger, "The Decomposition Reactions of Tributyl Phosphate and its Diluents and Their Effect on Uranium Recovery Processes," Process Chemistry, (Pergamon Press, New York, 1958), Series III, Vol. 2, Chapt. 7, p. 317.
- 19. G. I. Cathers, "Radiation Damage to Radiochemical Processing Reagents," Process Chemistry, (Pergamon Press, New York, 1956), Series III, Vol. 1, Chapt. 2, p. 74.
- 20. J. G. Burr, "The Radiolysis of Tributyl Phosphate," <u>Radiation Research</u>, <u>8</u>, p. 214 (1958).
- 21. H. A. Dewhurst, "Radiation Chemistry of Organic Compounds. I. n-Alkane Liquids," Journal of Physical Chemistry. 61, 1466 (1957).
- 22. J. Spinks and R. Woods, An Introduction to Radiation Chemistry, (John Wiley & Sons, Inc., New York, 1964), Chapt. 4, p. 106-112.
- 23. K. W. Saunders and H. A. Taylor, "The Photolysis of Acetone in Presence of Mercury," Journal of Chemical Physics, 9, 616 (1941).
- 24. P. Brown, J. FLetcher, C. Hardy, J. Kennedy, D. Scargill, A. Wain, and J. Woodhead, "The Significance of Certain Complexes of Ruthenium, Niobium, Zirconium, and Uranium in Plant Process," Process Chemistry (Pergamon Press, New York, 1961), Series III, Vol. 3, Chapt. 3, p. 147.
- 25. L. L. Burger and C. M. Slansky, "Density and Viscosity of Solutions in the Tributyl Phosphate Process for Uranium Recovery," (AEC)HW-15233 (1949).
- 26. Handbook of Chemistry and Physics, R. C. Wesast, Ed., Chemical Rubber Publishing Co., Cleveland, 56th Edn., p. C-274.
- L. L. Burger and E. D. McClanahan, "Tributyl Phosphate and its Diluent Systems," <u>Industrial and Engineering Chemistry</u>, 50, 153 (1958).
- R. M. Wagner, E. M. Kinderman, and L. H. Towle, "Radiation Stability of Organophosphorus Compounds," <u>Industrial and Engineering Chemistry</u>, 51, 45 (1959).
- 29. J. F. Merklin, "The Radiation Chemistry of Organic Compounds," Ph.D. Thesis, University of Minnesota (1963).
- 30. C. J. Hardy and D. Scargil, "Studies on Mono- and Di-n-Butylphosphoric Acids-I, The Separation of Mono- and Di-n-butylphosphoric Acids by Solvent Extraction and by Paper Chromatography," Journal of Inorganic Nuclear Chemistry, 1959, Vol. 10, p. 323.

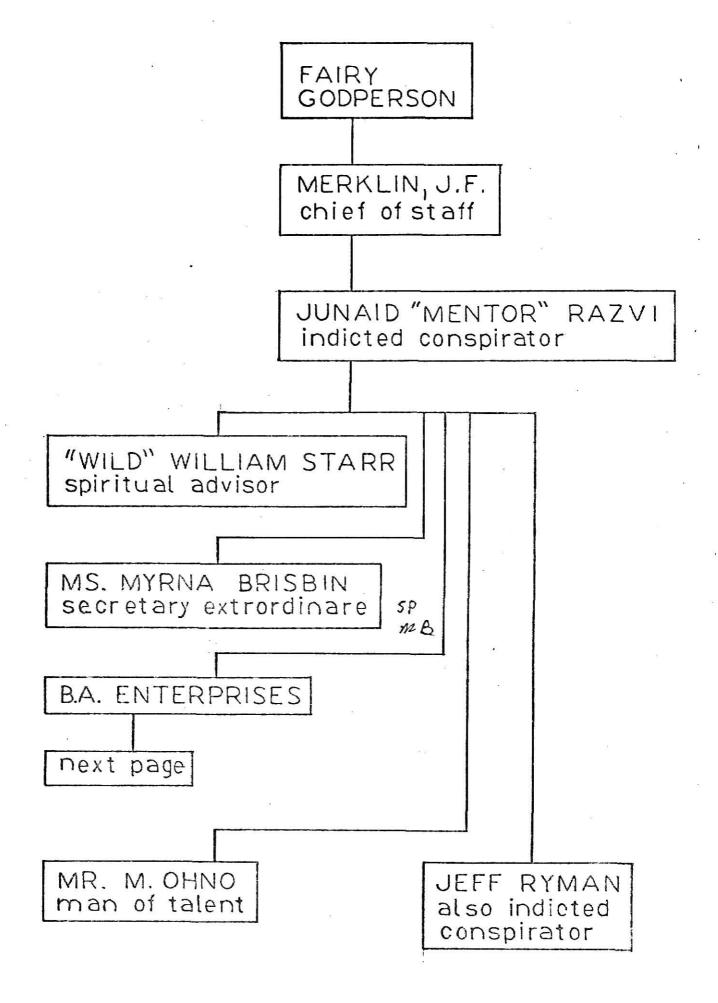
ACKNOWLEDGEMENTS

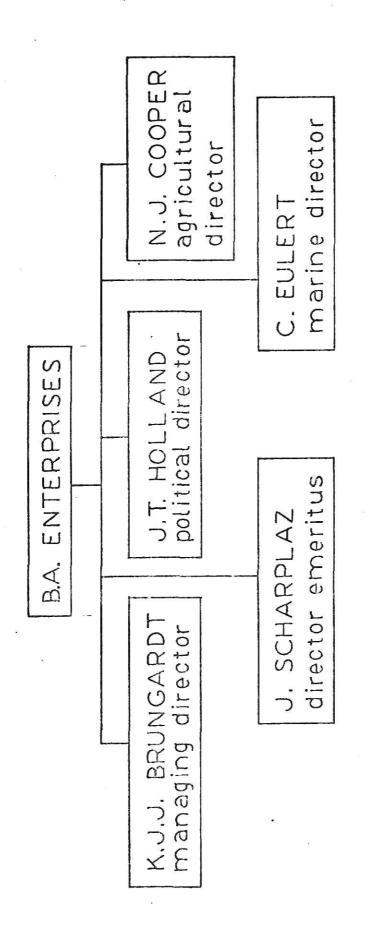
I would like to thank my Fairy Godperson and staff for getting me thru my masters. Table of organization on following two pages.

I would like to also thank the Nuclear Engineering.

Department faculty for causing me to do this thesis, it

was one of the luckiest things to happen to me.





$\label{eq:APPENDIX} \textbf{A}$ Some Physical Properties of the TBP-Dodecane System.

Table A-1 Physical properties of butyl phosphates.

Property	TBP	DBP	MBP
*molecular weight	263.3	210.2	154.1
*density (gm/cm ³)	0.97	1.065	1.22
*viscosity (mp, 25 °C)	33	520	4300
**boiling point	289 °C		
***pK		1.72	1.89 & 6.84
**solubility in water (gm/liter)	0.2		

^{*[2]}

Table A-2 Physical properties of dodecane*

Property	Dodecane
molecular weight	170.34
melting point	-9.6 °C
boiling point	216.3 °C
density	$0.7487 (gm/cm^3)$

^{*[26]}

Table A-3 TBP-Dodecane mixture data.

TBP Electron Fraction	Dodecane Electron Fraction	TBP v/o	Dodecane v/o	Density (gm/cm ³)	Dose Correction Factor*
100	0	100	0.0	0,9727	0.9407
60	40	54.8	45.2	0.871	0.8589
30	70	25.7	74.3	0.8063	0.8063
20	80	16.8	83.2	0.7863	0.7902
10	90	8.2	91.8	0.7671	0.7747
5	95	4.0	95.9	0.7569	0.7672
0	100	0.0	100.0	0.7487	0.7598

^{*}Dose Correction Factor corrects for the difference in electron density of these mixtures and the Fricke dosimeter solution.

^{*}*[25]

^{***[18]}

APPENDIX B: UV spectrophotometer Results

Figure B-1 shows the results of UV spectrophotometric analysis of practical grade dodecane and dodecane after purification. Included on Figure B-1 is a plot of the maximum permissible absorbance for spectrophotometric grade dodecane as given in the Aldrich Catalog-Handbook of Organic and Biochemicals, 1977-1978, Aldrich Chemical Company, Inc. This plot indicates that the purified dodecane used in this work is near spectrophotometric grade in purity.

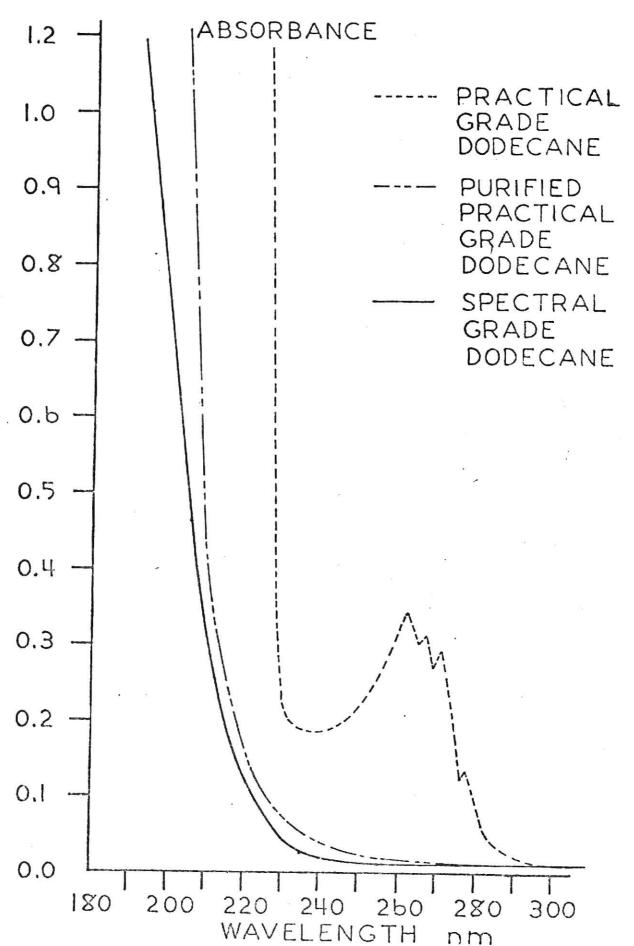
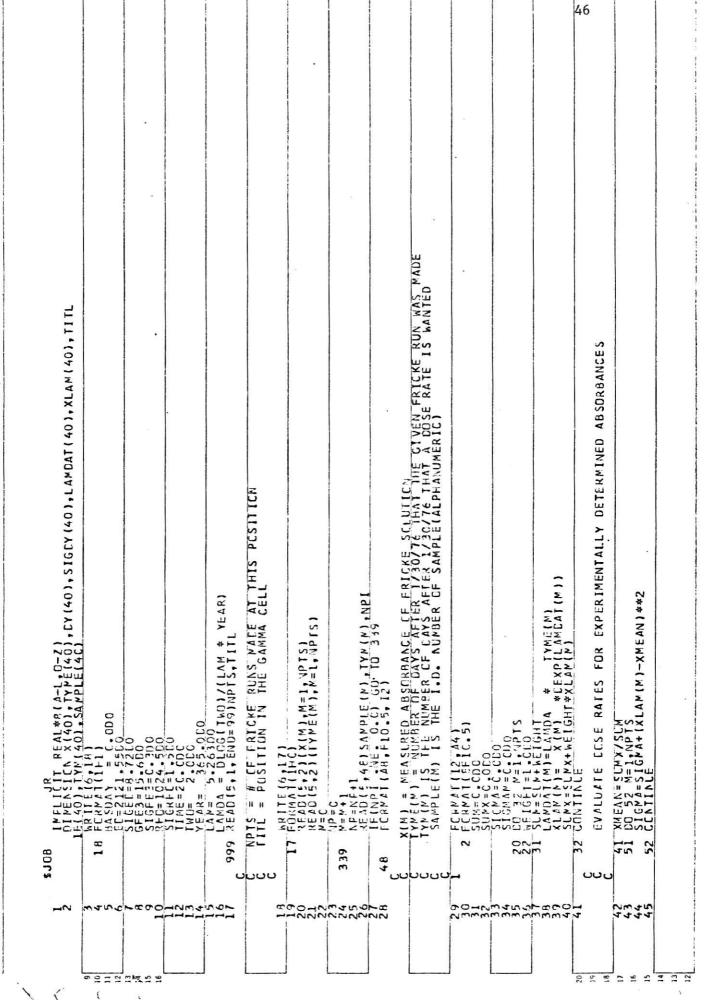


Fig. B-1: UV spectrophotometric results for spectral grade, purified practical grade, and unpurified practical grade dodecane.

APPENDIX C: Dose Rate Program

A sample output from the program used to calculate the dose rate is shown on the following pages. The program first calculates the dose rate for the twelve positions of sample holder on January 30, 1976, this is done by using the results of eighteen Fricke dosimeter runs that were preformed over a period of six months. Each Fricke measurement is corrected to the dose rate of 1/30/76 by a decay correction factor.

The next step of the program is the calculation of dose rate for the irradiated sample. This is done by correcting the January 30, 1976 dose rate at each position to the date of the sample irradiation by means of a decay correction factor. The resulting dose rates are those that would be absorbed by a Fricke dosimeter solution on that specific date, so a correction factor for the difference in electron density of Fricke solution and irradiated sample must be applied. This correction factor is listed in Appendix A, Table A-3.



				47	
	3) \$1 **2+(\$1 GRH O/RHO	SIGDWL 4,1X,D10,4,3X,D1	# '', 4x, 'DO SE RATE WATT/L', DRNL'SIGDWL '1X, DIO.4, 3X, DIO.	()	
IGMA/FREE)	TES -C23E23/RHC)*(EAN)**2+(SIGED) C2D-14 1.6020-14 6 DR)**2+2.14370 T(SIGDWL)	1 GDR- 1 GDR- 5 X , Y PE 5 X , F B 1 A M CA	0.20-14 1.6c20-14 1.6c20-14 1.816DkL) 1CN'* 44.2x, 'LATE', 2x, 2x, 'SAMPLE 1CDN*EV, RAD/MIN, SIGDR, URKAD, SIGRD M), SAMPLE(M), DR, SIGDR, URKAD, SIGRD 6x, AB, 15x, ClO.4, 2x, ClO.4, IX, ClO.4		
FREENPTS-1 FREENTS-1 FREENTS-1	C EVALUATE CCSE R C DR = [YMEAN FD) * (1	1	DRAD = DR * 1. SIGRD = SIGDR * SIGRD = SIGDR * SIGRL = (5.10) * SIGRL = (5.10) * SIGRL = (5.11) TITL II F F (6, 17 7) TYP WRITE (6, 17 7) TYP WRITE (6, 17 7) TYP TA F CONTINUE (7.1) 14, 2x, 51 C (2.4) 777 CONTINUE (7.4) 99 STUP	\$ ENT RY	
4111	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	0 000000		200	13 13 15 15 15 15 15 15 15 15 15 15 15 15 15

c dasoar

Data Documents, Inc. 02

-

MAT1/L. SIGEN-W-02 0.19110 00 0.39796-02 WAT1/L. SIGEN-W-0.1796 00 0.36016-02 WAT1/L. SIGEN-W-02	0.19200 00 0.40330-02 WATITLE SIGDR-W 0.17440 00 0.3663C-02 WATITLE SIGDR-W	######################################	2 16000 2 16000 3 1
S1GDR-RAD. C. 23260 07 S1GUR-RAD. O.21050 02 S1GDR-RAD. O.20910 02	SIGDR-RAD 5.23580 C2 SIGOR-RAD 0.21410 U2 SIGOR-RAD 0.210.20 02	0 5.1250 B D D D D D D D D D D D D D D D D D D	0. 210 % 0.
RAD/WIN* 0.11200 04 RAD/MIN* 0.1013C 04 RAD/WIN*	RAD/WINT 0.11250 04 10220 04 RAD/WINT 0.10030 04	2. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	0.101200.04 0.102100.04 0.101700.04 0.10150.04 0.10150.04 0.10120.04 0.1009010.04
SIGDR-EV 0.14520 16 SIGDR-EV 0.13140 16 SIGDR-EV	SIGDR-EV- 0-14720-16 SIGDR-EV- 0-13360-16 SIGDR-EV- 0-13120-16	\$\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\	0.130000 0.1300000 0.13000000 0.130000000000
EV/GM-MIN 0-699CD 17 EV/GM-MIN 0-6325D 17 EV/GM-MIN 0-6 284D 17	0.70230 IN 0.63760 IN 0.63760 IN 0.63760 IN 0.62690 IN		0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
DOSE RATE: DOSE RATE: DOSE RATE:	DOSE RATE: DOSE RATE: DOSE RATE:	DOSE RATE: DCSE RATE: DOSE RATE:	DOSE RATE: DOSE RATE: DOSE RATE: DOSE RATE: DOSE RATE:
ADSORBANCE O 787 SAMPLE # C-141 SAMPLE #	ABSORBANCE 0, 791 SAMPLE # 5, 121 SAMPLE #	S C C C C C C C C C C C C C C C C C C C	2 A A B C C C C C C C C C C C C C C C C C
2777 2777 2777 2951	DATE CATE 2677 2677 318.0	7070 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
POSITION A	15 PGSITICN B POSITION B PGSITION B	0.5171 0.5171 0.5171 0.5171 0.5171 0.5171 0.5171 0.5171	POSITION D

POSITION D	318.0 DATE 322.0	C-95.52 SANPLE # D-8.51	DOSE RATE:	0.62880 17 EV /GP-MIN 0.6279D 17	0.13040 16 SIGOR-EV 0.13020 16	0.10070 C4 RAE/MIN 0.1006E 04	0.2089D 02 SIGDR-RAD. 0.2086D 02	0.1719D 00 WAIT/L	0.35745-02 SIGDR-W 0.35680-02
PCSITION E POSITION E	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	ABSORBANCE SAMPLE#	DOSE RATE:	0 0 6 6 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	SIGNR-EV 0.1020R-EV 0.1020R-EV 0.11090R-EV 0.11090R-EV 0.11090R-EV 0.11090R-EV 0.11090R-EV 0.11080-EV 0.11080-EV 0.11080-EV 0.11080-EV 0.11080-EV 0.11080-EV	0 8 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0 SIGOR-RAD.	0.44717/L 0.41717/L	SIGDR-W SIG
POSITION F	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	A B S C R B A D R B A	DOSE RATE:	0.559180 IN O.559180 IN O.5591	S160R-EV 0.13450 16 0.12220 16 0.12220 16 0.1220 16 0.120R-EV 0.160R-EV 0.160R-EV 0.160R-EV 0.160R-EV 0.160R-EV 0.160R-EV 0.160R-EV 0.160R-EV	RAD/MIN. 0.810440 0.874810.03 0.874810.03 0.8787810.03 0.8787810.03 0.8787810.03 0.8787810.03 0.8787810.03 0.8787810.03 0.8787810.03	SISDR-RAD. SISDR-RAD. SIGOR-RAD. SIGOR-RAD. SIGOR-RAD. SIGOR-RAD. SIGOR-RAD. OSIGOR-RAD. OSIGOR-RAD. OSIGOR-RAD. OSIGOR-RAD. OSIGOR-RAD. OSIGOR-RAD. OSIGOR-RAD. OSIGOR-RAD. OSIGOR-RAD. OSIGOR-RAD. OSIGOR-RAD. OSIGOR-RAD. OSIGOR-RAD. OSIGOR-RAD. OSIGOR-RAD. OSIGOR-RAD.	WATTYL WATTYL WATTYL WATTYL C. 15950 WATTYL O. 15950 WATTYL O. 15870 O. 15870 WATTYL O. 15870 O. 15870	SIGCR-W C. 3688D-02 SICUS-W SICUS-W SICUS-W SICUS-W SICR
PCSITION G POSITION G POSITION G POSITICN G POSITICN G POSITION G POSITION G	2 0 AT E 2 93 - C 2 9	ABSORDANCE 0.739 0.739 1-182 # 5 APPLE # 0-144 # 5 AMPLE # 5 AMPLE # 5 AMPLE # 5 AMPLE # 5 AMPLE #	DOSE RATE: DOSE RATE: DOSE RATE: DOSE RATE: DOSE RATE:	0.55960 17 0.55960 17 0.55960 17 0.55960 17 0.55960 17 0.5660 17 0.5660 17 0.5660 17 0.5660 17 0.5660 17	SIGDR-EV 0.13420 16 0.12130 16 0.12130 16 0.12080 16 0.12080 16 0.12080 16 0.12080 16 0.12080 16	RAD/WIN, 0. 1051D 04 0. 1051D 04 0. 9496D 03 0. 9496D 03 0. 9455D 03 0. 9445D 03 0. 9411D 03 RAD/WIN, 3	SIGDR-RAD. 0.21500 RAD. 0.19430 U2 0.19430 U2 0.19430 O2 0.19320 O2 0.19320 O2 0.19250 O2	WATT/L, 00 . 17940 00 . 17940 00 . 0. 16210 00 . 0. 1617L, 00 . 0. 1612C 00 . WATT/L, 00 . 16060 00 . 0. 0. 16060 00 . 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	SIGER-W 0.362950-02 SIGER-W 0.33240-02 SIGER-W 0.33076-02 SIGER-W SIGER-W SIGER-W SIGER-W

					50
SIGNA-W 0.3285C-02 SIGDR-W 0.3285C-02 SIGDR-W 0.3277D-02 SIGDR-W 0.3277D-02 SIGCR-W 0.3271D-02	S16CR-W S16CR-W S16SR-W S16SR-W S16CR-W	SIGER-W 0.33916-02 SIGBR-W 0.33490-02	SIGER-W C 3420-02 SIGER-W SIGER-W SIGER-W SIGER-W C 30926-02 C 30770-02	SIGER-W SICOR-W 0.3046-02 SIGER-W 0.3046-02 SIGER-W 0.30160-02	S1663-W 0.33480-02 S1668-W 0.30100-02
0.16060 C0 MATT/L 0.15010 00 MATT/L WATT/L 0.15990 00 WATT/L 0.15950 00 WATT/L 0.15950 00	MATT/L. 0.17930 00 1.16280 00 0.16280 00 MATT/L. 0.16080 00 0.16080 00 0.16080 00 0.16080 00 0.16080 00 0.15990 00	0.16670 00 WATT/L, 0.14990 00	WATT/L, CO WATT/L, CO WATT/L, OU WATT/L, OU WATT/L, OO	WATT/L. C. 16510 WATT/L. O. 1499C OO WATT/L. C. 14840 CC	0.16580 00 WATT/L 0.14900 00
S 1975D 02 S 160R-RAD S 130R-RAD S 1617D 62 S 161R-RAD S 1618-RAD S 1618-RAD S 160R-RAD S 160R-RAD S 160R-RAD	4 0.2150R-RAD, 5 160R-RAD, 5 160R-RAD, 5 160R-RAD, 5 160R-RAD, 5 160R-RAD, 6 19150 02 6 19150 02 7 160R-RAD, 8 0.19150 02 8 0.19150 02 9 0.19150 02 8 0.19080 02 8 0.19080 02 8 0.19080 02 8 0.19080 02 9 0.19080 02 8 0.19080 02 9 0.19080 02 9 0.19080 02 9 0.19080 02	S 16DR-RAD, 3 0.19820 02 S 16DR-RAD, 3 0.17820 02	SISDR-RAD. SIGNG-RAD. SIGNG-RAD. SIGNG-RAD. SIGNG-RAD. SIGNG-RAD. SIGNG-RAD. SIGNG-RAD.	SIGDR-RAD. SIGDR-RAD. 3 0.17800 02. 3 0.17620 02.	3 0, 19570 02 SIGDR-RAD. 3 0,17590 02
6 0.94C70 03 8 0.9384C 03 8 0.9384C 03 8 0.93700 03 6 0.93700 03 6 0.936C 03 6 0.936C 03 6 0.936C 03 6 0.936C 03 6 0.93160 03	**************************************	6 0.8782D 0	RAD/WIN, 6 0.982/WIN, 6 0.88830 C RAD/MIN, 6 0.88760	RAD/MIN; 60.9673D C RAE/MIN; 60.8784E 0 RAD/MIN; 70.8696D 0	6 0 97140 0 8 0 97140 0 6 0 87330 C
0.12010 1 0.12010 1 1.0.11980 1 N.0.11980 1 N.0.11970 1 N.0.11970 1 N.0.11970 1 N.0.11930 1 N.0.11930 1 N.0.11930 1	N	N SIGDR-EV N SIGOR-EV N 0.1112D 1	N SIGDR-EV N 0.12490 EV N 0.11290 EV N 0.11280 EV N 0.11280 EV N 0.11220 EV	N SIGDR-EV N SIGDR-EV 7 0.1111D 1 N SIGDR-EV 7 0.1110D 1	SIGDR-EV N SIGDR-EV N C.1098D 1
0.58720 0.58570 0.58570 0.58570 0.58690 0.55690 0.55690 0.55690 0.55690 0.55690 0.55690 0.55690 0.55690 0.55690 0.55690	0.000000000000000000000000000000000000	. 6V /GM-MI 0.60980 1 EV /GW-MI 0.54820 1	EV / GW - M C + V / G	EV /GR-MI - 64 /GR-MI 0.54830 - 64 /GR-MI 0.54830	EV/GM-MI 0.606001 EV/GM-MI 0.545101
DCSE RATE DOSE RATE DOSE RATE DOSE RATE DOSE RATE	DOSE RATE DOSE RATE DOSE RATE DCSE RATE DOSE RATE DCSE RATE DCSE RATE DCSE RATE	DOSE RATE DOSE RATE	DOSE RATE DOSE RATE DOSE RATE DOSE RATE	DOSE RATE DOSE RATE DOSE RATE	DOSE RATE
SAMPLE 3 SAMPLE 3 CN-022 # CN-952 # SAMPLE 3 SAMPLE 3 SAMPLE 3 SAMPLE 3 SAMPLE 3	ABSORBANCE SAPPLE# SAPPLE# SAPPLE# SAPPLE# SAPPLE# SAPPLE# SAPPLE# SAPPLE# SAPPLE# SAPPLE# SAPPLE# SAPPLE# SAPPLE# SAPPLE#	ABSORPANCE 0.687 SAPPLE #	ABSCRBANCE SAMPLE # SAMPLE # SAMPLE # 17121 SAMPLE # REF	ABSORBANCE SAMPLE # SAMPLE # SAMPLE # SAMPLE #	ABSURBANCE 0.683 SAMPLE# REF
307.0 318.0 318.0 318.0 328.0 328.0 334.1 0	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	DATE 0.0 DATE 295.C	279. C 279. C 279. C 2 81. C 2 95. C	DATE 000 000 001 267 267 295	DATE 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
POSITION G	POSITION H	PCSITICN I	PCSITICN J PCSITION J POSITION J	PCSITION K POSITION K PCSITION K	PCSITION L PS PCSITION L PS PS PS PS PS PS PS PS PS P

APPENDIX D

Saunders-Taylor Calibration Data (Done by O. Block, 5/21/71)

Table D-1

Volume Number	Free Volume in ml at 25°*
$\mathbf{v_1}$	76.5759 ± 0.0929
v ₂	8.5446 ± 0.0706
v ₃ .	0.8360 ± 0.0027
v_4	0.2149 ± 0.0071
v ₅	0. 1396 ± 0.0079
v ₆	0.0825 ± 0.00736

^{*}Density of Hg was taken to be 13.5340 $\mathrm{gm/cm}^3$ at 25 °C.

APPENDIX E

Varian 90P3 Gas Chromatograph Calibration Data

The Varian 90P3 was calibrated by injecting known amounts of hydrogen, methane, oxygen, nitrogen, and carbon monoxide. The area under the resulting peaks was determined by cutting out the peak and weighing. The peak weight in grams as a function of micromoles of gas at a particular attenuation, was the data for a least squares fit program, fitting to the formula y = ax, y being peak weight, x be. moles of gas, and a being slope. Below is a tabulation of a for hydrogen, methane, oxygen, nitrogen, and carbon monoxide.

Table E-1

Gas	Attenuation	Slope, a (micromoles/gm)
^H 2	x1	0.009684 ± 0.004174
СН ₄	x16	0.0578 ± 0.0003382
02	x 16	0.02915 ± 0.000446
N ₂	x32	0.01472 ± 0.001832
со	x 16	0.0 02779 ± 0.0004515

THE IRRADIATION EFFECTS ON A MODEL SOLVENT EXTRACTION SYSTEM OF TRIBUTYL PHOSPHATE-DODECANE

by

JOE PASCHAL HOLLAND

B.S., Kansas State University, 1974

AN ABSTRACT OF A MASTER'S THESIS

submitted in partial fulfillment of
the requirements for the degree

MASTER OF SCIENCE

Department of Nuclear Engineering

Kansas State University Manhattan, Kansas 66506

ABSTRACT

The radiation effects on the system of tributyl phosphate (TBP) and dodecane, which is the solvent extraction system used for the Purex process, was studied.

TBP, dodecane, and mixtures of TBP and dodecane were irradiated at an absorbed dose rate of about 5.0 x 10^{16} eV/g-min with absorbed doses of 6.1 x 10^{18} eV/g to 1.75 x 10^{20} eV/g.

The irradiated samples were analyzed for gaseous products noncondensible at 161 °K and acid products from TBP. The gaseous products observed were hydrogen and methane and the acid products were dibutyl phosphate (DBP) and monobutyl phosphate (MBP). The average yield of hydrogen from dodecane was, $G(H_2) = 6.71$, $G(H_2)$ from TBP was 2.02, and G(Acid) from TBP was 3.71.

No significant dose dependence was observed from TBP or dodecane. Deviation from mixture law was observed for the yields of hydrogen and acid products for the mixtures of TBP and dodecane. Sensitized decomposition of TBP seems indicated.